# A Neural Networks Method to Predict Activity Coefficients for Binary Systems Based on Molecular Functional Group Contribution 

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#### Abstract

Artificial neural network (ANN) techniques and functional group contributions were used to develop an algorithm to predict chemical activity coefficients. The ANN algorithm was trained using experimental data for more than 900 binary systems obtained from DECHEMA, a phase-equilibrium database. All experimental data binary systems used in this study are isothermal. The prediction scheme is based on the fact that the atoms in a chemical compound can be grouped in a functional group with its own physical and chemical properties. Thus, almost any chemical compound can be built by combining the right number of functional groups. The functional group interactions among the components in a mixture are estimated and the combination of functional group interactions provides the intermolecular relationship among the components of a mixture and consequently the activity coefficients can be predicted. The intramolecular interactions were not considered in this study. The four-suffix Margules equation was used as the base thermodynamic model to calculate the activity coefficients. The Margules equation is good for modeling enthalpic contributions to the activity coefficient but is not good for modeling entropic contributions to the activity coefficient. The design of functional groups based on quantum mechanics was adopted to develop a method for predicting activity coefficients. ANN techniques are especially useful for modeling a highly nonlinear interaction among the functional groups and the corresponding activity coefficient. One of the major contributions of this research is to propose a method to identify the initial point and the structure of an ANN. The minimum mean squared


prediction error criterion was implemented to determine both a suitable initial point and the structure of the ANN. A random search method was used to determine the optimal initial point and the Levenberg-Marquardt algorithm was used to train the ANN to generate a sample of prediction values and the trim mean based on $20 \%$ data elimination was selected as the best representation of the ensemble prediction of the Margules equation parameters. The algorithm was validated with nineteen vapor-liquid equilibrium systems and results show that the ANN provides a relative improvement over the UNIFAC method. The scope of this study is limited to some chemical compound families (i.e. alcohols, phenols, aldehydes, ketones and ethers), it is required to include more experimental data to cover additional chemical compound families such as carboxylic acids, anhydrides, esters, aliphatic hydrocarbons and halogens.

## Resumen

Se utilizaron redes neuronales artificiales y la contribución de grupos funcionales se utilizaron para desarrollar un algoritmo para predecir coeficientes de actividad. El algoritmo de la red neuronal se adiestró utilizando datos experimentales para más de 900 sistemas obtenidos de DECHEMA, una base de datos de equilibrio líquido-vapor. Todos los sistemas binarios de data experimental utilizados son isotermales. El esquema de predicción se basó en el hecho de que los átomos de un compuesto químico se pueden agrupar formando grupos funcionales con propiedades químicas y físicas únicas. Por lo tanto, cualquier compuesto se puede construir a partir de la combinación exacta de grupos funcionales. Las interacciones de grupos funcionales entre los compuestos de una mezcla son estimadas y la combinación de las interacciones de grupos funcionales provee información sobre las relaciones intermoleculares entre los componentes de la mezcla de modo que los coeficientes de actividad se pueden predecir. Las interacciones intramoleculares no fueron consideradas en este estudio. La ecuación de Margules fue utilizada como el modelo termodinámico base para calcular los coeficientes de actividad. La ecuación de Margules es eficaz para modelar las contribuciones entálpicas al coeficiente de actividad pero no es eficaz para modelar las contribuciones entrópicas. Se adoptó un diseño de grupos funcionales basados en mecánica cuántica para desarrollar el método de predecir coeficientes de actividad. Las técnicas de redes neuronales son útiles para modelar las relaciones no lineales entre los grupos funcionales y su correspondiente coeficiente de actividad. Una de las contribuciones de mayor importancia de esta
investigación es el desarrollo de un método para identificar el punto inicial y la estructura de la red neuronal. El criterio del promedio del cuadrado de los errores se utilizó para determinar tanto el punto inicial óptimo como la estructura óptima de la red neuronal. Un método basado en una búsqueda aleatoria se utilizó para determinar el punto inicial óptimo y el algoritmo de Levenberg-Marquardt se utilizó para entrenar la red neuronal generando una muestra de valores de predicción para la cual el promedio de muestra reducida basado en la eliminación de $20 \%$ de los datos se seleccionó como la mejor representación de la predicción de los parámetros de la ecuación de Margules. El algoritmo desarrollado se validó con 19 sistemas de equilibrio líquido-vapor y los resultados muestran que el método de redes neuronales provee una mejora notable sobre el método UNIFAC. Este estudio esta limitado a algunas familias de los compuestos químicos (alcoholes, fenoles, aldehídos, cetonas y éteres), es requerido incluir datos experimentales adicionales para cubrir familias de compuesto químicos adicionales tales como ácidos carboxílicos, anhídridos, esteres, hidrocarburos alifáticos y halógenos.

To God and to my family ...

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## 1 INTRODUCTION

Several empirical models have been developed to estimate the activity coefficients for a mixture and the most accurate approach is the one that is based on experimental vapor-liquid equilibrium data. Margules and van Laar are two of the empirical models that have been developed to estimate the activity coefficient (Smith et al., 1996). Modern activity coefficient models are based on the local-composition concept, which was introduced by Wilson (1964). Due to molecular size and intermolecular forces, local compositions are assumed to take into account the shortrange orders and nonrandom molecular orientations inside a liquid solution. The success of Wilson equation on vapor-liquid equilibrium calculations was supported by the development of alternate local compositions models. Two of the most well known models are the Non-Random-Two-Liquid (NRTL) developed by Renon and Prausnitz (1968) and the Universal QUAsi-Chemical (UNIQUAC) developed by Abrams and Prausnitz (1975). These models are capable of correlating experimental activity coefficients for species $i$ in a liquid solution over a wide composition and temperature range. They are also capable of interpolating and/or extrapolating the experimental activity coefficients for a wide range of temperatures and compositions based on a few experimental points.

In the absence of experimental data, group contribution methods have been used to predict activity coefficients. In these methods, atoms in a chemical compound are grouped forming functional groups that are assumed to have their own physical and
chemical identity (Fredenslund et al., 1975). Wilson and Deal (1962) introduced the Analytical Solutions of Groups (ASOG) method. Fredenslund et al. (1975) developed the Universal Functional-group Activity Coefficients (UNIFAC) method to predict activity coefficients based on molecular functional groups contribution. UNIFAC is one of the most prominent methods that uses a combinatorial and a residual part with functional groups parameters such as: group volume, group surface area, and binary group interactions to predict the activity coefficients. The UNIFAC's prediction capabilities have been improved by Weldlich and Gmehling (1987) and also by Larsen et al. (1987). They included a modified empirical combinatorial part, temperature dependant group interactions, and additional main groups (Gmehling, 2003).

The group contribution strategy has also been used to estimate pure compounds physical properties. Constantinou and Gani (1994) proposed a new group contribution design for estimating important physical and thermodynamic properties of pure compounds. Essentially, they proposed a general linear regression model that relates the contribution of the functional groups to several physical and thermodynamic properties such as: critical temperature, critical pressure, critical volume, melting point, normal boiling point, standard Gibbs energy, and standard enthalpy. Skander and Chitour (2002, 2003) proposed a group-contribution method to estimate physical properties of hydrocarbons: boiling point, freezing point, and liquid density. They separated experimental data and created the following compound families: $n$-paraffins, isoparaffins, olefins, alkynes, naphthenes, and aromatics. They used a regression equation to extrapolate physical properties of heavier compounds. More recently, Álvarez and

Valderrama (2004) and, Valderrama and Álvarez (2006) have also proposed groupcontribution methods to estimate critical properties.

Almost any chemical compound can be built by combining the right number of functional groups. Thus, in this research we have exploited the idea that functional group interactions among the components in a mixture can be estimated and, by adding these interactions appropriately, the activity coefficients can be predicted.

The aforementioned group-contribution methods use linear and nonlinear regression techniques to represent the relations among the variables of a given system. The relationship between the physical and thermodynamic properties is highly non-linear, and consequently an artificial neural network (ANN) can be a suitable alternative to model the underlying thermodynamic properties. ANN is an especially efficient algorithm to approximate any function with finite number of discontinuities by learning the relationships between input and output vectors (Hagan et al., 1996). Thus, an ANN is an appropriate technique to model the nonlinear behavior of chemical properties. Chow et al. (1995) developed a method for estimating aqueous activity coefficients for aromatic organic compounds using ANN. They demonstrated that when choosing the appropriate network parameters the ANN method provided more accurate predictions of the aqueous activity coefficients than the regression analysis approach.

The purpose of this research is to derive a method to predict activity coefficients. The activity coefficient is a dimensionless parameter; its logarithm is a measure of the deviation of the behavior of a component in a mixture from the ideal-solution behavior. The activity coefficients are crucial in the design of separation processes equipment such as distillation and absorption columns (Smith et al., 1996). Activity coefficients are
predicted to develop feasibility studies and preliminary chemical engineering calculations for separation processes equipment design. Prediction results are usually confirmed with experimental studies on the final design stage of a project. It should be noted that the ANN at the earlier design stage prediction of activity coefficients provides a cost effective decision tool. Our proposed activity coefficients prediction tool based on ANN will provide an additional strategy that may reduce the uncertainties of predicting activity coefficients. Thus, the development of the new method is not intended to fully replace the UNIFAC method but to enhance the forecast and minimize business risk.

Chapter 2 deals with the justification for performing this research. A literature review of publications most relevant to this research is included in Chapter 3. A theoretical background to introduce the fundamental concepts and principles for deriving the activity coefficients and the functionality of the neural networks is presented in Chapter 4. The fifth chapter describes the proposed methodology to estimate activity coefficients. Chapter 6 presents a numerical example to illustrate step by step the application of the suggested methodology. Chapter 7 presents a comparison between the ANN and the UNIFAC methods and Chapter 8 presents some conclusions and future work.

## 2 JUSTIFICATION

Computer developments lead to use computers as a good design tool in all engineering disciplines. Several computers software had been developed during the last two decades to help engineers in performing efficient designs. Those programs help engineers to deeply study their designs and to predict with accuracy its performance by computer simulations before the construction step. Thus, design process is faster and more efficient since computers development because engineers have more capacity to detect design errors and correct them during the design phase.

Numerous computers simulation software are used in Chemical Engineering to design industrial processes equipment such as: chemical reactors, distillation columns, cooling towers, gas scrubbers, and boilers. To perform the necessary calculations for designing those equipments it is necessary to know the chemical, physical and thermodynamic properties of the compounds present in a given process. These properties can be obtained from experimental data or can be estimated from empirical models. Experimental data is the best way to obtain the properties of a chemical compound but it is not always possible because of economical and time limitations. Thus, the analytical and/or empirical models are used to obtain the chemical, physical, and thermodynamic properties of compounds.

The Gibbs free energy is a thermodynamic property that is intimated related to vapor-liquid equilibrium calculations, which are needed for separation processes equipment design. Gibbs free energy also leads to calculations of other thermodynamic
properties such as: internal energy, enthalpy, and entropy. If thermodynamic properties of compounds are known, then it is possible to calculate physical properties such as: boiling point, thermal expansivity, and heat capacity. It should be noticed that the Gibbs free energy is obtained by calculating the activity coefficients, which can be estimated using experimental vapor-liquid equilibrium data or using empirical models. The activity coefficient is a dimensioless variable that measures the deviation of a mixture behavior from ideal. The important role of activity coefficients on thermodynamics is that it is possible to describe the real behavior of a given mixture by using a mathematical model derived for the ideal behavior.

There are computer software with specific algorithms that make the necessary calculations to obtain chemical compounds properties and to design industrial process equipments. However, if the approximate methods produce large deviations from the actual values, then design calculations will be incorrect causing either over specification of the equipment or that the designed equipment will not have the capacity to perform the designed task. That situation leads to waste of time and money.

The low accuracy of the existent models to predict activity coefficients causes the design of industrial processes equipment to be not completely reliable. To obtain reliable design of industrial process equipment it is necessary to perform experiments by making pilot plants and then scale up to an industrial process.

The main purpose of the current work was to develop a method to estimate activity coefficients to improve the accuracy of existent methods. It has been shown that a neural network is an efficient tool to model nonlinear relationships among
thermodynamic variables (Chow et al., 1995). Thus, it is expected that neural networks be an appropriate technique to model the nonlinear behavior of activity coefficients. The proposed method uses molecules functional groups interactions contributions and experimental vapor-liquid equilibrium data to develop a model that could accurately predict activity coefficients when experimental data are not available. An advanced optimization method using neural networks was used to model the nonlinear behavior between functional groups interactions and vapor-liquid equilibrium data.

## 3 LITERATURE REVIEW

The reference more directly related to this study is the publication of UNIFAC method (Fredenslund et al., 1975). It combines a functional-group-contribution concept with a model for activity coefficients based on an extension of the quasi-chemical theory of liquid mixtures, UNIQUAC. The resulting method, UNIFAC, contains two adjustable parameters per pair of functional groups. By using group interaction parameters obtained from experimental data reduction, activity coefficients for binary mixtures may be predicted. Wu and Sandler (1991) improved the UNIFAC method by using quantum mechanics for functional groups. This study provides a strong theoretical background for the identification of functional groups in molecules.

This study is a combination of the use of the functional-groups concept with neural networks to predict activity coefficients. The idea of using neural networks to predict activity coefficients was taken from a Project called Stability Prediction for Drug Products. That project was sponsored by INDUNIV (Industry-University Research Center) during August 1997 to July 1999. The main purpose of the project was to develop a mathematical method to predict expiration dates of pharmaceutical drug products for both liquids and solids formulations. Prediction of the activity coefficients for the drug components were needed to predict the expiration dates. Here comes the idea of using neural networks and functional-groups concept to predict activity coefficients since usually there are not experimental data available for pharmaceutical drugs.

The proposed method consisted on training a neural network using a functional group coefficient that relates the interaction among the functional groups as input and NRTL interaction constants as outputs. Once trained, the neural network was used to predict the NRTL interaction constants and the NRTL model for multicomponent mixtures to calculate the activity coefficients. However, during this investigation it was found that the four-suffix Margules equation offered a better estimation of the activity coefficients for the 921 experimental vapor-liquid equilibrium data systems included in the database. Therefore, the final proposed method used the four-suffix Margules equation as base thermodynamic model to calculate the activity coefficients.

There are several publications regarding the use of ANN to predict physical and thermodynamic properties of chemical compounds. Petersen et al. (1994) developed a predictive tool for activity coefficients using ANN. However, their work was very limited on the data used for training the ANN. Also, a methodology to determine the optimum network structure was not discussed. A comparison with UNIFAC was performed resulting UNIFAC superior to the ANN method. Bilgin (2004) used an ANN approach to estimate activity coefficients for isobaric binary systems. The approach used was based on giving the low boiling component liquid concentration as input to the ANN and the activity coefficients as output. The training of the ANN was performed with half the system experimental data in order to estimate the complete data set. The results ontained were compared between ANN and UNIFAC and it was concluded that the ANN method was superior in estimating the activity coefficients.

Mitchell and Jurs (1998a) developed a model to predict infinite-dilution activity coefficients $\left(\gamma^{\infty}\right)$ for organic compounds under the framework of molecular structure information and ANN. Their model demonstrated to be equivalent to the linear solvation energy relationship (LSER) method reported by Sherman et al. (1996). Mitchell and Jurs (1998b), in a second publication, also developed a model to predict aqueous solubility of organic compounds under the framework of molecular structure and ANN obtaining good results. Rani and Dutt (2002) developed a method to predict infinite-dilution activity coefficients for halocarbons in water and organic compounds in hydrofluoroparaffins using ANN. They obtained results equivalent to the method developed by Mitchell and Jurs (1998a).

Dehghani et al. (2006) developed a method to predict the activity coefficient ratio of electrolytes in solutions containing amino acids using ANN. The root-mean-square deviation for the predicted system was less than 0.01 . Urata et al. (2002) developed a method for predicting vapor-liquid equilibrium of binary systems containing hydrofluoroeters using ANN. Even though they have good accuracy in the results, it was found that the predicted activity coefficient might not fulfill the restrictions of the GibbsDuhem theorem. Taskinen and Yliruusi (2003) performed a literature review on methods for predicting physicochemical properties (i.e. partition coefficient, water solubility, aqueous activity coefficients and boiling point among others) of organic compounds using ANN. From the studied literature they have found that: most physicochemical properties can be predicted from the molecular structure using ANN modeling, it has not been shown that ANN methods are superior to other methods and that much of the
published work can be characterized as exploration of the area rather than development of serious models with properly validated performance.

ANN have been used in several applications to model complex data systems. Design of a pH control system (Kadirkkamanathan and Regunath, 2001), motor fault diagnosis (Gao and Ovaska, 2001), properties of cast irons (Voracek, 2001), fuzzy proportional-integral-derivative controllers (Golob, 2001), image processing (Koppen and Ruiz-del-Solar, 2001), dynamic systems with time delays (Ramirez-Beltran and Montes, 2002) and planning of heating and cooling plants (Inaoka et al., 2001) are cases in which neural networks were applied demonstrating improvement in comparison to the commonly used methods for process data modeling. It should be mentioned that neural networks had been widely applied on different technology disciplines with successful results. The ability to learn the behavior of the data generated by a system gives neural networks its versatility.

## 4 THEORETICAL BACKGROUND

To properly describe the proposed methodology, a fundamental background related to the theory of activity coefficients and neural network algorithms are provided.

### 4.1 Activity Coefficients

Given a closed system, the activity coefficient is a function of the temperature, pressure, and mole fraction of the compounds in the mixture. Smith et al. (1996) pointed out that, for the case of non-ideal solutions, the actual thermodynamic properties are obtained by measuring the energy deviation from the ideal solution, which is called the excess property. Thus, if $M$ represents a molar thermodynamic property, i.e., enthalpy (H), entropy (S), internal energy (U), Gibbs free energy (G), and Helmholtz energy (A), the excess property, $M^{E}$, is defined as the difference between the actual property, $M$, and the ideal-solution property, $M^{i d}$, at the same temperature, pressure, and composition. That is,

$$
\begin{equation*}
M^{E}=M-M^{i d} \tag{1}
\end{equation*}
$$

Usually, when the activity coefficient is studied, the major property of interest is the excess Gibbs free energy, which can be expressed as follows:

$$
\begin{equation*}
G^{E}=G-G^{i d} \tag{2}
\end{equation*}
$$

where, $G^{E}, G$, and $G^{i d}$ are the excess, the actual, and the ideal-solution Gibbs free energy, respectively. After some mathematical manipulations, the molar partial excess Gibbs free energy for the $i^{t h}$ compound can be written as follows:

$$
\begin{equation*}
\bar{G}_{i}^{E}=R T \quad \ln \left(\gamma_{i}\right) \tag{3}
\end{equation*}
$$

and

$$
\begin{equation*}
\gamma_{i}=\frac{\hat{f}_{i}}{x_{i} f_{i}}, \tag{4}
\end{equation*}
$$

where, $T$ is the temperature of the mixture, $R$ is the universal gas constant, $x_{i}$ is the liquid mole fraction for the $i^{\text {th }}$ compound, $f_{i}$ is the fugacity of the $i^{t h}$ pure compound, and $\hat{f}_{i}$ is the actual fugacity of the $i^{\text {th }}$ compound in the mixture. Fugacity is a property that measures the degree of freedom of a molecule moving inside of a given compound (Smith et al., 1996). The variable, $\gamma_{i}$, is called the activity coefficient for the $i^{\text {th }}$ compound. The activity coefficient is equal to 1 for a pure component. Thus, when the activity coefficient of a compound in a mixture is larger than one, it indicates that its molecules have a larger degree of freedom for moving around comparing with a pure compound. On the other hand, an activity coefficient less than one indicates that the molecules in the mixture are closer to each other due to intermolecular attraction and has a smaller tendency to escape by vaporizing than when comparing to a pure compound (Levine, 1988).

The logarithm of the activity coefficient is a partial property with respect to $\bar{G}_{i}{ }^{E} / R T$ according to the following relation (Smith et al., 1996):

$$
\begin{equation*}
\ln \gamma_{i}=\left[\frac{\partial\left(n G^{E} / R T\right)}{\partial n_{i}}\right]_{P, T, n_{j}} \tag{5}
\end{equation*}
$$

where, $n$ is the total number of moles in the mixture, $n_{i}$ is the number of moles of component $i$, and $n_{j}$ is the number of moles of the other compounds in the mixture. Also, the activity coefficient must fulfill the expression:

$$
\begin{equation*}
\frac{\bar{G}_{i}^{E}}{R T}=\sum_{i} x_{i} \ln \gamma_{i} \tag{6}
\end{equation*}
$$

and the Gibbs/Duhem equation:

$$
\begin{equation*}
\sum_{i} x_{i} d \ln \gamma_{i}=0 \quad(\text { const } T, P) \tag{7}
\end{equation*}
$$

For a binary system the Gibbs/Duhem equation can be expressed as follows:

$$
\begin{equation*}
x_{1} \frac{d \ln \gamma_{1}}{d x_{1}}+x_{2} \frac{d \ln \gamma_{2}}{d x_{1}}=0 \quad(\text { const } T, P) \tag{8}
\end{equation*}
$$

The Gibbs/Duhem equation has the following effects on the activity coefficient behavior with respect to the liquid mole fraction:

- At every composition, the slope of $\gamma_{1}$ curve is opposite in sign to the slope of $\gamma_{2}$ curve.
- When $x_{1} \rightarrow 1$, the slope of $\gamma_{1}$ curve is zero and $\gamma_{1} \rightarrow 1$ and when $x_{2} \rightarrow 1$, the slope of $\gamma_{2}$ curve is zero and $\gamma_{2} \rightarrow 1$.

Estimation of the activity coefficient can be obtained using experimental vaporliquid equilibrium data and selecting a suitable thermodynamic model. While $\bar{G}_{i}{ }^{E} / R T$ is a function of $T, P$ and mole fraction, for liquid solutions at low to moderate pressures it is a weak function of $P$ and the pressure dependence of activity coefficients can be neglected (Smith et al., 1996). Therefore, if an empirical mathematical expression is
given for $\bar{G}_{i}{ }^{E} / R T$, then equation (5) can be used to derive an empirical model for the activity coefficients and equation (8) can be used to verify the model consistency with the Gibbs/Duhem theorem. Among the most important thermodynamic models to estimate activity coefficients based on experimental data are the following: Margules, van Laar, Wilson, Non-Random Two Liquids (NRTL), and UNIversal QUAsi-Chemical (UNIQUAC).

For instance, this study used the four-suffix Margules equation as base method for the activity coefficients calculation. The expression for $\bar{G}_{i}{ }^{E} / R T$ for the four-suffix Margules equation is written as follows (Reid et al., 1987):

$$
\begin{equation*}
\frac{G^{E}}{R T}=x_{1} x_{2}\left[A+B\left(x_{1}-x_{2}\right)+C\left(x_{1}-x_{2}\right)^{2}\right] \tag{9}
\end{equation*}
$$

Using equation (5), the expressions for $\ln \gamma_{1}$ and $\ln \gamma_{2}$ are:

$$
\begin{equation*}
\ln \gamma_{1}=(A+3 B+5 C) x_{2}^{2}-4(B+4 C) x_{2}^{3}+12 C x_{2}^{4} \tag{10}
\end{equation*}
$$

and

$$
\begin{equation*}
\ln \gamma_{2}=(A-3 B+5 C) x_{1}^{2}+4(B-4 C) x_{1}^{3}+12 C x_{1}^{4} \tag{11}
\end{equation*}
$$

Thermodynamic models such as Margules, Wilson and van Laar can be used to estimate the activity coefficients. Thus, it is required to obtain experimental data for the system of interest to determine the model parameters and generate the analytical expression, based on the chosen model, for calculating the activity coefficients. However, when experimental data are not available, a prediction method is needed to obtain the activity coefficients. The available prediction methods for activity coefficients are based on functional groups contribution and the most well known are the Analytical Solution of

Groups (ASOG) method (Wilson and Deal, 1962) and the Universal Functional-group Activity Coefficients (UNIFAC) method (Fredenslund et al., 1975). These methods express the activity coefficient as a function of the liquid mole fraction in addition of some physical parameters.

UNIFAC is an effective method for predicting the activity coefficients of various chemical mixtures. The criterion for forming functional groups used in the UNIFAC model is based mostly on molecular geometry. In this research, we proposed a thermodynamic model to predict the activity coefficients using a neural networks technique and functional groups based on quantum mechanics calculations introduced by Wu and Sandler (1991). The list of the functional groups is presented in Appendix B.

There are two fundamental conditions for identifying the functional groups in a given mixture. The first condition states that the group should be independent of the molecule in which it appears and should always have the same geometry. The second condition states that each atom in a group and the group as a whole should have approximately the same net charge independently of the molecule that it appears. This is a very important requirement because it is considered that the intermolecular interaction energy between two groups on different molecules come mainly from electrostatic forces (due to charges on the groups), repulsion forces, van der Waals forces, London (dispersion) forces, and hydrogen-bonding forces.

### 4.2 Neural Networks

Artificial neural network methodology is proposed to model the linear or nonlinear relationships among the functional groups interactions and the activity coefficients. The ANN model technique can be viewed as a general nonlinear modeling approach. Artificial neural networks are a biological inspiration based on various characteristics of the brain functionality. Artificial neurons are simple computational devices that are highly interconnected and the connections between neurons determine the transfer function of the network (Hagan et al., 1996). An artificial neural network determines an empirical relationship between the inputs and outputs of a given system. Where the inputs of the system are the independent variables ( $x$ 's) and the outputs are the dependent variables ( $y$ 's). Therefore, it is important for the user to have a good understanding of the science behind the underlying system to provide the appropriate input and, consequently, to support the identified relationship.

Figure 1 shows the selected structure of the implemented neural network for this study. This figure shows that the identified neural network has three neurons in the hidden layer and three neurons in the output layer with a log-sigmoidal and linear transfer functions in the hidden and the output layers, respectively. Hagan et al. (1996) provides a detailed discussion on the structure and functionality of neural networks. The input $P$ matrix to train the neural network is formed by physical parameters and functional groups interactions information of a given binary mixture system. The variables w's are the weight matrices, $b$ 's are the bias vectors, $n$ ' $s$ are the net input, and $a$ is the output of the
neural network and represents the predicted Margules equation parameters. An efficient procedure to identify the appropriate structure of a neural network is given by RamirezBeltran and Montes (2002).


Figure 1. The Neural Network Structure

The input vector (left), the hidden layer (center) and the output layer (right) are the main components of the selected neural network. $t$ and $p$ are the temperature and the pressure of the system and $\eta$ is the interaction proportion, $w$ 's are the weights, $b$ 's are the bias $n$ is the net input and a's is the output of the network, which are the Margules equation parameters.

Once the structure of the neural network is identified, the next step is to use an optimization technique to estimate the weights and biases in such a way that the output of the network is as close as possible to the target values. In this case the target values are the Margules equation parameters calculated from the experimental data. This optimization strategy is known as the training process and the neural network will learn
the relation between the inputs and the outputs of a dynamic system. Thus, once the neural network is trained the optimal weights are saved with the purpose of predicting the Margules equation parameters.

There are various learning algorithms to train neural networks. Some of the most useful are: Perceptron, Hebbian, Widrow-Hoff, and Backpropagation; the latter is a suitable algorithm for this research because it has the capability of training multilayer neural networks for function approximation (Hagan et al., 1996). However, the original Backpropagation algorithm has several limitations and its major drawback is its low convergence rate for most practical applications. Various modifications of the backpropagation algorithm have been developed and most of them are based on heuristic and numerical optimization strategies.

The heuristic strategies are: the momentum and the variable learning rate. The method of momentum is a heuristic algorithm that improves convergence by using a lowpass filter to smooth out the oscillations of the surface response.

$$
\begin{equation*}
y(k)=\gamma y(k-1)+(1-\gamma) w(k) \tag{12}
\end{equation*}
$$

where, $w(k)$ is the input to the filter, $y(k)$ is the output of the filter and the momentum coefficient $\gamma$ must satisfy: $0 \leq \gamma<1$. The weight and biases are modified according to the following equations that represent the modification to the original backpropagation:

$$
\begin{equation*}
\Delta W^{m}(k)=\gamma \Delta W^{m}(k-1)-(1-\gamma) \alpha \frac{\partial \hat{F}}{\partial n^{m}}\left(a^{m-1}\right)^{T} \text { for weights } \tag{13}
\end{equation*}
$$

and

$$
\begin{equation*}
\Delta b^{m}(k)=\gamma \Delta b^{m}(k-1)-(1-\gamma) \alpha \frac{\partial \hat{F}}{\partial n^{m}} \text { for biases } \tag{14}
\end{equation*}
$$

where, $k$ is the iteration number, $\mathrm{a}^{\mathrm{m}-1}$ is the output of the previous network layer, $\hat{F}$ is the performance index and corresponds to the mean square error of the network, and $\alpha$ is the learning rate.

The key idea of the variable learning rate is to modify the weights and biases update by changing the momentum and learning rate, based on the behavior of the squared errors. There are many variations of the variable learning rate algorithm (Hagan et al., 1996). However, the general rules of the variable learning rate backpropagation algorithm are:

1) If the squared error increases by more than a set percentage $\zeta$ after a weight update, then the weight update is discarded, the learning rate is multiplied by a factor $0<\rho<1$, and the momentum coefficient $\gamma$ is set to zero.
2) If the squared error decreases after a weight update, then the weight update is accepted and the learning rate is multiplied by another factor $\eta>1$. If the momentum coefficient $\gamma$ has been previously set to zero, it is reset to its original value.
3) If the squared error increases by less than $\zeta$, then the weight update is accepted but the learning rate and the momentum coefficient are unchanged.

The heuristic techniques provide significant improvements over the conventional backpropagation algorithm; however, they also exhibit the disadvantage that a trial an error approach must be implemented to identify the appropriate set of training parameter. The improved techniques based on optimization algorithms are more promising since an automatic learning-rate adjustment can be designed. The most prominent techniques are the conjugate gradient (CG) and the Levenberg-Marquardt (LM) algorithms. The major advantage of the CG algorithm is that it does not require calculation of the second derivatives and yet it still has the quadratic convergence property, i.e., convergence is accomplished as if the surface functions were a quadratic function. The CG algorithm applied to neural networks training consists on the following steps (Hagan et al., 1996):

1) Interval location: The interval location step is used to find an initial interval that contains a local minimum. First, the performance index of the network is evaluated at an initial point. Then the performance index is evaluated at a second point, which is at a distance $\varepsilon$ from the initial point along the first search direction $p_{0}$. The search direction can be obtained from the steepest descent direction obtained from the backpropagation algorithm. The performance index is successively evaluated doubling the distance between the points until the function increases after two consecutive evaluations (see Figure 2). The last three evaluations (points $c, d$, and $e$ ) will bracket the local minimum point defining the initial interval.


Figure 2. Interval location
2) Interval reduction: This step reduces the size of the initial interval until the local minimum is reached to a desired accuracy. The extreme points of the initial interval become points $a$ and $b$ respectively. The performance index is evaluated at two points (points $c$ and $d$ ) within the initial interval to reduce its size (see Figure 3). A method called the Golden Section Search is used to determine the location of the internal points $c$ and $d$. The Golden Section search will reduce the interval until reaching the local minimum point with certain accuracy. The algorithm for the Golden Section Search is as follow.

For $\tau=0.618$,

Set

$$
\begin{aligned}
& c_{l}=a_{l}+(1-\tau)\left(b_{1}-a_{l}\right), F_{c}=F\left(c_{1}\right) \\
& d_{l}=b_{1}-(1-\tau)\left(b_{1}-a_{l}\right), F_{d}=F\left(d_{l}\right)
\end{aligned}
$$

For $k=1,2, \ldots$ repeat
If $F_{c}<F_{d}$ then

$$
\text { Set } \begin{array}{ll} 
& a_{k+1}=a_{k} ; b_{k+1}=d_{k} ; d_{k+1}=c_{k} \\
& c_{k+1}=a_{k+1}+(1-\tau)\left(b_{k+1}-a_{k+1}\right) \\
& F_{d}=F_{c} ; F_{c}=F\left(c_{k+1}\right)
\end{array}
$$

else

$$
\text { Set } \begin{array}{ll} 
& a_{k+1}=c_{k} ; b_{k+1}=b_{k} ; c_{k+1}=d_{k} \\
& d_{k+1}=b_{k+1}-(1-\tau)\left(b_{k+1}-a_{k+1}\right) \\
& F_{c}=F_{d} ; F_{d}=F\left(d_{k+1}\right)
\end{array}
$$

end
end until $b_{k+1}-a_{k+1}<t o l$
where $t o l$ is the accuracy tolerance set by the user.


Figure 3. Interval Size Reduction
3) New search direction: This step determines a new search direction to continue with the neural network training until reaching the performance index function minimum. The next gradient is calculated with the backpropagation algorithm and the conjugate gradient algorithm is used to update the weights.
4) Convergence: The procedure will continue until reaching convergence where the difference between the network response and the targets reaches an acceptable level.

The LM algorithm introduces an automatic calculation of a constant that ensure that the Jacobian matrix will be a positive definite matrix and consequently convergence is accomplished. This method was designed to minimize functions that are sums of squared errors of other nonlinear functions. The LM algorithm steps are as follow (Hagan et al., 1996):

1. Using the inputs and the initial point to the network, calculate the corresponding network outputs. The inputs are the chosen parameters for the system beign analyzed and the initial point consists of the initial values, randomly selected, of the weights and biases. Calculate the errors using the network outputs and the targets values and, calculate the sum of squared errors (sse) for all inputs.

$$
\left.\begin{array}{c}
v^{T}=\left[\begin{array}{llll}
v_{1} & v_{2} & \cdots & v_{N}
\end{array}\right]=\left[\begin{array}{lllllll}
e_{1,1} & e_{2,1} & \cdots & e_{S^{M}, 1} & e_{1,2} & \cdots & e_{S^{M}, Q}
\end{array}\right] \\
x^{T}=\left[\begin{array}{llll}
x_{1} & x_{2} & \cdots & x_{n}
\end{array}\right]=\left[\begin{array}{lllllllll}
w_{1,1}^{1} & w_{1,2}^{1} & \cdots & w_{S^{1}, R}^{1} & b_{1}^{1} & \cdots & b_{S^{1}}^{1} & w_{1,1}^{2} & \cdots
\end{array} b_{S^{M}}^{M}\right. \tag{16}
\end{array}\right] .
$$

$$
\begin{gather*}
a_{q}^{(m)}=f^{(m)}\left(w^{(m)} a_{q}^{(m-1)}+b_{q}^{(m)}\right)  \tag{17}\\
e_{q}=t_{q}-a_{q}^{(M)}  \tag{18}\\
\operatorname{sse}(k)=\sum_{i=1}^{S^{(M)}} \sum_{q=1}^{Q} e_{i, q}^{2}(k) \tag{19}
\end{gather*}
$$

2. Calculate the Jacobian matrix.

$$
J(x)=\left[\begin{array}{cccccc}
\frac{\partial e_{1,1}}{\partial w_{1,1}^{1}} & \frac{\partial e_{1,1}}{\partial w_{1,2}^{1}} & \cdots & \frac{\partial e_{1,1}}{\partial w_{s^{1}, R}^{1}} & \frac{\partial e_{1,1}}{\partial b_{1}^{1}} & \cdots  \tag{20}\\
\frac{\partial e_{2,1}}{\partial w_{1,1}^{1}} & \frac{\partial e_{2,1}}{\partial w_{1,2}^{1}} & \cdots & \frac{\partial e_{2,1}}{\partial w_{S^{1}, R}^{1}} & \frac{\partial e_{2,1}}{\partial b_{1}^{1}} & \cdots \\
\vdots & \vdots & & \vdots & \vdots & \\
\frac{\partial e_{S^{n}, 1}}{\partial w_{1,1}^{1}} & \frac{\partial e_{S^{n}, 1}}{\partial w_{1,2}^{1}} & \cdots & \frac{\partial e_{S^{n}, 1}}{\partial w_{s^{1}, R}^{1}} & \frac{\partial e_{S^{n}, 1}}{\partial b_{1}^{1}} & \cdots \\
\frac{\partial e_{1,2}}{\partial w_{1,1}^{1}} & \frac{\partial e_{1,2}}{\partial w_{1,2}^{1}} & \cdots & \frac{\partial e_{1,2}}{\partial w_{s^{1}, R}^{1}} & \frac{\partial e_{1,2}}{\partial b_{1}^{1}} & \cdots \\
\vdots & \vdots & & \vdots & \vdots &
\end{array}\right]
$$

The elements of the Jacobian matrix are calculated using the following equations:

$$
\begin{gather*}
{[J]_{h, l}=\frac{\partial v_{h}}{\partial x_{l}}=\frac{\partial e_{k, q}}{\partial w_{i, j}^{m}}=\frac{\partial e_{k, q}}{\partial n_{i, q}^{m}} \times \frac{\partial n_{i, q}^{m}}{\partial w_{i, j}^{m}}=s_{i, h}^{\sim} \times a_{j, q}^{m-1}}  \tag{21}\\
{[J]_{h, l}=\frac{\partial v_{h}}{\partial x_{l}}=\frac{\partial e_{k, q}}{\partial b_{i}^{m}}=\frac{\partial e_{k, q}}{\partial_{i, q}^{m}} \times \frac{\partial n_{i, q}^{m}}{\partial b_{i}^{m}}=s_{i, h}^{\sim m} \times \frac{\partial n_{i, q}^{m}}{\partial b_{i}^{m}}=s_{i, h}^{\sim m}}  \tag{22}\\
s_{i, h}^{\sim m} \equiv \frac{\partial v_{h}}{\partial n_{i, q}^{m}}=\frac{\partial e_{k, q}}{\partial n_{i, q}^{m}} \tag{23}
\end{gather*}
$$

3. Calculate the new weights and biases.

$$
\begin{equation*}
\mathbf{x}_{k+1}=\mathbf{x}_{k}-\left[\mathbf{J}^{\mathbf{T}}\left(x_{k}\right) \mathbf{J}\left(x_{k}\right)+\mu_{k} \mathbf{I}\right]^{-1} \mathbf{J}^{\mathbf{T}}\left(x_{k}\right) v\left(x_{k}\right) \tag{24}
\end{equation*}
$$

4. Re-calculate the sum of squared errors with the values for the weights and biases. If the new sse is smaller that those calculated in step 1 , then decrease the scalar $\mu$, let the weights and biases become the new values and go back to step 1. Otherwise, increase the scalar $\mu$ and go back to step 3.
5. The LM algorithm will converge when the gradient is less than a predetermined value or if the sse are reduced to an error goal.

One of the limitations of this method is the large amount of memory required for performing calculations. However, for the underlying application the LM algorithm becomes a suitable technique since a small data set is used to train the neural network. It should be noted that only the systems that contain interactions of the system of interest are the ones that will be used to predict the activity coefficient and consequently the required memory is reduced. In this research, heuristics and optimizations techniques were tested and it was determined that for the selected training patterns the best performance was obtained by the Levenberg-Marquardt algorithm. The training patterns studied are presented in Table 1.

The system chloroform (1) + n-butyl alcohol (Ohe, 1989) was selected to test the performance of each training pattern shown in Table 1. The activity coefficients were predicted three times using the ANN method and the overall mean absolute error for $\gamma_{1}$ and $\gamma_{2}$ was calculated for each training algorithm. It can be shown that the LevenbergMarquardt algorithm gave the smaller overall mean absolute error and standard deviation for predicting $\gamma_{1}$. On the other hand, while the Levenberg-Marquardt algorithm did not
give the minimum overall mean absolute error for predicting $\gamma_{2}$ it gave the smaller standard deviation. Thus, the Levenberg-Marquardt algorithm offers the best performance in training the artificial neural network for predicting activity coefficients (see Table 2).

## Table 1. ANN Training Algorithms

| MatLab <br> Command | Training Algorithm Description |
| :---: | :--- |
| traingdm | Batch Gradient Descent with Momentum |
| traingda | Gradient descent with adaptive learning rate backpropagation |
| traingdx | Gradient descent with momentum and adaptive learning rate backpropagation |
| traincgf | Conjugate gradient backpropagation with Fletcher-Reeves updates |
| traincgb | Conjugate gradient backpropagation with Powell-Beale restarts |
| traincgp | Conjugate gradient backpropagation with Polak-Ribiere updates |
| trainscg | Scaled conjugate gradient backpropagation |
| trainoss | One step secant backpropagation |
| trainbfg | BFGS quasi-Newton backpropagation |
| trainrp | Resilient backpropagation |
| trainlm | Levenberg-Marquardt backpropagation |

Table 2. Overall Mean Absolute Error by ANN Training Algorithm

| Algorithm | MAE for <br> $\boldsymbol{\gamma} \mathbf{1}$ | STDEV <br> for $\boldsymbol{\gamma} \mathbf{1}$ | MAE for <br> $\boldsymbol{\gamma} \mathbf{2}$ | STDEV <br> for $\boldsymbol{\gamma} \mathbf{2}$ |
| :---: | :---: | :---: | :---: | :---: |
| traingdm | 0.1491 | 0.1067 | 0.5057 | 0.4829 |
| traingda | 0.1702 | 0.1643 | 0.3372 | 0.5224 |
| traingdx | 0.1311 | 0.0954 | 0.3046 | 0.4882 |
| traincgf | 0.1541 | 0.1217 | 0.2920 | 0.3735 |
| traincgb | 0.1792 | 0.1357 | 0.2217 | 0.3208 |
| traincgp | 0.1361 | 0.1715 | 0.2042 | 0.3695 |
| trainscg | 0.1595 | 0.1325 | 0.2064 | 0.3529 |
| trainoss | 0.0897 | 0.0826 | 0.3033 | 0.3388 |
| trainbfg | 0.0491 | 0.0353 | 0.2371 | 0.3143 |
| trainrp | 0.1424 | 0.1225 | 0.2724 | 0.3284 |
| trainlm | 0.0194 | 0.0147 | 0.2815 | 0.2984 |

It should be noted that careful attention must be devoted to the application of neural networks, since an automatic application of the neural network may lead to misleading predictions and exaggeratedly large computational time. Thus, a contribution of this research is to improve the method of identifying the appropriate neural network structure. The mean squared prediction error criterion is proposed in this study to ensure that the identification of a network structure provides a reliable prediction scheme. In addition, this method uses the ensemble prediction concept that consists on generating members of ensemble by using different initial conditions and selecting the best representation of the population central tendency as the ensemble prediction.

## 5 METHODOLOGY

The conventional approach to obtain the activity coefficients in liquid solutions requires vapor-liquid equilibrium experiments. The main purpose of this research is to predict the activity coefficients without experimental data, since in practice experimentation is extremely expensive and time consuming. The proposed approach is possible because there is a large experimental equilibrium data set that can be used to train a neural network to recognize the relation among functional groups interactions and the Margules equation parameters (Sorensen and Arlt, 1979).

### 5.1 ANN Method Description

The entertained methodology in this research is based on decomposing the chemical compounds of a mixture into its functional groups, identifying the required interactions among functional groups, and training a neural network to predict the activity coefficients (see Figure 4). The four-suffix Margules equation has been used as base method for calculating the activity coefficients. Two MatLab programs were developed to perform the tasks required to apply this methodology. A description of the programs and the MatLab code is included in Appendix C. Figure 4 shows the steps of this methodology.


Figure 4. Methodology for Activity Coefficients Prediction with ANN

## Step 1: Experimental Data

The vapor-liquid equilibrium data used in this study are limited to the systems of binary mixtures containing several equilibrium data points. Nine hundred and twenty one (921) binary systems were used to create the information matrix and train a neural network. The sample size (921) was limited because of the availability of experimental data systems and because of required computational time. The experimental data were entered into a spreadsheet to be used by the MatLab program.

## Step 2: Decompose Molecules in Functional Groups and Determine Functional

## Groups Interactions

The functional groups used in this work were introduced by Wu and Sandler (1991) and are based on quantum mechanics calculations. The list of the functional
groups is presented in Appendix B. Figure 5 shows a symbolic representation of two molecules. It is assumed that the first and second molecules contain 4 and 3 functional groups, respectively. Figure 5 also shows all possible interactions $(2 \times 4 \times 3=24)$ among the functional groups.


Molecule 1


Molecule 2

| Interactions 1-2 |  | Interactions 2-1 |  |
| :---: | :---: | :---: | :---: |
| AE | CE | EA | FC |
| AF | CF | EB | FD |
| AG | CG | EC | GA |
| BE | DE | ED | GB |
| BF | DF | FA | GC |
| BG | DG | FB | GD |

Figure 5. Functional groups decomposition and interactions
Molecule 1 is composed of 4 functional groups and molecule 2 is composed of 3 functional groups. The total amount of possible functional groups interactions is 12 for each molecule.

## Step 3: Calculate the Experimental Activity Coefficients and the Margules Constants

The experimental activity coefficients are calculated from the vapor-liquid experimental data using the modified Raoult's law and the Antoine equation (Smith et al., 1996). That is, for the $i^{\text {th }}$ component in the solution:

$$
\begin{equation*}
y_{i} P=x_{i} \gamma_{i} P_{i}^{s a t} \quad \text { and } \quad \log P_{i}^{s a t}=A^{\prime}-\frac{B^{\prime}}{t-C^{\prime}} \tag{25}
\end{equation*}
$$

where, $y_{i}$ is the vapor-phase mole fraction, $P$ is the pressure of the system, $x_{i}$ is the liquid-phase mole fraction, $\gamma_{i}$ is the activity coefficient, $P_{i}^{\text {sat }}$ is the vapor pressure in mm $\mathrm{Hg}, A^{\prime}, B^{\prime}$ and $C^{\prime}$ are the Antoine constants and $t$ is the temperature of the system in degree Celsius.

The Margules constants were estimated for each of the experimental data systems using a quasi-Newton method. The objective function consisted on minimizing the sum of squared errors (SSE). The problem formulation was to find the Margules parameters such that:

$$
\begin{equation*}
\min \operatorname{SSE}\left(\hat{\gamma}_{i}\right)=\sum_{i=1}^{m}\left(\hat{\gamma}_{i}-\gamma_{i}\right)^{2} \tag{26}
\end{equation*}
$$

where $\gamma_{i}$ is the experimental value and $\hat{\gamma}_{i}$ is the predicted value calculated using the Margules equations (10) and (11).

## Step 4: Create the Experimental Data Information Matrix

The vapor-liquid equilibrium experimental data for each system was organized in columns and rows within a three dimensional matrix called the experimental data information matrix. The data in each row of the experimental data information matrix belong to one of the compounds of a binary system. Thus, every two rows of data belong to the experimental data of one binary system. The columns contain the information that belongs to the functional groups interactions. The columns are expanded tridimensionally into eight columns of data each containing the information of a functional group interaction (See Figure 6).


Figure 6. Experimental Data Information Matrix
Each interaction column represents eight columns with experimental data information. Note that the interactions are not sequentially ordered since the program position the information as it appears in the experimental data.

The first column of a group of eight columns within the experimental data information matrix contains the chemical interaction number between the $h$ and $k$ functional groups. The interaction number $\left(N_{h, k}\right)$ is computed by using the following equation:

$$
\begin{equation*}
N_{h, k}=g(h-1)+k \tag{27}
\end{equation*}
$$

where, $g$ is the total number of selected functional groups, $h$ and $k$ are the numbers associated to the first and the second functional groups, respectively. For instance, this study includes a total of 186 functional groups and the interaction number between the second and fourth functional groups can be computed as follows:

$$
N_{2,4}=186(2-1)+4=190
$$

In a similar fashion, the interaction number between the fourth and second functional group would be:

$$
N_{4,2}=186(4-1)+2=560
$$

The remaining seven columns from a columns group are used to save the following parameters: system temperature, system pressure, functional groups quantities, functional groups molecular weights, and functional groups mole fractions. Thus, any interaction between a functional group and itself is not included in the neural network training because it is expected to follow an ideal behavior and thus would have no contribution to the activity coefficient.

## Step 5: System of Interest

The data from the system of interest is entered into a spreadsheet, similar to that used for the experimental data, to be used by the MatLab program.

## Step 6: Determine the Functional Groups and Functional Groups Interactions for the

## System of Interest

The molecules from the system of interest are decomposed into their respective functional groups and the functional group interactions are determined as described in step 2. The data from the system of interest are arranged into an information matrix the same way as the experimental data.

## Step 5: Extract Necessary Data from the Experimental Data Matrix

The next step is to extract the required data from the experimental data information matrix. Searching techniques are used to identify the columns of the
experimental data information matrix that contains any of the functional group interactions of interest to create the training patterns. The selected information is called the reduced experimental data information matrix and is used to train a neural network and finally the optimal weights are used to predict the Margules equation parameters. Then, the four-suffix Margules equation is used to calculate the activity coefficients.

It should be noted that the proposed approach develops a model using only the required interactions with the purpose of reducing the computational effort and increase prediction capability.

## Step 6: Create Training Matrices

The training patterns of the neural networks are formed by the input and output vectors. In this study, the input vector, $\boldsymbol{P}$, includes the following variables: system temperature, system pressure, and the proportions of the functional groups interactions. The target, $\boldsymbol{T}$, of this prediction scheme contains the observed Margules equation parameters that are computed using experimental data. Thus the training patterns can be expressed as follows:

$$
\begin{equation*}
P=\left[t, p, \eta_{1,1}^{i} \cdots \eta_{h, k}^{i} \cdots \eta_{H, K}^{i}\right] \quad \text { and } \quad T=\left[A_{M}, B_{M}, C_{M}\right] \quad i=1,2, \ldots, m \tag{28}
\end{equation*}
$$

where, $t$ and $p$ are the temperature and pressure of the system, respectively; $m$ is the total number of rows of the reduced experimental data information matrix, the upper and lower supercripts corresponds to the $i^{\text {th }}$ row, and the subcripts corresponds to the $h^{\text {th }}$ functional group, and the $k^{\text {th }}$ functional group, respectively. The functional group $h$ belongs to the compound in the $i^{\text {th }}$ row and the functional group $k$ belongs to other compound in that mixture. $H$ and $K$ are the total number of functional groups, respectively in the first and
second compounds of the mixture. The $\eta_{h, k}^{i}$ is the amount of interactions between a functional group $h$ and $k$ divided by the total amount of possible interactions between the functional groups present in the mixture.

$$
\begin{equation*}
\eta_{h, k}^{i}=\frac{q_{h}^{i} \times q_{k}^{j}}{\sum_{h=1}^{H} \sum_{k=1}^{K} q_{h}^{i} \times q_{k}^{j}+\sum_{k=1}^{K} \sum_{h=1}^{H} q_{k}^{j} \times q_{h}^{i}} \tag{29}
\end{equation*}
$$

where, $q_{h}^{i}$ is the amount of functional groups in the $\mathrm{i}^{\text {th }}$ molecule and $q_{k}^{j}$ is the amount of functional groups in the $\mathrm{j}^{\text {th }}$ molecule.

## Step 7: Train the Neural Network

A systematic method is introduced to identify the neural network structure for modeling the non-linear behavior between the functional groups interactions and the Margules equation parameters. The neural networks with more than two layers were discarded since those networks over-parameterize the learning process causing reduction of skill prediction capability. On the other hand, a neural network composed with a single layer was not used because it does not have the capability of modeling nonlinear relationships. Therefore, the selected general structure included two layers, the hidden and the output layer (Figure 1).

A searching procedure was implemented to identify the minimum number of neurons in the hidden layer and the type of transfer function that minimizes the mean squared prediction error. The suggested identification procedure consists on selecting a transfer function and then varying the number of neurons in the hidden layer while measuring prediction accuracy by the mean squared prediction errors (mspe). This
process was repeated for three different transfer functions and varying the number of neuron from 1 to 5 in the hidden layer. Finally, the structure of the neural network is selected such that the mspe is minimized. It should be noted that the prediction was done with data that were not used for training. To perform this identification procedure, the data were split in two equal parts. The first part of the data was used to perform training and the second part was used to predict the Margules parameters. The mean squared prediction errors were calculated between the known experimental Margules parameters and the predicted values with the neural network. The mean squared prediction errors were computed as follows:

$$
\begin{equation*}
m s p e=\frac{1}{9} \sum_{i=1}^{m}\left[\left(\hat{A}_{M i}-A_{M i}\right)+\left(\hat{B}_{M i}-B_{M i}\right)+\left(\hat{C}_{M i}-C_{M i}\right)\right]^{2} \tag{30}
\end{equation*}
$$

where, $\hat{A}_{M i}, \hat{B}_{M i}$ and $\hat{C}_{M i}$ are the predicted Margules parameters, $A_{M i}, B_{M i}$ and $C_{M i}$ are the observed Margules parameters and were obtained from the experimental data, and $m$ is the number of data rows of the reduced experimental data information matrix used to predict the Margules parameters.

Three different transfer functions (TF) combinations for the neural network structure were explored in this research:

- purelin-purelin combination: a linear TF used in both, the hidden and output layers.
- logsig-purelin combination: a log-sigmoid TF in the hidden layer and a linear TF in the output layer.
- tansig-purelin combination: a hyperbolic tangent TF in the hidden layer and a linear TF in the output layer.

The mathematical representation of the three different TF is the following:

$$
\begin{equation*}
\text { Linear function: } f_{1}(n)=n=w p+b \tag{31}
\end{equation*}
$$

Log-sigmoidal function: $f_{2}(n)=\frac{1}{1+e^{-n}}$
Hyperbolic tangent function: $f_{3}(n)=\frac{e^{n}-e^{-n}}{e^{n}+e^{-n}}$
where, $n$ represents the net input into the network, $w$ is the weight matrix, and $b$ is the bias vector.

Thus, the structures of the neural network change depending on the natural relationship of the available data. The minimum mspe criterion was used to identify the appropriate transfer functions and the number of neurons in the hidden layer. The best performance was accomplished with a log-sigmoidal TF in the hidden layer, and a linear TF in the output layer. The number of neurons in the hidden layer varies for every case, depending on the mspe values. Once the optimal neural network is determined the network is trained with the LM algorithm using the training patterns from the reduced experimental data information matrix.

## Step 8: Predict the Margules Equation Parameters

The input vector for prediction is constructed with the system of interest data following equation (28). Then, the next step is to predict the Margules parameters with the trained ANN and the input vector constructed with the system of interest data. It was observed that, even though the TF and the optimum number of neurons were determined, the
outputs of the ANN provide different prediction values. This is due to the fact that the selected initial point to train the ANN is different every time the training is performed and consequently it may converge to a different local minimum. Thus, the ensemble prediction strategy was used to derive consistent prediction values. A searching process was designed to select the initial point that minimizes the mspe and perform prediction. The neural network was trained nine times with a different initial point and each time a new member of ensemble prediction was obtained. Finally, the Margules equation parameters were obtained by computing the trim mean based on $20 \%$ data elimination from the ensemble members. In this study just nine members of the ensemble population were generated because of computational effort limitations.

## Step 9: Calculate $\gamma$ using the Margules Equation

Once the Margules parameters are obtained, the activity coefficients are calculated using the four-suffix Margules equations as shown in equations (10) and (11).

In this study, a feedforward ANN was trained to predict the Margules parameters to calculate the activity coefficients. It was shown that it is possible to combine the interactions of the functional groups from a mixture and reasonable prediction of activity coefficients can be obtained under the framework of the artificial neural networks. The accuracy of the prediction tool is illustrated by comparing the neural network approach with the conventional functional groups contribution procedure UNIFAC.

### 5.2 Limitation of the Proposed Methodology

The proposed methodology is limited to estimate activity coefficients for binary liquid mixtures. A list of the DECHEMA database books is presented in Table 3. The
selected 921 systems used to build the experimental database are limited to alcohols, phenols, aldehydes, ketones and ethers. In the case of a system of interest is out of the mentioned compound families it is possible that all the interactions of the system may not be available and consequently the ANN method will provide either no results or a poor estimation of the activity coefficients. Thus, an expansion of the experimental database built during this work is recommended to include a wider range of compound families and functional group interactions.

Table 3. DECHEMA Chemistry Database

| Part | Title | ISBN | Pages | Published | Number of Systems |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | Aqueous-Organic Systems | 3-926959-30-4 | 750 | 1991 | 7 |
| 1a | Supplement 1 | 3-926959-90-8 | 750 | 1998 | 0 |
| 1b | Supplement 2 | 3-921567-91-2 | 658 | 1988 | 0 |
| 2a | Alcohols | 3-921567-62-9 | 750 | 1986 | 189 |
| 2b | Alcohols and Phenols | 3-926959-18-5 | 620 | 1990 | 147 |
| 2c | Alcohols Supplement 1 | 3-921567-29-7 | 730 | 2001 | 197 |
| 2d | Alcohols and Phenols Supplement 2 | 3-921567-43-2 | 830 | 1982 | 0 |
| 2 e | Alcohols and Phenols Supplement 3 | 3-921567-92-0 | 650 | 1988 | 96 |
| 2 f | Alcohols and Phenols Supplement 4 | 3-926959-16-9 | 716 | 1990 | 76 |
| 3/4 | Aldehydes, Ketones, Ethers | 3-921567-14-9 | 650 | 1979 | 113 |
| 3 a | Aldehydes, Supplement 1 | 3-921567-93-9 | 280 | 1993 | 0 |
| 3 b | Ketones, Supplement 1 | 3-921567-44-4 | 750 | 1993 | 0 |
| 4 a | Ethers, Supplement 1 | 3-921567-86-6 | 534 | 1996 | 0 |
| 4b | Ethers, Supplement 2 | 3-926959-98-3 | 476 | 1999 | 0 |
| 5 | Carboxylic Acids, Anhydrides, Esters | 3-921567-20-3 | 750 | 2001 | 0 |
| 5a | Carboxylic Acids, Anhydrides, Supplement 1 | 3-89746-040-8 | 500 | 2002 | 0 |
| 5b | Esters, Supplement 2 | 3-89746-041-6 | 600 | 2002 | 0 |
| 6 a | Aliphatic Hydrocarbons $\mathrm{C}_{4}-\mathrm{C}_{6}$ | 3-926959-42-8 | 716 | 1997 | 0 |
| 6 b | Aliphatic Hydrocarbons $\mathrm{C}_{7}-\mathrm{C}_{18}$ | 3-926959-87-8 | 540 | 1997 | 0 |
| 6c | Aliphatic Hydrocarbons Supplement 1 | 3-921567-51-3 | 689 | 1983 | 0 |
| 6d+e | Aliphatic Hydrocarbons $\mathrm{C}_{4}-\mathrm{C}_{30}$ | 3-89746-007-6 | 1011 | 1999 | 0 |
| 7 | Aromatic Hydrocarbons | 3-926959-88-6 | 600 | 1997 | 77 |


| Part | Title | ISBN | Pages | Published | Number of <br> Systems |
| :---: | :--- | :---: | :---: | :---: | :---: |
| $7 \mathrm{a} / 7 \mathrm{~b}$ | Supplement 1 | $3-89746-012-2$ | 789 | 2000 | 19 |
| 8 | Halogen, Nitrogen, Sulfur and other <br> Compounds | $3-921567-24-6$ | 600 | 1984 | 0 |
| 8 a | Halogen, Nitrogen, Sulfur and other <br> Compounds, Supplement 1 | $3-89746-028-9$ | 600 | 2001 | 0 |

Because the activity coefficient is derived from the molar partial Gibbs free energy it has two thermodynamic contributions, the enthalpic and the entropic, as defined by the Gibbs energy,

$$
\begin{equation*}
G_{i}=H_{i}-T S_{i} \tag{34}
\end{equation*}
$$

where, $G_{i}$ is the Gibbs energy, $H_{i}$ is the enthalpy and $S_{i}$ is the entropy for the $i^{\text {th }}$ compound in a mixture. The enthalpic contribution to the activity coefficient is associated to the molecular interactions while the entropic contribution is associated to the molecules size and geometry. It is known that the Margules equation takes into consideration only the enthalpic contribution to the activity coefficient while the UNIFAC is based on the UNIQUAC equation, which takes into account both the enthalpic and the entropic contributions to the activity coefficient. It is expected that the UNIFAC method will better predict the activity coefficient for a system where the entropic contribution domains over the enthalpic contribution due to large molecular size. The ANN method should be able to use other thermodynamic models such as NRTL and UNIQUAC, to increase its capability of predicting the activity coefficient for systems with large molecular size.

## 6 NUMERICAL EXAMPLE

The purpose of this example is to illustrate a step-by-step calculation of predicting the activity coefficients for a binary system. An arbitrary binary system was selected and corresponds to a mixture of 2,4-dimethylpentane and benzene (Ohe, 1989). Table 4 shows the vapor-liquid equilibrium data for the system. Table 5 shows the Antoine constants of the selected system and eight steps were designed to predict the activity coefficients.

Table 4. VLE Data for the system 2,4-dimethylpentane (1) + benzene (2)

| $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{y}_{\mathbf{1}}$ | Temperature <br> $\left({ }^{\circ} \mathbf{C}\right)$ | Pressure <br> $(\mathbf{m m H g})$ |
| :---: | :---: | :---: | :---: |
| 0.078 | 0.125 | 77.3 | 757 |
| 0.106 | 0.164 | 77.0 | 757 |
| 0.140 | 0.195 | 76.5 | 757 |
| 0.152 | 0.219 | 76.3 | 757 |
| 0.192 | 0.242 | 76.1 | 757 |
| 0.224 | 0.268 | 75.9 | 757 |
| 0.251 | 0.292 | 75.7 | 757 |
| 0.281 | 0.318 | 75.5 | 757 |
| 0.335 | 0.357 | 75.4 | 757 |
| 0.378 | 0.392 | 75.4 | 757 |
| 0.432 | 0.432 | 75.2 | 757 |
| 0.480 | 0.469 | 75.4 | 757 |
| 0.525 | 0.504 | 75.3 | 757 |
| 0.572 | 0.541 | 75.5 | 757 |
| 0.616 | 0.576 | 75.5 | 757 |
| 0.662 | 0.614 | 75.9 | 757 |
| 0.700 | 0.652 | 76.1 | 757 |
| 0.74 | 0.686 | 76.3 | 757 |
| 0.785 | 0.731 | 76.6 | 757 |
| 0.839 | 0.785 | 77.2 | 757 |

Table 5. Antoine Constants

| Component | A | B | C |
| :---: | :---: | :---: | :---: |
| 1 | 6.82621 | 1192.041 | 221.634 |
| 2 | 6.90565 | 1211.033 | 220.790 |

Step 1. Structural formula. The structural formula for each compound of the mixture is written to facilitate the identification of the functional groups. Figure 7 shows the structural formula for each chemical compound.


2, 4-Dimethylpentane


Benzene

Figure 7. Chemical Structures

Step 2. Identifying chemical structures functional groups. The number of functional groups associated to each compound was identified. Table 6 sumarizes the functional groups associated to each compound, which are:

- 2,4-Dimethylpentane has two units of the functional group number $2,(\mathrm{CH})$; one unit of the functional group number $3,\left(\mathrm{CH}_{2}\right)$; and four units of the functional group number 4, $\left(\mathrm{CH}_{3}\right)$. Appendix B shows the enumeration of the functional groups.
- Benzene has six (6) units of the functional group number 135, (aCH).

Table 6. Compounds Functional Groups

| Compound | Functional Groups and Quantities |  |  |
| :---: | :---: | :---: | :---: |
| 2,4-Dimethylpentane | $2 \times \mathrm{G} 2$ | $1 \times \mathrm{G} 3$ | $4 \times \mathrm{G} 4$ |
| Benzene | $6 \times \mathrm{G} 135$ |  |  |

Step 3. Identify functional groups interactions. The functional group interaction numbers are calculated and arranged into the system of interest information matrix. Calculations are obtained by using equation (27) and Table 7 shows the functional group interactions for the system 2, 4-dimethylpentane (1) + benzene (2).

Table 7. System Interactions

| Interactions 1-2 | Interaction <br> Number | Interactions 2-1 | Interaction <br> Number |
| :---: | :---: | :---: | :---: |
| G2 G135 | 321 | G135 G2 | 24926 |
| G3 G135 | 507 | G135 G3 | 24927 |
| G4 G135 | 693 | G135 G4 | 24928 |

The functional groups numbers were assigned using Appendix B.
Step 4. Develop the information matrix. The system of interest information matrix is similar to the experimental data information matrix. The data is arranged in a tridimensional matrix as presented in Figure 8.


Figure 8. System Information Matrix
This system information matrix was generated by the MatLab program NNvsUNIFAC.m and is used to create the input matrix required to predict the Magurles parameters with the trained neural network.

The data contained for each functional group interaction along the $3^{\text {rd }}$ dimension of the system information matrix are presented in Table 8.

Table 8. System Functional Group Interactions Data

| Int\#1 | t | p | GF1 | GF2 | wGF1 | wGF2 | Ones |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 321 | 76.005 | 757 | 2 | 6 | 26 | 78 | 1 |
| 24926 | 76.005 | 757 | 6 | 2 | 78 | 26 | 1 |
| Int\#2 | t | p | GF1 | GF2 | wGF1 | wGF2 | Ones |
| 507 | 76.005 | 757 | 1 | 6 | 14 | 78 | 1 |
| 24927 | 76.005 | 757 | 6 | 1 | 78 | 14 | 1 |
| Int\#3 | t | p | GF1 | GF2 | wGF1 | wGF2 | Ones |
| 693 | 76.005 | 757 | 4 | 6 | 60 | 78 | 1 |
| 24928 | 76.005 | 757 | 6 | 4 | 78 | 60 | 1 |

The system information matrix is used to search within the experimental data information matrix for all systems that contain at least one of the functional group interactions of interest and build a reduce experimental data information matrix. The reduced experimental data information matrix consists of all systems within the experimental data, whose functional group interactions match at least one of the interactions of interest. The reduced experimental data information matrix was used to train the neural network.

Step 5. Generate the training patterns. The training patterns are obtained from the reduced experimental data information matrix and are organized to perform the neural network-training task following equation (28). All available training patterns for the system of interest were arranged using the reduced experimental data information matrix with 165 rows and 208 columns, i.e., there were 165 systems out of the 921 systems within the experimental data information matrix that contain at least one of the interactions of interest.

Step 6. Train the neural network. The neural network is trained with the reduced experimental data information matrix. The inputs patterns include the variables described by equation (28). The target includes the Margules parameters as shown by equation 28. The structure of the network includes a log-sigmoid transfer function in the hidden layer and a linear transfer function in the output layer. The ANN was trained with nine different initial points and the optimum initial point is the one that minimizes the mspe. Figure 9 shows the training process of the MatLab software. The horizontal axis shows the number of epochs, which represents the number of time the training patterns are presented to the ANN and the vertical axis represents the mspe.


Figure 9. Neural Network Training

Step 7. Predicting the Margules parameters. The ensemble prediction technique was use to generate the nine ensemble members and the trim mean with $20 \%$ data elimination was used to calculate the predicted value for the Margules parameters. Table 9 shows the members of the ensemble prediction. Note that within the nine predicted values for the Margules parameters, there are outliers that deviate considerably from the other values. The ensemble prediction method is capable of eliminating those outliers from the calculation of the predicted Margules parameters giving more consistent results (see Table 10).

Table 9. Predicted Margules parameters values

| Predicted <br> Value | $\mathbf{A}_{\mathbf{M}}$ | $\mathbf{B}_{\mathbf{M}}$ | $\mathbf{C}_{\mathbf{M}}$ |
| :---: | :---: | :---: | :---: |
| 1 | 0.5958 | 0.1204 | -0.0262 |
| 2 | 0.5301 | 0.0993 | 0.0394 |
| 3 | 0.9227 | -0.0641 | 0.0164 |
| 4 | 0.9226 | -0.0641 | 0.0163 |
| 5 | 0.5253 | -0.1985 | -0.1219 |
| 6 | -1.0525 | -1.3918 | -1.7782 |
| 7 | 0.5188 | 0.0518 | 0.1006 |
| 8 | 0.9453 | -0.2725 | -0.0657 |
| 9 | 0.5453 | 0.0926 | -0.0054 |

Table 10. Predicted Margules parameters values with $20 \%$ data elimination

|  | $\mathbf{A}_{\mathbf{M}}$ | $\mathbf{B}_{\mathbf{M}}$ | $\mathbf{C}_{\mathbf{M}}$ |
| :---: | :---: | :---: | :---: |
|  | 0.5253 | -0.1985 | -0.0657 |
|  | 0.5301 | -0.0641 | -0.0262 |
|  | 0.5453 | -0.0641 | -0.0054 |
|  | 0.5958 | 0.0518 | 0.0163 |
|  | 0.9226 | 0.0926 | 0.0164 |
| Average | $\mathbf{0 . 6 2 3 8}$ | $\mathbf{- 0 . 0 3 6 5}$ | $\mathbf{- 0 . 0 1 2 9}$ |

Step 8. Predicting the activity coefficients using Margules equation. The predicted Margules parameters are used to calculate the activity coefficients for both
components of the mixture. Figure 10 and Table 11 shows the results of the predicted activity coefficients using the ANN method. This table also shows the activity coefficients predicted by the UNIFAC method and the observed activity coefficients obtained by the modified Raoult's Law and the Antoine equation.

Table 11. Activity Coefficients Estimation

| Mole fraction |  | Activity Coefficient Estimated from Experimental Data |  | Activity Coefficient Estimated from Neural Networks (using functional groups) |  | Activity Coefficient Estimated from UNIFAC (using functional groups) |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $x_{1}$ | $x_{2}$ | $\gamma_{1}$ | $\gamma_{2}$ | $\gamma_{1}$ | $\gamma_{2}$ | $\gamma_{1}$ | $\gamma_{2}$ |
| 0.078 | 0.922 | 1.7593 | 1.0313 | 1.7276 | 1.0041 | 1.5491 | 1.0054 |
| 0.106 | 0.894 | 1.7142 | 1.0258 | 1.6693 | 1.0076 | 1.4863 | 1.0097 |
| 0.140 | 0.860 | 1.5672 | 1.0431 | 1.6034 | 1.0133 | 1.4203 | 1.0162 |
| 0.152 | 0.848 | 1.6312 | 1.0328 | 1.5814 | 1.0157 | 1.3992 | 1.0188 |
| 0.192 | 0.808 | 1.4359 | 1.0587 | 1.5122 | 1.0252 | 1.3359 | 1.0287 |
| 0.224 | 0.776 | 1.3714 | 1.0713 | 1.4614 | 1.0344 | 1.2925 | 1.0377 |
| 0.251 | 0.749 | 1.3418 | 1.0803 | 1.4215 | 1.0434 | 1.2601 | 1.0460 |
| 0.281 | 0.719 | 1.3134 | 1.0910 | 1.3801 | 1.0546 | 1.2280 | 1.0559 |
| 0.335 | 0.665 | 1.2407 | 1.1157 | 1.3130 | 1.0783 | 1.1789 | 1.0753 |
| 0.378 | 0.622 | 1.2073 | 1.1279 | 1.2658 | 1.1004 | 1.1467 | 1.0919 |
| 0.432 | 0.568 | 1.1715 | 1.1612 | 1.2136 | 1.1323 | 1.1133 | 1.1142 |
| 0.480 | 0.520 | 1.1375 | 1.1783 | 1.1734 | 1.1648 | 1.0889 | 1.1349 |
| 0.525 | 0.475 | 1.1211 | 1.2087 | 1.1404 | 1.1988 | 1.0700 | 1.1552 |
| 0.572 | 0.428 | 1.0977 | 1.2335 | 1.1105 | 1.2381 | 1.0536 | 1.1769 |
| 0.616 | 0.384 | 1.0852 | 1.2700 | 1.0865 | 1.2784 | 1.0409 | 1.1979 |
| 0.662 | 0.338 | 1.0632 | 1.2970 | 1.0650 | 1.3243 | 1.0300 | 1.2200 |
| 0.700 | 0.300 | 1.0611 | 1.3091 | 1.0500 | 1.3652 | 1.0227 | 1.2387 |
| 0.740 | 0.260 | 1.0495 | 1.3543 | 1.0366 | 1.4110 | 1.0163 | 1.2585 |
| 0.785 | 0.215 | 1.0446 | 1.3898 | 1.0243 | 1.4661 | 1.0106 | 1.2810 |
| 0.839 | 0.161 | 1.0303 | 1.4557 | 1.0131 | 1.5369 | 1.0056 | 1.3079 |

This table presents the final results for the activity coefficients predicted by the ANN method in addition to the results from UNIFAC and the activity coefficients calculated from the experimental vapor-liquid equilibrium data for the system: 2, 4 - dimethylpentane (1) + benzene (2).


Figure 10. Comparison of activity coefficients for system:
2,4-dimethylpentane (1) + benzene (2)

This figure shows a graphical comparison for the activity coefficients $\gamma_{1}$ and $\gamma_{2}$ between the experimental values, predicted by ANN method and predicted by UNIFAC method. The prediction performance for both ANN and UNIFAC methods is about the same.

One of the well-known measurements of prediction accuracy is the mean absolute error (MAE), which is defined as follows:

$$
\begin{equation*}
M A E_{i}=\frac{1}{n} \sum_{j=1}^{n}\left|\gamma_{i, j}-\hat{\gamma}_{i, j}\right| \tag{35}
\end{equation*}
$$

where, $n$ is the number of concentration levels. $M A E_{i}$ is the mean absolute error for the $i^{\text {th }}$ compound, $\gamma_{i, j}$ and $\hat{\gamma}_{i, j}$ are the activity coefficients obtained from experimental data and from the neural network methodology, respectively. Subscript $j$ refers to the applied concentration and the subscript $i$ represents the chemical compound. The $M A E$ for the activity coefficients predicted by the ANN and UNIFAC methods for the system
presented above are shown in Table 12. The ANN method shows an improvement of the activity coefficients prediction over the UNIFAC method, as also shown in Table 12.

Table 12. Mean Absolute Error for the System: 2, 4-dimethylpentane (1) + benzene (2)

| Liquid Mole <br> fraction |  | Absolute Prediction <br> Errors for <br> Neural Networks |  | Absolute Prediction <br> Errors for <br> UNIFAC |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\boldsymbol{x}_{1}$ | $x_{2}$ | $\gamma_{1}$ Error | $\gamma_{2}$ Error | $\gamma_{1}$ Error | $\gamma_{2}$ Error |
| 0.078 | 0.922 | 0.0317 | 0.0271 | 0.2102 | 0.0259 |
| 0.106 | 0.894 | 0.0449 | 0.0181 | 0.2279 | 0.0161 |
| 0.140 | 0.860 | 0.0362 | 0.0297 | 0.1469 | 0.0269 |
| 0.152 | 0.848 | 0.0498 | 0.0170 | 0.2320 | 0.0140 |
| 0.192 | 0.808 | 0.0763 | 0.0333 | 0.1000 | 0.0300 |
| 0.224 | 0.776 | 0.0900 | 0.0367 | 0.0789 | 0.0336 |
| 0.251 | 0.749 | 0.0797 | 0.0368 | 0.0817 | 0.0343 |
| 0.281 | 0.719 | 0.0667 | 0.0362 | 0.0854 | 0.0351 |
| 0.335 | 0.665 | 0.0723 | 0.0372 | 0.0618 | 0.0404 |
| 0.378 | 0.622 | 0.0585 | 0.0273 | 0.0606 | 0.0360 |
| 0.432 | 0.568 | 0.0421 | 0.0287 | 0.0582 | 0.0470 |
| 0.480 | 0.520 | 0.0359 | 0.0133 | 0.0486 | 0.0434 |
| 0.525 | 0.475 | 0.0193 | 0.0097 | 0.0511 | 0.0535 |
| 0.572 | 0.428 | 0.0128 | 0.0048 | 0.0441 | 0.0566 |
| 0.616 | 0.384 | 0.0013 | 0.0086 | 0.0443 | 0.0721 |
| 0.662 | 0.338 | 0.0018 | 0.0275 | 0.0332 | 0.0770 |
| 0.700 | 0.300 | 0.0111 | 0.0563 | 0.0384 | 0.0704 |
| 0.740 | 0.260 | 0.0129 | 0.0569 | 0.0332 | 0.0958 |
| 0.785 | 0.215 | 0.0203 | 0.0764 | 0.0340 | 0.1088 |
| 0.839 | 0.161 | 0.0172 | 0.0814 | 0.0247 | 0.1478 |
| Mean Absolute | 0.0390 | 0.0331 | 0.0848 | 0.0531 |  |
| Error |  |  |  |  |  |

This table presents the absolute prediction errors for the activity coefficients predicted by the ANN and UNIFAC methods. The mean absolute error is presented at the end of the table.

## 7 COMPARISON BETWEEN ANN AND UNIFAC

Initially, we tried to find a data set from a source other than the DECHEMA database to perform a fair comparison between the ANN and UNIFAC methods; however, the identified number of systems was very small. Nineteen systems were selected to perform a comparison between the ANN method and the UNIFAC method. Nine out of nineteen systems were obtained from Ohe (1989) and the other ten systems were taken directly from DECHEMA database (Sorensen and Arlt, 1979). Although the information comes from different sources it was noticed that all of the nineteen systems are available in the complete DECHEMA database and the UNIFAC method was developed using all of the 8,600 systems available in the complete DECHEMA database (Gmehling, 2003). The ANN method was developed using only 921 systems from DECHEMA. The activity coefficients, $\gamma_{1}$ and $\gamma_{2}$ were predicted for the nineteen systems using the ANN and the UNIFAC methods (see Appendix A). Appendix A also shows graphically the performance comparison between the ANN and UNIFAC methods for all nineteen systems. Appendix A figures show that the prediction capabilities of the considered methods are about the same.

The mean absolute errors (MAE) from the nineteen systems were used to measure the accuracy of the prediction methods. The MAE's do not follow a normal distribution due to the outliers' results as shown in Figure 11.


Figure 11. MAE Populations Boxplot
It is well known that the median is a better representation of the central tendency of the population when outliers are present. Thus, a non-parametric test was used to prove whether or not the median of the $M A E$ from the ANN method is smaller than the median of the MAE obtained from UNIFAC. The selected non-parametric test was the Mann-Whitney (Hayter, 1996) test. When predicting the activity coefficient $\gamma_{1}$, the medians of the $M A E$ from the ANN method and from UNIFAC show no significant difference at $95 \%$ confidence since the p-value was 0.6614 . The ANN method performance is slightly better, with a median of the MAE equal to 0.0483 while the median of the MAE for the UNIFAC method is equal to 0.0669 .

## Mann-Whitney Test and CI: MAE ANN1_M, MAE U1

```
N Median
MAE ANN1_M 19 0.04831
MAE U1 19 0.06691
Point estimate for ETA1-ETA2 is 0.00716
95.3 Percent CI for ETA1-ETA2 is (-0.02561,0.05846)
W = 386.0
Test of ETA1 = ETA2 vs. ETA1 not = ETA2 is significant at 0.6614
```

When predicting $\gamma_{2}$ the medians of the $M A E$ from the ANN method and from UNIFAC show no significant difference at $95 \%$ confidence since the p-value was 0.2933 . The ANN method performance is slightly better, with a median of the MAE equal to 0.0764 while the median of the $M A E$ for the UNIFAC method is equal to 0.0842 .

## Mann-Whitney Test and CI: MAE ANN2_M, MAE U2

```
MAF ANN2 M N N Median
MAE ANN2_M 19 0.0764
MAE U2 19 0.0842
Point estimate for ETA1-ETA2 is -0.0193
95.3 Percent CI for ETA1-ETA2 is (-0.0785,0.0308)
W = 334.0
Test of ETA1 = ETA2 vs. ETA1 not = ETA2 is significant at 0.2933
```

Even though, the ANN method performs a slightly better than the UNIFAC method, the improvement is not statistically significant. In summary, based on the nineteen systems studied, the performance of the ANN method is slightly better than the UNIFAC method. Table 13 summarizes the results for the mean absolute errors.

Table 13. Mean Absolute Errors for the Activity Coefficients

|  | Molecule 1 | Molecule 2 | Mean Absolute Prediction Errors for Neural Networks |  | Mean Absolute Prediction Errors for UNIFAC |  | セٌ¢¢ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  | $\gamma_{1}$ | $\gamma_{2}$ | $\gamma_{1}$ | $\gamma_{2}$ |  |
| 1 | acetone | methanol | 0.0155 | 0.0268 | 0.0112 | 0.0227 | 1 |
| 2 | methanol | 3-methylbutanol | 0.0227 | 0.0732 | 0.0066 | 0.0957 | 1 |
| 3 | acetone | ethanol | 0.0536 | 0.0438 | 0.0875 | 0.0405 | 1 |
| 4 | tetrachloromethane | 2-propanol | 0.1254 | 0.0919 | 0.0276 | 0.4035 | 1 |
| 5 | methanol | 1-propanol | 0.0311 | 0.0598 | 0.0825 | 0.0504 | 1 |
| 6 | methanol | 1-butanol | 0.0398 | 0.0764 | 0.0669 | 0.0642 | 1 |
| 7 | methyl acetate | methanol | 0.0138 | 0.0214 | 0.0333 | 0.0329 | 1 |
| 8 | acetone | benzene | 0.0273 | 0.0138 | 0.0412 | 0.0291 | 1 |
| 9 | acetone | hexane | 0.0320 | 0.0794 | 0.0725 | 0.0677 | 1 |
| 10 | acetone | toluene | 0.0454 | 0.0390 | 0.0421 | 0.0804 | 1 |
| 11 | 2,4-dimethyl pentane | benzene | 0.0390 | 0.0331 | 0.0848 | 0.0531 | 2 |
| 12 | cyclohexane | isopropyl alcohol | 0.2253 | 0.1311 | 0.1001 | 0.2922 | 2 |
| 13 | ethylcyclohexane | isopropyl alcohol | 0.3572 | 0.1501 | 0.0999 | 1.0492 | 2 |
| 14 | benzene | isopropyl alcohol | 0.1546 | 0.3573 | 0.0701 | 0.0842 | 2 |
| 15 | toluene | isopropyl alcohol | 0.0849 | 0.1542 | 0.0596 | 0.2226 | 2 |
| 16 | ethyl ether | acetone | 0.1240 | 0.1998 | 0.0971 | 0.2669 | 2 |
| 17 | acetone | isopropyl alcohol | 0.1585 | 0.3837 | 0.0938 | 0.4554 | 2 |
| 18 | isopropyl alcohol | ethyl acetate | 0.0483 | 0.0200 | 0.0355 | 0.0953 | 2 |
| 19 | chloroform | n-butyl alcohol | 0.2012 | 0.1355 | 0.0397 | 0.1548 | 2 |
| Average Median |  |  | 0.0947 | 0.1100 | 0.0606 | 0.1874 |  |
|  |  |  | 0.0483 | 0.0764 | 0.0669 | 0.0842 |  |

Sources: (1) Sorensen and Arlt (1979) (DECHEMA); (2) Ohe (1989)

This table presents the mean absolute errors for the activity coefficients for each of the nineteen systems studied. The mean absolute error is used to standardize the data and compare the prediction results populations.

The relative comparison between two prediction methods can be accomplished by using a skill score (SS) that relates the mean absolute prediction of the forecast methods.

The skill score is widely used in different fields (Wilks, 2006) and is defined as follows:

$$
\begin{equation*}
S S=\frac{A-A_{\text {ref }}}{A_{\text {perf }}-A_{\text {ref }}} \times 100 \tag{36}
\end{equation*}
$$

where, $A$ is a particular measure of accuracy of the method to be compared such as MAE, MSE or RMSE. $A_{\text {ref }}$ is the measure of accuracy of the reference method, $A_{\text {perf }}$ is the value of the accuracy measure that would be achieved by a perfect forecast and is equal to 0 when using $M S E$ or $M A E$ as accuracy measure.

The skill score is a positive value when the method of interest is better than the reference method and negative otherwise. The skill score based on the median of the MAE for the ANN method was $28 \%$ when predicting $\gamma_{1}$ and $9 \%$ when predicting $\gamma_{2}$.

## 8 CONCLUSIONS AND FUTURE WORK

A new methodology using artificial neural networks was designed to predict the activity coefficients based on the knowledge of the structural formula, temperature, pressure and liquid molar composition for the compounds in a mixture. The proposed methodology is a potential tool to estimate the activity coefficients of chemical compounds when experimental data are not available. The neural network method was compared to the UNIFAC method and it was found that the performance of the ANN method was slightly better for the nineteen studied systems.

The mean squared prediction error criterion was used to identify the appropriate structure of the feedforward artificial neural network. The introduced methodology basically consists of selecting a neural network structure for a single neuron in the hidden layer and then the number of neurons increases until the mean squared prediction error has been accomplished. Finally, the neural network structure that provides the minimum variance prediction with the least number of neurons is selected as the best neural network structure.

The neural network method exhibits a high variability in the results. However, the optimum initial point determination and ensemble prediction technique was able to stabilize the output of the neural network method and increase its prediction accuracy. A practical tool was developed as an alternative method that may be used to obtain a reliable prediction of activity coefficients for a given chemical mixture and the MatLab code is presented in Appendix C.

As future work, it is recommended to expand the experimental database to other compound families not included in this work in order to cover a wider range of functional group interactions. Also the ANN method should be trained with other thermodynamic models (i.e. Wilson, van Laar, NRTL and UNIQUAC) and the program should have the flexibility for the user to choose the thermodynamic model for predicting the activity coefficient. The program for the ANN method should be capable of measuring the contribution to the activity coefficient of each functional group interaction. A comparison between the ANN and UNIFAC methods to predict the activity coefficient at infinite dilution $\gamma^{\infty}$ should be performed.

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## Appendix A Graphical Comparison Between ANN and UNIFAC



Figure 12. System 1: Acetone (1) + Methanol (2) This system is included in the 921 systems compiled from DECHEMA. None of the prediction methods were able to predict the deviation peak of $\gamma_{2}$ at a low $x_{2}$ value

Table 14. Activity Coefficients Results for System 1

| Temp $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{1}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | Exp |
| 55 | 0.1046 | 1.6481 | 1.6532 | 1.6940 | 1.0085 | 1.0072 | 1.0016 |
| 55 | 0.1357 | 1.5833 | 1.5956 | 1.6200 | 1.0140 | 1.0121 | 1.0080 |
| 55 | 0.1452 | 1.5649 | 1.5789 | 1.5692 | 1.0160 | 1.0138 | 1.0260 |
| 55 | 0.1663 | 1.5260 | 1.5431 | 1.5768 | 1.0207 | 1.0181 | 1.0148 |
| 55 | 0.2173 | 1.4425 | 1.4637 | 1.4866 | 1.0344 | 1.0309 | 1.0266 |
| 55 | 0.2390 | 1.4110 | 1.4328 | 1.4525 | 1.0412 | 1.0375 | 1.0286 |
| 55 | 0.2787 | 1.3587 | 1.3803 | 1.3860 | 1.055 | 1.0511 | 1.0566 |
| 55 | 0.3579 | 1.2715 | 1.2895 | 1.2755 | 1.0882 | 1.0850 | 1.1023 |
| 55 | 0.4050 | 1.2285 | 1.2434 | 1.2346 | 1.1115 | 1.1096 | 1.1300 |
| 55 | 0.4480 | 1.1939 | 1.2058 | 1.2151 | 1.1353 | 1.1353 | 1.1396 |
| 55 | 0.5052 | 1.1540 | 1.1619 | 1.1576 | 1.1710 | 1.1743 | 1.1930 |
| 55 | 0.5432 | 1.1307 | 1.1362 | 1.1469 | 1.1976 | 1.2035 | 1.1995 |
| 55 | 0.6332 | 1.0844 | 1.0856 | 1.0940 | 1.2712 | 1.2844 | 1.2776 |
| 55 | 0.6538 | 1.0754 | 1.0759 | 1.0767 | 1.2905 | 1.3055 | 1.3277 |
| 55 | 0.6605 | 1.0726 | 1.0729 | 1.0741 | 1.2970 | 1.3125 | 1.3163 |
| 55 | 0.6945 | 1.0592 | 1.0586 | 1.0542 | 1.3318 | 1.3500 | 1.3731 |
| 55 | 0.7327 | 1.0458 | 1.0445 | 1.0375 | 1.3748 | 1.3958 | 1.4307 |
| 55 | 0.7525 | 1.0395 | 1.0380 | 1.0428 | 1.399 | 1.4210 | 1.4070 |
| 55 | 0.7752 | 1.0328 | 1.0313 | 1.0320 | 1.4283 | 1.4514 | 1.4841 |
| 55 | 0.9080 | 1.0059 | 1.0052 | 1.0099 | 1.6460 | 1.6632 | 1.6438 |
| 55 | 0.9088 | 1.0058 | 1.0051 | 1.0111 | 1.6476 | 1.6646 | 1.6545 |
| 55 | 0.9197 | 1.0045 | 1.0039 | 0.9969 | 1.6698 | 1.6850 | 1.9194 |
| 55 | 0.9448 | 1.0022 | 1.0019 | 1.0106 | 1.7242 | 1.7337 | 1.7461 |
|  |  |  |  |  |  |  |  |



Figure 13. System 2: Methanol (1) + 3-Methylbutanol
This system is included in the 921 systems compiled from DECHEMA.

Table 15. Activity Coefficients Results for System 2

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |  |
| 60 | 0.1 | 1.2252 | 1.2288 | 1.2251 | 1.0025 | 1.0013 | 0.9703 |  |
| 60 | 0.2 | 1.1717 | 1.1974 | 1.1926 | 1.0104 | 1.0060 | 0.9774 |  |
| 60 | 0.3 | 1.1247 | 1.1655 | 1.1586 | 1.0243 | 1.0151 | 0.9994 |  |
| 60 | 0.4 | 1.0853 | 1.1336 | 1.1253 | 1.0442 | 1.0305 | 1.0000 |  |
| 60 | 0.5 | 1.0540 | 1.1023 | 1.0853 | 1.0694 | 1.0545 | 1.2579 |  |
| 60 | 0.6 | 1.0306 | 1.0725 | 1.0653 | 1.0990 | 1.0908 | 1.0456 |  |
| 60 | 0.7 | 1.0147 | 1.0452 | 1.0401 | 1.1311 | 1.1445 | 1.0468 |  |
| 60 | 0.8 | 1.0053 | 1.0223 | 1.0228 | 1.1630 | 1.2238 | 1.1138 |  |
| 60 | 0.9 | 1.0010 | 1.0062 | 1.0003 | 1.1910 | 1.3408 | 1.0420 |  |



Figure 14. System 3: Acetone (1) + Ethanol (2) This system is included in the 921 systems compiled from DECHEMA.

Table 16. Activity Coefficients Results for System 3

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | exp |  |
| 40 | 0.025 | 1.8567 | 2.1767 | 2.0581 | 1.0005 | 1.0005 | 0.9954 |  |
| 40 | 0.050 | 1.7939 | 2.0896 | 1.9530 | 1.0018 | 1.0021 | 0.9957 |  |
| 40 | 0.075 | 1.7361 | 2.0085 | 1.8453 | 1.0040 | 1.0048 | 1.0025 |  |
| 40 | 0.100 | 1.6827 | 1.9330 | 1.7657 | 1.0070 | 1.0085 | 1.0129 |  |
| 40 | 0.150 | 1.5875 | 1.7968 | 1.6483 | 1.0154 | 1.0190 | 1.0366 |  |
| 40 | 0.200 | 1.5053 | 1.6782 | 1.5519 | 1.0269 | 1.0339 | 1.0530 |  |
| 40 | 0.250 | 1.4338 | 1.5747 | 1.4672 | 1.0415 | 1.0532 | 1.0741 |  |
| 40 | 0.300 | 1.3713 | 1.4842 | 1.3904 | 1.0592 | 1.0771 | 1.1013 |  |
| 40 | 0.400 | 1.2677 | 1.3358 | 1.2630 | 1.1050 | 1.1400 | 1.1733 |  |
| 40 | 0.500 | 1.1859 | 1.2226 | 1.1755 | 1.1670 | 1.2255 | 1.2583 |  |
| 40 | 0.600 | 1.1211 | 1.1375 | 1.1097 | 1.2502 | 1.3385 | 1.3565 |  |
| 40 | 0.700 | 1.0703 | 1.0754 | 1.0642 | 1.3627 | 1.4856 | 1.4615 |  |
| 40 | 0.800 | 1.0327 | 1.0330 | 1.0334 | 1.5177 | 1.6762 | 1.5654 |  |
| 40 | 0.900 | 1.0087 | 1.0082 | 1.0127 | 1.7361 | 1.9240 | 1.6764 |  |



Figure 15. System 4: Tetrachloromethane (1) + 2-Propanol (2) This system is included in the 921 systems compiled from DECHEMA.

Table 17. Activity Coefficients Results for System 4

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | exp |
| 70 | 0.086 | 2.5354 | 2.8327 | 2.8057 | 1.0060 | 1.0059 | 1.0641 |
| 70 | 0.166 | 2.2720 | 2.5160 | 2.5406 | 1.0220 | 1.0234 | 1.0821 |
| 70 | 0.238 | 2.0734 | 2.2670 | 2.2771 | 1.0460 | 1.0508 | 1.1110 |
| 70 | 0.384 | 1.7384 | 1.8499 | 1.8277 | 1.1334 | 1.1527 | 1.2301 |
| 70 | 0.559 | 1.4144 | 1.4744 | 1.4780 | 1.3671 | 1.4154 | 1.4922 |
| 70 | 0.711 | 1.1957 | 1.2352 | 1.2669 | 1.8399 | 1.9353 | 1.9684 |
| 70 | 0.815 | 1.0865 | 1.1128 | 1.1656 | 2.5117 | 2.7205 | 2.5806 |
| 70 | 0.945 | 1.0086 | 1.0137 | 1.0574 | 4.3935 | 5.5942 | 4.5631 |
| 70 | 0.975 | 1.0018 | 1.0031 | 1.0355 | 5.1647 | 7.2058 | 5.1094 |



Figure 16. System 5: Methanol (1) + 1-Propanol (2)
This system is included in the 921 systems compiled from DECHEMA.

Table 18. Activity Coefficients Results for System 5

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | exp |
| 60.02 | 0.0368 | 1.0792 | 1.1830 | 1.0128 | 0.99996 | 1.0001 | 1.0537 |
| 60.02 | 0.0528 | 1.0797 | 1.1789 | 1.0236 | 0.99994 | 1.0003 | 1.0592 |
| 60.02 | 0.0611 | 1.0799 | 1.1768 | 1.0212 | 0.99993 | 1.0004 | 1.0538 |
| 60.02 | 0.0649 | 1.0799 | 1.1759 | 1.0354 | 0.99993 | 1.0005 | 1.0537 |
| 60.02 | 0.0764 | 1.0799 | 1.1740 | 1.0354 | 0.99992 | 1.0007 | 1.0615 |
| 60.02 | 0.1007 | 1.0794 | 1.1668 | 1.0184 | 0.99997 | 1.0012 | 1.0550 |
| 60.02 | 0.1393 | 1.0774 | 1.1570 | 1.0210 | 1.0002 | 1.0023 | 1.0562 |
| 60.02 | 0.1842 | 1.0734 | 1.1457 | 1.0100 | 1.0010 | 1.0042 | 1.0624 |
| 60.02 | 0.2151 | 1.0698 | 1.1379 | 1.0100 | 1.0018 | 1.0059 | 1.0640 |
| 60.02 | 0.2625 | 1.0635 | 1.1261 | 1.0103 | 1.0037 | 1.0092 | 1.0648 |
| 60.02 | 0.3206 | 1.0547 | 1.1117 | 1.0062 | 1.0071 | 1.0146 | 1.0718 |
| 60.02 | 0.3806 | 1.0452 | 1.0972 | 1.0098 | 1.0121 | 1.0218 | 1.0722 |
| 60.02 | 0.4459 | 1.0350 | 1.0819 | 1.0040 | 1.0191 | 1.0321 | 1.0834 |
| 60.02 | 0.5022 | 1.0269 | 1.0691 | 1.0111 | 1.0263 | 1.0432 | 1.0781 |
| 60.02 | 0.552 | 1.0205 | 1.0583 | 1.0078 | 1.0336 | 1.0551 | 1.0858 |
| 60.02 | 0.597 | 1.0154 | 1.0489 | 1.0032 | 1.0406 | 1.0678 | 1.0981 |
| 60.02 | 0.6338 | 1.0117 | 1.0417 | 1.0044 | 1.0466 | 1.0798 | 1.0986 |
| 60.02 | 0.7034 | 1.0063 | 1.0290 | 1.0022 | 1.0580 | 1.1068 | 1.1143 |
| 60.02 | 0.737 | 1.0043 | 1.0235 | 0.9987 | 1.0633 | 1.1223 | 1.1379 |
| 60.02 | 0.783 | 1.0023 | 1.0166 | 0.9984 | 1.0700 | 1.1464 | 1.1346 |
| 60.02 | 0.8275 | 1.0010 | 1.0109 | 0.99896 | 1.0756 | 1.1734 | 1.1448 |
| 60.02 | 0.8804 | 1.0002 | 1.0055 | 0.99903 | 1.0807 | 1.2110 | 1.1353 |
| 60.02 | 0.9238 | 1.0000 | 1.0023 | 0.99873 | 1.0829 | 1.2469 | 1.1705 |
| 60.02 | 0.9707 | 0.99998 | 1.0004 | 0.99953 | 1.0830 | 1.2918 | 1.1305 |
|  |  |  |  |  |  |  |  |



Figure 17. System 6: Methanol (1) +1 -Butanol (2) This system is included in the 921 systems compiled from DECHEMA.

Table 19. Activity Coefficients Results for System 6

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |  |
| 25 | 0.0871 | 1.1979 | 1.2169 | 1.0929 | 1.0022 | 1.0010 | 1.0585 |  |
| 25 | 0.0953 | 1.193 | 1.2144 | 1.0980 | 1.0026 | 1.0012 | 1.0579 |  |
| 25 | 0.1200 | 1.1793 | 1.2069 | 1.0743 | 1.0040 | 1.0020 | 1.0520 |  |
| 25 | 0.1295 | 1.1743 | 1.2040 | 1.0919 | 1.0047 | 1.0023 | 1.0625 |  |
| 25 | 0.1690 | 1.1556 | 1.1919 | 1.0748 | 1.0075 | 1.0041 | 1.0554 |  |
| 25 | 0.2340 | 1.1299 | 1.1720 | 1.0693 | 1.0132 | 1.0084 | 1.0646 |  |
| 25 | 0.2654 | 1.1194 | 1.1624 | 1.0696 | 1.0163 | 1.0111 | 1.0719 |  |
| 25 | 0.3072 | 1.107 | 1.1496 | 1.0650 | 1.0209 | 1.0156 | 1.0813 |  |
| 25 | 0.3173 | 1.1042 | 1.1465 | 1.0664 | 1.0221 | 1.0169 | 1.0786 |  |
| 25 | 0.3557 | 1.0942 | 1.1349 | 1.0603 | 1.0268 | 1.0222 | 1.0868 |  |
| 25 | 0.3628 | 1.0925 | 1.1327 | 1.0631 | 1.0277 | 1.0232 | 1.0928 |  |
| 25 | 0.4172 | 1.0800 | 1.1165 | 1.0562 | 1.0352 | 1.0328 | 1.0891 |  |
| 25 | 0.4258 | 1.0782 | 1.1139 | 1.0565 | 1.0365 | 1.0345 | 1.0952 |  |
| 25 | 0.4569 | 1.0718 | 1.1048 | 1.0543 | 1.0414 | 1.0413 | 1.1081 |  |
| 25 | 0.5048 | 1.0624 | 1.0909 | 1.0467 | 1.0499 | 1.0535 | 1.1214 |  |
| 25 | 0.5845 | 1.0481 | 1.0689 | 1.0367 | 1.0672 | 1.0796 | 1.1441 |  |
| 25 | 0.6544 | 1.0363 | 1.0509 | 1.0281 | 1.0870 | 1.1100 | 1.1621 |  |
| 25 | 0.7237 | 1.0255 | 1.0348 | 1.0182 | 1.1127 | 1.1488 | 1.2094 |  |
| 25 | 0.8164 | 1.0129 | 1.0168 | 1.0088 | 1.1604 | 1.2188 | 1.2827 |  |
| 25 | 0.8660 | 1.0074 | 1.0094 | 1.0046 | 1.1944 | 1.267 | 1.3519 |  |
| 25 | 0.9290 | 1.0023 | 1.0028 | 1.001 | 1.2491 | 1.3422 | 1.4593 |  |



Figure 18. System 7: Methyl Acetate (1) + Methanol (2) This system is included in the 921 systems compiled from DECHEMA.

Table 20. Activity Coefficients Results for System 7

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | exp |  |
| 55 | 0.125 | 2.1741 | 2.0455 | 2.1343 | 1.0131 | 1.0133 | 1.0284 |  |
| 55 | 0.250 | 1.7972 | 1.7131 | 1.7839 | 1.0590 | 1.0557 | 1.0426 |  |
| 55 | 0.378 | 1.5006 | 1.4617 | 1.5055 | 1.1505 | 1.1354 | 1.1404 |  |
| 55 | 0.480 | 1.3243 | 1.3113 | 1.3372 | 1.2638 | 1.2321 | 1.2466 |  |
| 55 | 0.625 | 1.1510 | 1.1568 | 1.1778 | 1.5025 | 1.4387 | 1.4433 |  |
| 55 | 0.652 | 1.1274 | 1.1346 | 1.1318 | 1.5586 | 1.4888 | 1.5592 |  |
| 55 | 0.750 | 1.0608 | 1.0692 | 1.0573 | 1.7972 | 1.7117 | 1.8197 |  |
| 55 | 0.875 | 1.0137 | 1.0175 | 1.0185 | 2.1856 | 2.1232 | 2.1559 |  |



Figure 19. System 8: Acetone (1) + Benzene (2) This system is included in the 921 systems compiled from DECHEMA.

Table 21. Activity Coefficients Results for System 8

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 1.5766 | 1.4501 | 1.5333 | 1.0021 | 1.0011 | 1.0089 |  |
| 40 | 0.1027 | 1.4944 | 1.4091 | 1.4592 | 1.0068 | 1.0036 | 1.0126 |  |
| 40 | 0.1608 | 1.4050 | 1.3600 | 1.2695 | 1.0163 | 1.0090 | 0.9662 |  |
| 40 | 0.2615 | 1.2824 | 1.2824 | 1.2442 | 1.0413 | 1.0250 | 1.0557 |  |
| 40 | 0.3240 | 1.2229 | 1.2390 | 1.1951 | 1.0619 | 1.0398 | 1.0728 |  |
| 40 | 0.3734 | 1.1832 | 1.2072 | 1.1605 | 1.0809 | 1.0544 | 1.0947 |  |
| 40 | 0.4636 | 1.1244 | 1.1547 | 1.1081 | 1.1212 | 1.0887 | 1.1297 |  |
| 40 | 0.5300 | 1.0906 | 1.1207 | 1.0859 | 1.1553 | 1.1213 | 1.1698 |  |
| 40 | 0.5892 | 1.0663 | 1.0937 | 1.0670 | 1.1889 | 1.1566 | 1.1964 |  |
| 40 | 0.7325 | 1.0256 | 1.0417 | 1.0253 | 1.2821 | 1.2726 | 1.2834 |  |
| 40 | 0.8051 | 1.0130 | 1.0228 | 1.0107 | 1.3357 | 1.3527 | 1.3445 |  |
| 40 | 0.8807 | 1.0047 | 1.0088 | 1.0042 | 1.3959 | 1.4564 | 1.4197 |  |



Figure 20. System 9: Acetone (1) + Hexane (2) This system is included in the 921 systems compiled from DECHEMA.

Table 22. Activity Coefficients Results for System 9

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 45 | 0.0651 | 3.8874 | 4.3018 | 3.7694 | 1.0068 | 1.0080 | 1.0175 |
| 45 | 0.1592 | 3.0064 | 3.1826 | 2.9722 | 1.0399 | 1.0470 | 1.0764 |
| 45 | 0.2549 | 2.3976 | 2.4547 | 2.3331 | 1.1031 | 1.1203 | 1.1431 |
| 45 | 0.3478 | 1.9805 | 1.9822 | 1.9260 | 1.1979 | 1.2283 | 1.2537 |
| 45 | 0.4429 | 1.6703 | 1.6479 | 1.6352 | 1.3391 | 1.3859 | 1.4005 |
| 45 | 0.5210 | 1.4776 | 1.4493 | 1.4539 | 1.5009 | 1.5618 | 1.5664 |
| 45 | 0.5907 | 1.3414 | 1.3140 | 1.3105 | 1.6942 | 1.7656 | 1.7287 |
| 45 | 0.6202 | 1.2923 | 1.2663 | 1.2709 | 1.7941 | 1.8686 | 1.8321 |
| 45 | 0.7168 | 1.1615 | 1.1430 | 1.1446 | 2.2260 | 2.2978 | 2.2188 |
| 45 | 0.7923 | 1.0876 | 1.0760 | 1.0878 | 2.7256 | 2.7672 | 2.6746 |
| 45 | 0.8022 | 1.0796 | 1.0689 | 1.1058 | 2.8058 | 2.8404 | 2.5458 |
| 45 | 0.8692 | 1.0355 | 1.0302 | 1.0274 | 3.4712 | 3.4271 | 3.3264 |
| 45 | 0.9288 | 1.0108 | 1.0090 | 1.0116 | 4.3058 | 4.1224 | 4.2642 |
| 45 | 0.9658 | 1.0025 | 1.0021 | 0.9884 | 4.9897 | 4.6660 | 4.7251 |



Figure 21. System 10: Acetone (1) + Toluene (2)
This system is included in the 921 systems compiled from DECHEMA.

Table 23. Activity Coefficients Results for System 10

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 35 | 0.1469 | 1.5461 | 1.3612 | 1.4453 | 1.0152 | 1.0051 | 1.0650 |
| 35 | 0.1988 | 1.4624 | 1.3309 | 1.4012 | 1.0271 | 1.0098 | 1.0273 |
| 35 | 0.2126 | 1.4424 | 1.3230 | 1.3677 | 1.0308 | 1.0114 | 1.0714 |
| 35 | 0.2757 | 1.3608 | 1.2868 | 1.3066 | 1.0503 | 1.0205 | 1.0624 |
| 35 | 0.3761 | 1.2581 | 1.2309 | 1.2022 | 1.0908 | 1.0428 | 1.1293 |
| 35 | 0.4541 | 1.1954 | 1.1891 | 1.1469 | 1.1311 | 1.0688 | 1.1853 |
| 35 | 0.5234 | 1.1492 | 1.1536 | 1.1007 | 1.1746 | 1.1003 | 1.2444 |
| 35 | 0.5821 | 1.1158 | 1.1251 | 1.0738 | 1.2183 | 1.1350 | 1.2570 |
| 35 | 0.6450 | 1.0850 | 1.0963 | 1.0492 | 1.2736 | 1.1828 | 1.3524 |
| 35 | 0.7043 | 1.0603 | 1.0713 | 1.0283 | 1.3359 | 1.2409 | 1.3634 |
| 35 | 0.7519 | 1.0434 | 1.0530 | 1.0178 | 1.3947 | 1.2994 | 1.3632 |
| 35 | 0.8026 | 1.0282 | 1.0357 | 1.0055 | 1.4679 | 1.3769 | 1.4446 |
| 35 | 0.8578 | 1.0152 | 1.0199 | 0.9967 | 1.5628 | 1.4848 | 1.5315 |
| 35 | 0.9257 | 1.0043 | 1.0060 | 0.9893 | 1.7078 | 1.6649 | 1.6577 |



Figure 22. System 11: 2,4-Dimethylpentane (1) + Benzene (2) This system was not included in the 921 systems compiled from DECHEMA.

Table 24. Activity Coefficients Results for System 11

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 77.3 | 0.078 | 1.7276 | 1.5491 | 1.7593 | 1.0041 | 1.0054 | 1.0312 |
| 77 | 0.106 | 1.6693 | 1.4863 | 1.7142 | 1.0076 | 1.0097 | 1.0257 |
| 76.5 | 0.14 | 1.6034 | 1.4203 | 1.5672 | 1.0133 | 1.0162 | 1.0430 |
| 76.3 | 0.152 | 1.5814 | 1.3992 | 1.6312 | 1.0157 | 1.0188 | 1.0327 |
| 76.1 | 0.192 | 1.5122 | 1.3359 | 1.4359 | 1.0252 | 1.0287 | 1.0585 |
| 75.9 | 0.224 | 1.4614 | 1.2925 | 1.3714 | 1.0344 | 1.0377 | 1.0711 |
| 75.7 | 0.251 | 1.4215 | 1.2601 | 1.3418 | 1.0434 | 1.0460 | 1.0802 |
| 75.5 | 0.281 | 1.3801 | 1.2280 | 1.3134 | 1.0546 | 1.0559 | 1.0908 |
| 75.4 | 0.335 | 1.3130 | 1.1789 | 1.2407 | 1.0783 | 1.0753 | 1.1155 |
| 75.4 | 0.378 | 1.2658 | 1.1467 | 1.2073 | 1.1004 | 1.0919 | 1.1277 |
| 75.2 | 0.432 | 1.2136 | 1.1133 | 1.1715 | 1.1323 | 1.1142 | 1.1610 |
| 75.4 | 0.48 | 1.1734 | 1.0889 | 1.1375 | 1.1648 | 1.1349 | 1.1781 |
| 75.3 | 0.525 | 1.1404 | 1.0700 | 1.1211 | 1.1988 | 1.1552 | 1.2085 |
| 75.5 | 0.572 | 1.1105 | 1.0536 | 1.0977 | 1.2381 | 1.1769 | 1.2333 |
| 75.5 | 0.616 | 1.0865 | 1.0409 | 1.0852 | 1.2784 | 1.1979 | 1.2698 |
| 75.9 | 0.662 | 1.0650 | 1.0300 | 1.0632 | 1.3243 | 1.2200 | 1.2968 |
| 76.1 | 0.700 | 1.0500 | 1.0227 | 1.0611 | 1.3652 | 1.2387 | 1.3089 |
| 76.3 | 0.74 | 1.0366 | 1.0163 | 1.0495 | 1.4110 | 1.2585 | 1.3541 |
| 76.6 | 0.785 | 1.0243 | 1.0106 | 1.0446 | 1.4661 | 1.2810 | 1.3897 |
| 77.2 | 0.839 | 1.0131 | 1.0056 | 1.0303 | 1.5369 | 1.3079 | 1.4555 |



Figure 23. System 12: Cyclohexane (1) + Isopropyl Alcohol (2)
This system is included in the 921 systems compiled from
DECHEMA as an isothermal system at a different temperature.
Table 25. Activity Coefficients Results for System 12

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 67.3 | 0.029 | 5.8966 | 4.2363 | 4.5675 | 1.0025 | 1.0010 | 1.1364 |
| 67.0 | 0.068 | 4.7907 | 3.8929 | 3.7706 | 1.0131 | 1.0053 | 1.0328 |
| 63.1 | 0.138 | 3.5330 | 3.3805 | 3.2967 | 1.0488 | 1.0225 | 1.0833 |
| 61.2 | 0.213 | 2.7561 | 2.9176 | 2.7533 | 1.1052 | 1.0557 | 1.1213 |
| 60.1 | 0.266 | 2.3999 | 2.6403 | 2.4872 | 1.1543 | 1.0901 | 1.1672 |
| 59.1 | 0.313 | 2.1646 | 2.4239 | 2.2774 | 1.2038 | 1.1294 | 1.2508 |
| 58.3 | 0.408 | 1.8285 | 2.0534 | 1.9303 | 1.3234 | 1.2412 | 1.3775 |
| 58.0 | 0.475 | 1.6574 | 1.8386 | 1.7335 | 1.4303 | 1.3552 | 1.5011 |
| 57.8 | 0.556 | 1.4901 | 1.6203 | 1.5438 | 1.6021 | 1.5512 | 1.6984 |
| 57.8 | 0.637 | 1.3495 | 1.4395 | 1.3758 | 1.8560 | 1.8488 | 2.0065 |
| 57.9 | 0.734 | 1.2068 | 1.2640 | 1.2500 | 2.3732 | 2.4592 | 2.4882 |
| 58.5 | 0.818 | 1.1066 | 1.1433 | 1.1363 | 3.2129 | 3.4869 | 3.2916 |
| 59.1 | 0.884 | 1.0471 | 1.0688 | 1.0686 | 4.4163 | 5.1331 | 4.6018 |
| 61.9 | 0.963 | 1.0054 | 1.0093 | 1.0192 | 7.2844 | 10.364 | 8.1042 |



Figure 24. System 13: Ethylcyclohexane (1) + Isopropyl Alcohol (2) This system was not included in the 921 systems compiled from DECHEMA.

Table 26. Activity Coefficients Results for System 13

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | exp |
| 66.5 | 0.059 | 5.1585 | 5.4078 | 5.7770 | 1.0099 | 1.0063 | 1.0344 |
| 66.25 | 0.100 | 4.2455 | 4.7320 | 4.7842 | 1.0270 | 1.0180 | 1.0583 |
| 66.34 | 0.120 | 3.8974 | 4.4444 | 4.7150 | 1.0379 | 1.0259 | 1.0538 |
| 66.3 | 0.130 | 3.7423 | 4.3109 | 4.3936 | 1.0439 | 1.0304 | 1.0666 |
| 66.3 | 0.113 | 4.0132 | 4.5422 | 4.7387 | 1.0339 | 1.0230 | 1.0558 |
| 66.4 | 0.161 | 3.3276 | 3.9310 | 4.0579 | 1.0650 | 1.0467 | 1.0770 |
| 66.5 | 0.239 | 2.6015 | 3.1712 | 3.2597 | 1.1321 | 1.1043 | 1.1418 |
| 66.4 | 0.216 | 2.7790 | 3.3709 | 3.5390 | 1.1103 | 1.0847 | 1.1188 |
| 67.7 | 0.377 | 1.9077 | 2.2803 | 2.4396 | 1.2976 | 1.2778 | 1.2537 |
| 67.5 | 0.348 | 2.0160 | 2.4316 | 2.6274 | 1.2575 | 1.2322 | 1.2134 |
| 68.8 | 0.558 | 1.4502 | 1.6084 | 1.6792 | 1.6506 | 1.7364 | 1.6517 |
| 70.8 | 0.786 | 1.1244 | 1.1613 | 1.2921 | 2.8320 | 3.4287 | 2.9582 |
| 77.5 | 0.89 | 1.0369 | 1.0485 | 1.0434 | 4.3350 | 5.6805 | 4.0146 |
| 78.3 | 0.909 | 1.0258 | 1.0344 | 1.0380 | 4.7710 | 6.3847 | 4.5875 |
| 84.1 | 0.951 | 1.0079 | 1.0106 | 1.0335 | 6.0371 | 8.3865 | 5.7276 |
| 85.1 | 0.954 | 1.0070 | 1.0094 | 1.0266 | 6.1476 | 8.5371 | 5.7134 |
| 92.1 | 0.977 | 1.0018 | 1.0024 | 1.0165 | 7.1086 | 9.8605 | 6.6209 |
| 92.9 | 0.979 | 1.0015 | 1.0020 | 1.0046 | 7.2028 | 9.9750 | 6.8637 |
| 101.6 | 0.994 | 1.0001 | 1.0002 | 1.0141 | 7.9729 | 10.6650 | 8.4350 |
| 101.1 | 0.993 | 1.0002 | 1.0002 | 1.0081 | 7.9178 | 10.6120 | 8.0210 |



Figure 25. System 14: Benzene (1) + Isopropyl Alcohol (2)
This system is included in the 921 systems compiled from DECHEMA as an isothermal system at a different temperature.

Table 27. Activity Coefficients Results for System 14

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 69.5 | 0.039 | 3.1057 | 3.0254 | 3.5011 | 1.0025 | 1.0013 | 1.0210 |
| 67.1 | 0.089 | 2.6948 | 2.8018 | 2.9422 | 1.0122 | 1.0069 | 1.0392 |
| 65.4 | 0.142 | 2.3655 | 2.5814 | 2.6093 | 1.0295 | 1.0183 | 1.0500 |
| 63.9 | 0.197 | 2.1047 | 2.3733 | 2.3984 | 1.0543 | 1.0366 | 1.0652 |
| 62.9 | 0.255 | 1.8925 | 2.1739 | 2.1215 | 1.0874 | 1.0642 | 1.1086 |
| 61.8 | 0.355 | 1.6262 | 1.8768 | 1.7724 | 1.1620 | 1.1364 | 1.2058 |
| 61.0 | 0.414 | 1.5083 | 1.7275 | 1.6761 | 1.2179 | 1.1979 | 1.2677 |
| 60.9 | 0.495 | 1.3772 | 1.5476 | 1.4992 | 1.3137 | 1.3134 | 1.3528 |
| 60.3 | 0.566 | 1.2835 | 1.4141 | 1.3972 | 1.4228 | 1.4562 | 1.5141 |
| 60.2 | 0.640 | 1.2016 | 1.2949 | 1.2816 | 1.5730 | 1.6655 | 1.7310 |
| 60.1 | 0.716 | 1.1315 | 1.1930 | 1.1976 | 1.7860 | 1.9809 | 2.0360 |
| 60.3 | 0.797 | 1.0715 | 1.1061 | 1.1206 | 2.1170 | 2.5075 | 2.5360 |
| 63.0 | 0.942 | 1.0067 | 1.0105 | 1.0104 | 3.2457 | 4.6252 | 4.5911 |
| 64.7 | 0.976 | 1.0012 | 1.0019 | 0.9953 | 3.6938 | 5.5995 | 6.2019 |



Figure 26. System 15: Toluene (1) + Isopropyl Alcohol (2) This system was not included in the 921 systems compiled from DECHEMA. None of the prediction methods was able to predict the deviation peak of $\gamma_{21}$ at a low $\mathrm{X}_{2}$ value.

Table 28. Activity Coefficients Results for System 15

| Temp <br> $\left({ }^{\mathbf{}} \mathbf{C} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | exp |
| 81.6 | 0.067 | 3.0777 | 3.1255 | 3.0223 | 1.0069 | 1.0052 | 1.0237 |
| 81.2 | 0.142 | 2.5265 | 2.6786 | 2.5740 | 1.0302 | 1.0236 | 1.0529 |
| 81.2 | 0.185 | 2.2816 | 2.4636 | 2.3817 | 1.0510 | 1.0404 | 1.0696 |
| 81.4 | 0.220 | 2.1118 | 2.3070 | 2.1813 | 1.0718 | 1.0578 | 1.0854 |
| 81.5 | 0.258 | 1.9523 | 2.1544 | 2.1034 | 1.0986 | 1.0807 | 1.0997 |
| 81.5 | 0.296 | 1.8148 | 2.0178 | 1.9673 | 1.1297 | 1.1082 | 1.1353 |
| 81.8 | 0.324 | 1.7254 | 1.9252 | 1.8546 | 1.1557 | 1.1316 | 1.1525 |
| 82.2 | 0.426 | 1.4680 | 1.6437 | 1.5846 | 1.2731 | 1.2439 | 1.2749 |
| 83.2 | 0.531 | 1.2856 | 1.4234 | 1.3654 | 1.4376 | 1.4178 | 1.4330 |
| 84.0 | 0.603 | 1.1949 | 1.3046 | 1.2723 | 1.5820 | 1.5873 | 1.5742 |
| 85.4 | 0.688 | 1.1151 | 1.1918 | 1.1935 | 1.7941 | 1.8664 | 1.7752 |
| 86.6 | 0.744 | 1.0758 | 1.1321 | 1.1279 | 1.9641 | 2.1188 | 1.9817 |
| 88.5 | 0.797 | 1.0469 | 1.0853 | 1.0778 | 2.1521 | 2.4286 | 2.1768 |
| 91.0 | 0.851 | 1.0250 | 1.0475 | 1.0584 | 2.3762 | 2.8441 | 2.4000 |
| 94.4 | 0.897 | 1.0119 | 1.0234 | 1.0244 | 2.5980 | 3.3017 | 2.6305 |
| 96.6 | 0.922 | 1.0068 | 1.0136 | 1.0242 | 2.7325 | 3.6029 | 2.7742 |
| 104.6 | 0.970 | 1.0010 | 1.0021 | 0.7619 | 3.0227 | 4.2603 | 5.3889 |



Figure 27. System 16: Ethyl Ether (1) + Acetone (2) This system is included in the 921 systems compiled from DECHEMA as an isothermal system at a different temperature. The prediction for the activity coefficient of molecule 2 from the UNIFAC and ANN methods were close to each other but far from the experimental values.

Table 29. Activity Coefficients Results for System 16

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 0 | 0.156 | 1.8182 | 1.6010 | 1.8281 | 1.0214 | 1.0154 | 1.1136 |
| 0 | 0.192 | 1.7304 | 1.5429 | 1.4276 | 1.0321 | 1.0233 | 1.1643 |
| 0 | 0.364 | 1.4183 | 1.3220 | 1.2933 | 1.1140 | 1.0861 | 1.2191 |
| 0 | 0.510 | 1.2447 | 1.1901 | 1.0588 | 1.2330 | 1.1786 | 1.4402 |
| 0 | 0.617 | 1.1516 | 1.1178 | 1.0588 | 1.3634 | 1.2780 | 1.6908 |
| 0 | 0.835 | 1.0306 | 1.0238 | 1.0028 | 1.8394 | 1.6189 | 2.1738 |



Figure 28. System 17: Acetone (1) + Isopropyl Alcohol (2) This system is included in the 921 systems compiled from DECHEMA even though was taken from a different experimental database.

## Table 30. Activity Coefficients Results for System 17

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\gamma_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | $\exp$ | ANN | UNIFAC | $\exp$ |
| 25 | 0.175 | 1.8681 | 1.7034 | 1.4823 | 1.0384 | 1.0238 | 1.1202 |
| 25 | 0.339 | 1.4848 | 1.4127 | 1.3108 | 1.1225 | 1.0923 | 1.2898 |
| 25 | 0.514 | 1.2678 | 1.2090 | 1.1242 | 1.2620 | 1.2265 | 1.6016 |
| 25 | 0.669 | 1.1395 | 1.0938 | 1.0516 | 1.4751 | 1.4180 | 1.9182 |
| 25 | 0.839 | 1.0397 | 1.0220 | 1.0409 | 1.9681 | 1.7471 | 2.8548 |



Figure 29. System 18: Isopropyl Alcohol (1) + Ethyl Acetate (2) This system is included in the 921 systems compiled from DECHEMA even though was taken from a different experimental database.

## Table 31. Activity Coefficients Results for System 18

| Temp <br> $\left({ }^{\mathbf{}} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | $\exp$ |
| 40 | 0.0915 | 2.0621 | 2.2288 | 2.0862 | 1.0078 | 1.0086 | 1.0101 |
| 40 | 0.1860 | 1.7757 | 1.8928 | 1.8919 | 1.0324 | 1.0355 | 1.0331 |
| 40 | 0.3595 | 1.4155 | 1.4788 | 1.5003 | 1.1238 | 1.1357 | 1.1293 |
| 40 | 0.4600 | 1.2757 | 1.3197 | 1.3103 | 1.2078 | 1.2290 | 1.2020 |
| 40 | 0.5385 | 1.1922 | 1.2245 | 1.2235 | 1.2921 | 1.3243 | 1.2771 |
| 40 | 0.6150 | 1.1286 | 1.1515 | 1.1706 | 1.3924 | 1.4399 | 1.3895 |
| 40 | 0.7100 | 1.0699 | 1.0836 | 1.1233 | 1.5460 | 1.6225 | 1.5160 |
| 40 | 0.7300 | 1.0601 | 1.0721 | 1.0954 | 1.5829 | 1.6675 | 1.5749 |
| 40 | 0.8010 | 1.0319 | 1.0387 | 1.0771 | 1.7290 | 1.8492 | 1.7242 |
| 40 | 0.8500 | 1.0178 | 1.0219 | 1.0740 | 1.8446 | 1.9977 | 1.9641 |
| 40 | 0.8845 | 1.0105 | 1.0129 | 1.0532 | 1.9341 | 2.1156 | 1.9337 |
| 40 | 0.9300 | 1.0038 | 1.0047 | 1.0395 | 2.0634 | 2.2905 | 2.0824 |
| 40 | 0.9500 | 1.0019 | 1.0024 | 1.0372 | 2.1246 | 2.3752 | 2.1279 |
| 40 | 0.9620 | 1.0011 | 1.0014 | 1.0407 | 2.1627 | 2.4285 | 2.2248 |



Figure 30. System 19: Chloroform (1) + n-Butyl Alcohol (2) This system was not included in the 921 systems compiled from DECHEMA. None of the prediction methods was able to predict the deviation peak of $\gamma_{21}$ at a low $X_{2}$ value.

Table 32. Activity Coefficients Results for System 19

| Temp <br> $\left({ }^{\circ} \mathbf{C}\right)$ | $\boldsymbol{x}_{\mathbf{1}}$ | $\boldsymbol{\gamma}_{\mathbf{1}}$ |  |  |  | $\boldsymbol{\gamma}_{\mathbf{2}}$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | ANN | UNIFAC | exp | ANN | UNIFAC | exp |  |
| 115.1 | 0.0180 | 2.1604 | 1.4168 | 1.2632 | 1.0004 | 1.0000 | 0.9987 |  |
| 113.8 | 0.0300 | 2.1075 | 1.4136 | 1.2811 | 1.0010 | 1.0001 | 0.9855 |  |
| 106.4 | 0.0764 | 1.9334 | 1.4038 | 1.3392 | 1.0058 | 1.0009 | 1.0404 |  |
| 99.7 | 0.1388 | 1.7581 | 1.3855 | 1.3514 | 1.0173 | 1.0031 | 0.9932 |  |
| 93.4 | 0.2016 | 1.6285 | 1.3652 | 1.3401 | 1.0333 | 1.0073 | 0.9835 |  |
| 90.3 | 0.2272 | 1.5853 | 1.3571 | 1.3528 | 1.0409 | 1.0096 | 1.0354 |  |
| 89.3 | 0.2484 | 1.5527 | 1.3485 | 1.3062 | 1.0477 | 1.0119 | 1.0304 |  |
| 84.8 | 0.3036 | 1.4790 | 1.3272 | 1.3063 | 1.0672 | 1.0195 | 1.0352 |  |
| 84.4 | 0.3156 | 1.4647 | 1.3219 | 1.2770 | 1.0719 | 1.0215 | 1.0502 |  |
| 82.2 | 0.3452 | 1.4315 | 1.3096 | 1.2849 | 1.0841 | 1.0271 | 1.0330 |  |
| 80.0 | 0.3838 | 1.3917 | 1.2925 | 1.2541 | 1.1018 | 1.0360 | 1.0942 |  |
| 78.7 | 0.4060 | 1.3702 | 1.2825 | 1.2510 | 1.1130 | 1.0420 | 1.0894 |  |
| 77.5 | 0.4244 | 1.3531 | 1.2741 | 1.2564 | 1.1230 | 1.0475 | 1.0802 |  |
| 75.1 | 0.4798 | 1.3043 | 1.2470 | 1.2144 | 1.1576 | 1.0680 | 1.1595 |  |
| 74.6 | 0.4940 | 1.2922 | 1.2398 | 1.2065 | 1.1678 | 1.0743 | 1.1376 |  |
| 73.0 | 0.5300 | 1.2625 | 1.2216 | 1.1980 | 1.1968 | 1.0926 | 1.1293 |  |
| 70.8 | 0.598 | 1.2084 | 1.1854 | 1.1511 | 1.2668 | 1.1387 | 1.2364 |  |
| 69.2 | 0.6524 | 1.1670 | 1.1556 | 1.1225 | 1.3428 | 1.1906 | 1.2764 |  |
| 67.2 | 0.7220 | 1.1171 | 1.1171 | 1.0920 | 1.4788 | 1.2874 | 1.4204 |  |
| 66.3 | 0.7698 | 1.0857 | 1.0905 | 1.0591 | 1.6085 | 1.3843 | 1.5972 |  |
| 65.4 | 0.8084 | 1.0626 | 1.0698 | 1.0462 | 1.7435 | 1.4909 | 1.6087 |  |
| 64.5 | 0.8528 | 1.0393 | 1.0471 | 1.0269 | 1.9442 | 1.6614 | 1.7834 |  |
| 63.9 | 0.9032 | 1.0183 | 1.0241 | 0.9762 | 2.2540 | 1.9565 | 4.0908 |  |
| 62.6 | 0.9536 | 1.0045 | 1.0067 | 0.9932 | 2.6918 | 2.4646 | 2.1655 |  |

## Appendix B Functional Groups Table

Table 33. Organic Functional Groups Table Based on Quantum Mechanical Calculations

| Family name | Group \# | Functional Group | Family name | Group \# | Functional Group |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Alkane | G1 | C | Nitrile | G95 | CH 2 CN |
|  | G2 | CH |  | G96 | CH3CN |
|  | G3 | CH2 | Nitro | G97 | CNO2 |
|  | G4 | CH3 |  | G98 | CHNO2 |
|  | G5 | CH4 |  | G99 | CH2NO2 |
| Alkene | G6 | $\mathrm{C}=$ |  | G100 | CH3NO2 |
|  | G7 | $\mathrm{CH}=$ | Thiol | G101 | CSH |
|  | G8 | CH2= |  | G102 | CHSH |
| Alkyne | G9 | $\mathrm{C}^{\circ}$ |  | G103 | CH2SH |
|  | G10 | $\mathrm{CH}^{\circ}$ |  | G104 | CH3SH |
| Alcohol | G11 | COH | Chloroalkane | G105 | CCl |
|  | G12 | CHOH |  | G106 | CHCl |
|  | G13 | CH2OH |  | G107 | CH 2 Cl |
|  | G14 | CH3OH |  | G108 | CH 3 Cl |
| Glycol | G15 | GCOH | Fluoroalkane | G109 | CHF |
|  | G16 | GCHOH |  | G110 | CH2F2 |
|  | G17 | gCH 2 OH |  | G111 | CF |
| Ether | G18 | COC |  | G112 | CF2 |
|  | G19 | CHOCH |  | G113 | CF3 |
|  | G20 | CH2OCH2 |  | G114 | CHF2 |
|  | G21 | CH3OCH3 |  | G115 | CHF3 |
|  | G22 | COCH |  | G116 | CH3F |
|  | G23 | COCH2 |  | G117 | CH2F |
|  | G24 | COCH3 | Chlorofluoroalkane | G118 | CClF2 |
|  | G25 | CHOCH2 |  | G119 | CCl2F |
|  | G26 | CHOCH3 |  | G120 | CClF3 |
|  | G27 | CH2OCH3 |  | G121 | CCl 3 F |
|  | G28 | CH3OC |  | G122 | CHClF |
|  | G29 | CH3OCH |  | G123 | CHCl2 |
|  | G30 | CH3OCH2 |  | G124 | CHCl3 |
|  | G31 | CH2OC |  | G125 | CCl 2 |
|  | G32 | CH2OCH |  | G126 | CCl 3 |
|  | G33 | CHOC |  | G127 | CHClF2 |


| Family name | Group \# | Functional Group | Family name | Group \# | Functional Group |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Aldehyde | G34 | HCHO |  | G128 | CHCl2F |
|  | G35 | CCHO |  | G129 | CCIF |
|  | G36 | CHCHO |  | G130 | CH2ClF |
|  | G37 | CH2CHO |  | G131 | CH2Cl2 |
|  | G38 | CH3CHO |  | G132 | CCl2F2 |
| Ketone | G39 | CCOC |  | G133 | CCl 4 |
|  | G40 | CHCOCH | Arene | G134 | aC |
|  | G41 | CH2COCH2 |  | G135 | aCH |
|  | G42 | CH3COCH3 |  | G136 | aCOH |
|  | G43 | CCOCH |  | G137 | (aCH)2aCNH2 |
|  | G44 | CCOCH2 |  | G138 | $(\mathrm{aCH}) 2 \mathrm{aCNO} 2$ |
|  | G45 | CCOCH3 |  | G139 | (aCH) 2 aCCl |
|  | G46 | CHCOCH2 |  | G140 | aCHNaCH |
|  | G47 | CHCOCH3 | Amide(1) | G141 | CCONH2 |
|  | G48 | CH2COCH3 |  | G142 | CHCONH2 |
|  | G49 | CH3COC |  | G143 | CH2CONH2 |
|  | G50 | CH3COCH |  | G144 | CH3CONH2 |
|  | G51 | CH3COCH2 | Amide(2) | G145 | CCONHC |
|  | G52 | CH2COC |  | G146 | CHCONHCH |
|  | G53 | CH2COCH |  | G147 | $\begin{array}{\|c\|} \hline \mathrm{CH} 2 \mathrm{CONHCH} \\ 2 \\ \hline \end{array}$ |
|  | G54 | CHCOC |  | G148 | $\begin{array}{\|c\|} \hline \mathrm{CH} 3 \mathrm{CONHCH} \\ 3 \end{array}$ |
| Carboxylic Acid | G55 | HCOOH |  | G149 | CCONHCH |
|  | G56 | CCOOH |  | G150 | CCONHCH2 |
|  | G57 | CHCOOH |  | G151 | CCONHCH3 |
|  | G58 | CH 2 COOH |  | G152 | CHCONHCH2 |
|  | G59 | CH 3 COOH |  | G153 | CHCONHCH3 |
| Ester(1) | G60 | HCOOC |  | G154 | $\begin{array}{\|c\|} \hline \mathrm{CH} 2 \mathrm{CONHCH} \\ 3 \end{array}$ |
|  | G61 | HCOOCH |  | G155 | CH3CONHC |
|  | G62 | HCOOCH2 |  | G156 | CH3CONHCH |
|  | G63 | HCOOCH3 |  | G157 | $\begin{array}{\|c\|} \hline \mathrm{CH} 3 \mathrm{CONHCH} \\ 2 \end{array}$ |
| Ester(2) | G64 | CCOOC |  | G158 | CH2CONHC |
|  | G65 | CHCOOCH |  | G159 | CH2CONHCH |



## Appendix C MatLab Programs

The first MatLab program developed was called Create.m and it purpose is to organize the vapor-liquid equilibrium experimental data within the information matrix. The following diagram shows the algorithm developed to perform the mentioned task.


Figure 31. Algorithm flowchart for Create.m

The vapor-liquid equilibrium experimental data was entered into a spreadsheet using the format specified in the following table.

Table 34. Experimental raw data spreadsheet format

| System \# | 0 | 0 | 0 | 0 | 0 | 0 | 0 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0 | Temp | A12 | A21 | alfa12 | 0 | 0 | 0 |
| 0 | A1 | B1 | C1 | 0 | 0 | 0 | 0 |
| 0 | A2 | B2 | B3 | 0 | 0 | 0 | 0 |
| 0 | G11 | G12 | G13 | G14 | G15 | G16 | G17 |
| 0 | n11 | n12 | n13 | n14 | n15 | n16 | n17 |
| 0 | G21 | G22 | G23 | G24 | G25 | G26 | G27 |
| 0 | n21 | n22 | n23 | n24 | n25 | n26 | n27 |
| 0 | P1 | X1 | Y1 | T1 | $\square$ U11 | $\square$ U21 | 0 |
| 0 | P2 | X2 | Y2 | T2 | $\square$ U12 | $\square$ U22 | 0 |
| 0 | P3 | X3 | Y3 | T3 | $\square$ U13 | $\square$ U23 | 0 |
| 0 | P4 | X4 | Y4 | T4 | $\square$ U14 | $\square$ U24 | 0 |
| 0 | P5 | X5 | Y5 | T5 | $\square$ U15 | $\square$ U25 | 0 |
| 0 | P6 | X6 | Y6 | T6 | $\square$ U16 | $\square$ U26 | 0 |
| 0 | Pn | Xn | Yn | Tn | $\square$ U1n | $\square$ U2n | 0 |
| 0 | 0 | 0 | 0 | 0 | 0 | 0 | 0 |

This table presents the format used to organize the experimental vapor-liquid equilibrium data taken from DECHEMA.
where,
System \# is the data system number.
Temp is the temperature of the system if isothermal in ${ }^{\circ} \mathrm{C}$.
A12, A21and alfal2 are the NRTL model constants.
A1, B1 and C1 are the Antoine constants for molecule 1.
$A 2, B 2$ and $C 2$ are the Antoine constants for molecule 2.
G11 to G17 are the number of the functional groups for molecule 1.
n11 to n17 are the quantity of each functional group for molecule 1.
G21 to $G 27$ are the number of the functional groups for molecule 2.
n21 to $n 27$ are the quantity of each functional group for molecule 2 .
Pl to Pn are the system pressure for each data point.
$X 1$ to Xn are the liquid mol fraction for molecule 1 for each data point.
Y1 to $Y n$ are the vapor mol fraction for molecule 1 for each data point.

T1 to Tn are the system temperature for each data point.
$\mathcal{U 1 1}$ to $\mathcal{U 1 n}$ are the activity coefficient predicted by UNIFAC for molecule 1 for each data point.
$\chi 21$ to $\mathcal{W} 2 n$ are the activity coefficient predicted by UNIFAC for molecule 2 for each data point.

Filling all unused cells of the spreadsheet data table with zeros is required by MatLab to load the file. The MatLab program reads the data file, process the experimental raw data and creates the information matrix. The Create.m program uses the MatLab function fminunc and the function Createfun_Margules3.m to calculate the Margules equation parameters. The information matrix is saved in a file to be used by the second MatLab program. The MatLab code for program Create.m is presented below.

```
% Program Create.m
    % This program will create the data base for the activity
    coefficients
    % estimation program.
    % The raw data was taken from DECHEMA data series.
    clear
    clc
    % Load the data file where experimental data is contain.
    filename = input('Enter the experimental data file name:','s');
    s = ['load ' filename '.txt'];
    disp('A large data file is loading. This may take a few minutes.')
    disp('Please wait!')
    eval(s);
    disp('Data had been loaded!')
    g = 186;
\begin{tabular}{lllllllllll} 
MW \(=[12\) & 13 & 14 & 15 & 16 & 12 & 13 & 14 & 12 & 13 & 29 \\
30 & 31 & 32 & 29 & 30 & 31 & 40 & 42 & 44 & 46 & 41 \\
42 & 43 & 43 & 44 & 45 & 43 & 44 & 45 & 42 & 43 & 41 \\
43 & 44 & 42 & 54 & 56 & 58 & 53 & 54 & 55 & 55 & 56 \\
55 & 56 & 57 & 54 & 55 & 53 & 46 & 59 & 58 & 59 & 60 \\
57 & 58 & 59 & 60 & 68 & 70 & 72 & 74 & 69 & 70 & 71 \\
71 & 72 & 74 & 71 & 72 & 73 & 70 & 71 & 69 & 28 & 29
\end{tabular}
```

| 30 | 31 | 39 | 41 | 43 | 45 | 50 | 52 | 56 | 59 | 27 |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| 38 | 39 | 40 | 41 | 58 | 59 | 60 | 61 | 45 | 46 | 47 |
| 48 | 47.5 | 48.5 | 49.5 | 50.5 | 32 | 52 | 31 | 50 | 69 | 51 |
| 70 | 34 | 33 | 85.5 | 102 | 104.5 | 137.5 | 67.5 | 84 | 119.5 | 83 |
| 118.5 | 86.5 | 103 | 66.5 | 68.5 | 85 | 121 | 154 | 12 | 13 | 29 |
| 54 | 84 | 73.5 | 40 | 56 | 57 | 58 | 59 | 67 | 69 | 71 |
| 73 | 68 | 69 | 70 | 71 | 72 | 73 | 70 | 71 | 72 | 69 |
| 70 | 68 | 66 | 81 | 85 | 87 | 80 | 82 | 84 | 83 | 85 |
| 86 | 81 | 83 | 85 | 80 | 82 | 79 | 18 | 68 | 73 | 28 |
| 44 | 32 | 57 | 62.5 | 96 | $31] ;$ |  |  |  |  |  |

s2 = ['data = ' filename ';'];
eva1(s2)
% Raw data manipulation
systems = [nonzeros(data(:,1)) find(data(:,1))];
systems_Margu7es3 = [nonzeros(data(:,1)) find(data(:,1))];
systems_Margules3 = [systems_Margules3; 1ength(systems_Margules3)+1
1ength(data(:,1))];
X = [];
X1mo1= [];
X2mol = [];
Y1mo] = [];
Y2mol = [];
GF1 = [];
GF2 = [];
Antoine1 = [];
Antoine2 = [];
Gammas1E = [];
Gammas2E = [];
Gammas1U = [];
Gammas2U = [];
P_exp = [];
T_exp = [];
Max = max(systems(:,1));
for i = 1:1ength(systems(:,1))
S = int2str(i);
M = num2str(Max);
%c1c
sysnumber = ['Manipulating data of system \#' S ' of ' M '.'];
disp(sysnumber);
% X, Y and Gammas matrices creation
% Margules equation parameters calculation
X1_Margules3 = [];
X2_Margules3 = [];
Y1_Margules3 = [];
Y2_Margules3 = [];
T_Margules3 = [];
P_Margules3 = [];
Antoine1_Margules3 = [];
Antoine2_Margules3 = [];
points_Margules3(i) = systems_Margu1es3(i+1,2) -
systems_Margules3(i,2) - 8;
x1_Margules3 =
data(systems_Margules3(i,2)+8:systems_Margules3(i,2)+8+points_Margu1
es3(i)-1,3)';
X2_Margules3 = 1-X1_Margules3;
Y1_Margules3 =
data(systems_Margules3(i,2)+8:systems_Margules3(i,2)+8+points_Margul
es3(i)-1,4)';

```
```

    Y2_Margules3 = 1-Y1_Margules3;
    T_Margules3 =
    data(systems_Margu7es3(i,2)+8:systems_Margu7es3(i,2)+8+points_Margu7
es3(i)-1,5)';
P_Margu7es3 =
data(systems_Margu7es3(i,2)+8:systems_Margu7es3(i,2)+8+points_Margu7
es3(i)-1,2)';
Gamma1U =
data(systems_Margules3(i,2)+8:systems_Margules3(i,2)+8+points_Margu1
es3(i)-1,6)';
Gamma2U =
data(systems_Margu7es3(i,2)+8:systems_Margu7es3(i,2)+8+points_Margu7
es3(i)-1,7)';
Antoine1_Margules3 =
[nonzeros(data(systems_Margules3(i,2)+2,:))'];
Antoine2_Margu7es3 =
[nonzeros(data(systems_Margules3(i,2)+3,:))'];
if
or(or(X1_Margules3(1)==0,Y1_Margules3(1)==0) , or(X1_Margu7es3(1)==1,Y
1_Margules3(1)==1)) == 1
X1_Margu7es3(1) = [];
X2_Margules3(1) = [];
Y1_Margules3(1) = [1;
Y2_Margules3(1) = [];
T_Margules3(1) = [];
P_Margules3(1) = [];
Gamma1u(1) = [];
Gamma2U(1) = [];
points_Margules3(i) = points_Margules3(i)-1;
else
end
if
or(or(X1_Margules3(points_Margules3(i))==0,Y1_Margules3(points_Margu
1es3(i))==0),or(X1_Margules3(points_Margules3(i))==1,Y1_Margules3(po
ints_Margules3(i))==1)) == 1
X1_Margules3(points_Margules3(i)) = [];
X2_Margules3(points_Margules3(i)) = [];
Y1_Margules3(points_Margules3(i)) = [];
Y2_Margules3(points_Margules3(i)) = [];
T_Margules3(points_Margules3(i)) = [];
P_Margules3(points_Margules3(i)) = [];
Gamma1U(points_Margules3(i)) = [];
Gamma2u(points_Margules3(i)) = [];
points_Margules3(i) = points_Margules3(i)-1;
else
end
% Calculate Gamma i experimental
Gamma1E_Margules3 =
(Y1_Margules3.*P_Margules3)./(X1_Margules3.*10.^(Antoine1_Margules3(
1)-(Antoine1_Margules3(2)./(T_Margules3+Antoine1_Margules3(3)))));
Gamma2E_Margules3 =
(Y2_Margules3.*P_Margules3)./(X2_Margules3.*10.^(Antoine2_Margules3(
1)-(Antoine2_Margules3(2)./(T_Margu\es3+Antoine2_Margu7es3(3)))));
GeRT_exp_Margules3 = (X1_Margules3.*log(Gamma1E_Margules3)) +
(X2_Margules3.*1og(Gamma2E_Margules3));
Gamma1E_Gamma2E = [Gamma1E_Margules3 Gamma2E_Margu1es3];
save expdata x1_Margules3 X2_Margules3 T_Margules3
Gamma1E_Margules3 Gamma2E_Margu1es3 GeRT_exp_Margules3
Gamma1E_Gamma2E
options = optimset('MaxFunEvals',1000,'MaxIter',1000);

```
```

    A0_Margules3 = [1;1;1];
    A_Margules3_fminunc(i,:) =
    fminunc('Createfun_Margules3',A0_Margules3);
Antoine1 = [Antoine1;Antoine1_Margules3];
Antoine2 = [Antoine2;Antoine2_Margules3];
Gammas1E = [Gammas1E;Gamma1E_Margules3'];
Gammas2E = [Gammas2E;Gamma2E-Margules3'];
X1mol = [x1mol;X1_Margules3'];
X2mol = [x2mol;x2_Margules3'];
Y1mol = [Y1mol;Y1_Margules3'];
Y2mol = [Y2mol;Y2_Margules3'];
Gammas1u = [Gammas1u;Gamma1U'];
Gammas2U = [Gammas2U;Gamma2U'];
P_exp = [P_exp;P_Margules3'];
T_exp = [T_exp;T_Margules3'];
P = data(systems(i,2)+8,2);
points = 0;
point = 0;
while P ~= 0
xpoint = 1;
ypoint = 1;
if data(systems(i,2)+point+8,3) == 0
xpoint = 0;
end
if data(systems(i,2)+point+8,4) == 0
ypoint = 0;
end
if data(systems(i,2)+point+8,3) == 1
xpoint = 0;
end
if data(systems(i,2)+point+8,4) == 1
ypoint = 0;
end
if and(xpoint,ypoint) == 1
points = points + 1;
else
end
point = point + 1;
P = data(systems(i,2)+8+point,2);
end
systems(i,3) = points;
NGF1 = length(nonzeros(data(systems(i,2)+4,:)));
NGF2 = length(nonzeros(data(systems(i,2)+6,:)));
[o,p] = size(X);
k = 1;
1 = 0;
% Suma de la cantidad total de interacciones.
sumINT (o+1) = 0;
sumINT (o+2) = 0;
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
sumINT (0+1) = sumINT (0+1) +
(data(systems(i,2)+5,r+1)*data(systems(i,2)+7,s+1));
sumINT(o+2) = sumINT(o+2) +
(data(systems(i,2)+5,r+1)*data(systems(i,2)+7,s+1));
else
end
end

```
end
\% 1) Posisionar el numero de la interacción.
for \(r=1\) :NGF1
for \(s=1:\) NGF2
if data(systems \((i, 2)+4, r+1) \sim=\) data (systems \((i, 2)+6, s+1)\)
GF1 = [GF1; data(systems (i, 2) \(+4, r+1)]\);
GF2 = [GF2; data(systems (i,2) \(+6, \mathrm{~s}+1)]\);
\(x(0+1,1+k)=g *(\operatorname{data}(\) systems \((i, 2)+4, r+1)-1)+\)
data(systems (i,2)+6, s+1);
\(\mathrm{x}(\mathrm{o}+2,1+\mathrm{k})=\mathrm{g} *(\operatorname{data}(\) systems \((\mathrm{i}, 2)+6, \mathrm{~s}+1)-1)+\)
data(systems (i,2)+4,r+1); \(1=1+8 ;\)
e1se end
end
end
\(\mathrm{k}=\mathrm{k}+1\);
\(1=0\);
\% 2) Posisionar la Temperatura del sistema.
if systems \((i, 1)>943\)
for \(r=1\) :NGF1
for \(s=1:\) NGF2
if data(systems \((i, 2)+4, r+1) \sim=\) data(systems \((i, 2)+6, s+1)\)
X (0+1,1+k) = mean(T_Margules3);
\(\mathrm{x}(0+2,1+\mathrm{k})=\) mean(T_Margules3);
\(1=1+8\);
else
end
end
end
elseif systems(i,1) > 921
for \(r=1\) :NGF1
for \(s=1:\) NGF2
if data(systems \((i, 2)+4, r+1) \sim=\) data (systems \((i, 2)+6, s+1)\) \(\mathrm{X}(0+1,1+\mathrm{k})=\) mean(T_Margu1es3)-273.15;
\(\mathrm{X}(\mathrm{o}+2,1+\mathrm{k})=\) mean(T_Margules3)-273.15; \(1=1+8 ;\)
e1se
end

\section*{end}
end
else
for \(r=1\) :NGF1 for \(s=1:\) NGF2
if data (systems \((i, 2)+4, r+1) \sim=\) data (systems \((i, 2)+6, s+1)\) \(\mathrm{X}(\mathrm{o}+1,1+\mathrm{k})=\) mean (T_Margules3) ; X \((0+2,1+k)=\) mean(T_Margules3); \(1=1+8 ;\)
else
end
end
end
end
\(k=k+1\);
\(1=0\);
\% 3)Posisionar la Presión de1 sistema.
if systems (i,1) > 943
for \(r=1:\) NGF1
for \(s=1: N G F 2\)
```

        if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
                        X(0+1,1+k) = mean(P_Margules3);
                        X(0+2,1+k) = mean(P_Margules3);
                    1 = 1 + 8;
            else
                    end
            end
        end
    elseif systems(i,1) > 921
        for r = 1:NGF1
        for s = 1:NGF2
            if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
                    X(o+1,1+k) = mean(P_Margu7es3) * 7.500617;
                    x(0+2,1+k) = mean(P_Margu1es3) * 7.500617;
                    1 = 1 + 8;
                else
                end
        end
        end
    else
    for r = 1:NGF1
        for s = 1:NGF2
            if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
                X(0+1,1+k) = mean(P_Margu7es3);
                X(0+2,1+k) = mean(P_Margules3);
                    1 = 1 + 8;
            else
            end
        end
    end
    end
    k = k + 1;
    1 = 0;
    % 4)Posisionar la cantidad de GF de la molécula \#1 en la
interacción.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
x(0+1,1+k) = data(systems(i,2)+5,r+1);
X(o+2,1+k) = data(systems(i,2)+7,s+1);
1 = 1 + 8;
else
end
end
end
k = k + 1;
1 = 0;
% 5)Posisionar la cantidad de GF de la molécula \#2 en la
interacción.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
x(0+1,1+k) = data(systems(i, 2)+7,s+1);
x(0+2,1+k) = data(systems(i,2)+5,r+1);
1 = 1 + 8;
else
end
end
end
k = k + 1;

```
```

    1 = 0;
    sumMW1 = 0;
    sumMW2 = 0;
    % 6)Posisionar el peso molecular del grupo funcional de la molécula
    \#1.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
x(0+1,1+k) =
data(systems(i,2)+5,r+1)*MW(data(systems(i,2)+4,r+1));
x(0+2,1+k) =
data(systems(i,2)+7,s+1)*MW(data(systems(i,2)+6,s+1));
1 = 1 + 8;
else
end
end
sumMW1 = sumMW1 +
data(systems(i,2)+5,r+1)*MW(data(systems(i,2)+4,r+1));
end
k = k + 1;
1 = 0;
% 7)Posisionar el peso molecular del grupo funcional de la molécula
\#2.
for s = 1:NGF2
for r = 1:NGF1
if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
x(0+1,1+k) =
data(systems(i, 2)+7,s+1)*MW(data(systems(i,2)+6,s+1));
data(systems(i,2)+5,r+1)*MW(data(systems(i,2)+4,r+1));
1 = 1 + 8;
else
end
end
sumMW2 = sumMW2 +
data(systems(i,2)+7,s+1)*MW(data(systems(i,2)+6,s+1));
end
k = k + 1;
1 = 0;
% 8)Posisionar 1
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+4,r+1) ~= data(systems(i,2)+6,s+1)
x(o+1,1+k) = 1;
x(o+2,1+k) = 1;
1 = 1 + 8;
else
end
end
end
k = k + 1;
1 = 0;
end
disp('End of experimental data manipulation process!')
disp('Matrices X Y and Gammas had been created succesfully!')
disp('Saving data matrices to file Databasenew_Margules3.mat')
save Databasenew_Margules3 x X1mol X2mol Y1mol Y2mol systems
Antoine1 Antoine2 Gammas1E Gammas2E Gammas1U Gammas2U sumINT
A_Margules3_fminunc P_exp T_exp
disp('Data had been save succesfully!')

```
```

\% Program Createfun_Margules3.m
\% This program will determine the Margules constants A, B and C for
1iquid
\% binary systems.
function SSE = Createfun_Margules3(A)
load expdata
A1 = A(1);
$B=A(2)$;
$\mathrm{C}=\mathrm{A}(3)$;
X1 = X1_Margules3;
X2 = X2_Margules3;
GeRT = (A1+B.* $(X 1-X 2)+C . *(X 1-X 2) . \wedge 2)$;
Gamma1M $=\exp (((A 1+3 * B+5 * C) . *(X 2 . \wedge 2))-$
$((4 *(B+4 * C)) . *(X 2 . \wedge 3))+((12 * C) . *(X 2 . \wedge 4)))$;
Gamma2M $=\exp (((A 1-3 * B+5 * C) . *(X 1 . \wedge 2))+((4 *(B-$
$4 * C)) . *(X 1 . \wedge 3))+((12 * C) . *(X 1 . \wedge 4)))$;
Gamma1_Gamma2 = [Gamma1M Gamma2M];
de1ta = Gamma1_Gamma2 - Gamma1E_Gamma2E;
SSE = diag(de1ta * de7ta');

```

The second MatLab program developed was called NNvsUNIFAC.m and it purpose is to search and choose the required vapor-liquid equilibrium experimental data within the information matrix, create the training matrices, train the neural network, predict the Margules parameters and, calculate the activity coefficients using the foursuffix Margules equation. The following diagram shows the algorithm developed to perform the mentioned tasks.


Figure 32. Algorithm flowchart for NNvsUNIFAC.m
The program saves the predicted activity coefficients and plots a graph comparing the results given by the ANN and UNIFAC methods with the experimental data. The MatLab code for program NNvsUNIFAC.m is presented below.
\%Program NNvsUNIFAC.m
\% This program will compare the results of predicting the activity coefficients using the UNIFAC
\(\%\) and the Neural Networks methods based on the experimental data taken from DECHEMA series.
clear
clc
close all
warning off all
totalsys = 1000;
Predsys1 = [];
Predsys2 = [];
\% specify system(s) to be evaluated
\% evalsys = [960 954955957944950951948 949];
\(\%\) evalsys \(=\left[\begin{array}{llllllllll}22 & 50 & 74 & 202 & 358 & 366 & 550 & 736 & 771 & 772\end{array}\right] ;\)
evalsys = input('Enter the experimental data system number:');
for loop \(=1: 1\) ength (evalsys)
sys = evalsys(loop);
tic \% Start time counter.
\% Load the experimental database file from DECHEMA.
load Databasenew_Margules3.mat
sse3 = [];
[f,c] = size(x1mol);
\% Determine systems data position in Matrix x .
systems \((1,4)=1\);
systems \((1,5)=1\);
for \(\mathrm{i}=2: 1\) ength (systems (:, 1 )
            systems \((i, 4)=\operatorname{systems}(i-1,4)+2\);
            systems(i,5) \(=\operatorname{systems}(i-1,5)+\operatorname{systems}(i-1,3)\);
        end
        A-Margules3_eval = [];
        tfsys = [];
        nneusys = [];
        Gammaspred = [];
        Gammast = [];
        errorssys = [];
        Xevalc = [];
        Xeval = [];
        Xexp = [];
        Yeval = [];
        Y1exp =
        Y2exp = [];
        Peval = [];
        Pexp = [];
        Teval = [];
        Texp = [];
        Gamma1Ueval = [];
        Gamma2Ueval = [];
        Antoine1eval = [];
        Antoine2eval = [];
        TPeval = [];
        TPexp = [];
        x1eval = [];
        x2eva1 = [];
        x1x2exp = [];
        Gammaseval = [];
        Gammasexp = [];
```

    systemseval = [];
    systemsexp = [];
    IntXeval1 = [];
    IntXeva12 = [];
    S = num2str(sys);
    sysnumber = ['Evaluating system #' s '.'];
    disp(sysnumber);
    Xeva1 = X(systems(sys,4):systems(sys,4) + 1,:); % Matriz de
    evaluacion = sistema extraido.
IntXeva1 = Xeva1(:,1:8:1ength(Xeva1(1,:)));
Xevalc = X(systems(sys,4):systems(sys,4) +
1,1:8*1ength(nonzeros(IntXeva1(1,:)))); % Matriz de evaluacion con
la cantidad de interacciones de1 sistema a ser extraido.
Xexp = X (1:2*921, :);
Y1eval = Y1mol(systems(sys,5):systems(sys,5) + systems(sys,3) -
1); % vector de fracciones molares de fase vapor de1 sistema a
extraer.
Y2eval = Y2mol(systems(sys,5):systems(sys,5) + systems(sys,3) -
1); % vector de fracciones molares de fase vapor de1 sistema a
extraer.
Y1exp = Y1mol(1:f-740);
Y2exp = Y2mol(1:f-740);
Peval = X(systems(sys,4),3);
Peva1_Y = P_exp(systems(sys,5):systems(sys,5) + systems(sys,3)-
1);
Pexp = x (1:2*921,3);
Teval = X(systems(sys,4),2);
Teval_Y = T_exp(systems(sys,5):systems(sys,5) + systems(sys,3)-
1);
Texp = X(1:2*921,2);
Gamma1Ueva1 = Gammas1U(systems(sys,5):systems(sys,5) +
systems(sys,3) - 1);
Gamma2Ueva1 = Gammas2U(systems(sys,5):systems(sys,5) +
systems(sys,3) - 1);
Antoine1eval = Antoine1(sys,:);
Antoine2eva1 = Antoine2(sys,:);
A_Margules3_eva1 = A_Margu7es3_fminunc(sys,:);
sumINTexp = sumINT(1:2*921); % vector de cantidad de
interacciones de1 sistema a extraer.
sumINTeva1 = sumINT(systems(sys,4):systems(sys,4) + 1);
X1eva1 = X1mol(systems(sys,5):systems(sys,5) + systems(sys,3) -
1);
X2eva1 = X2mo1(systems(sys,5):systems(sys,5) + systems(sys,3) -
1);
Gammas1Eeva1 = Gammas1E(systems(sys,5):systems(sys,5) +
systems(sys,3) - 1); % Vector de coeficientes de actividad
experimentales del sistema a extraer.
Gammas2Eeva1 = Gammas2E(systems(sys,5):systems(sys,5) +
systems(sys,3) - 1); % vector de coeficientes de actividad
experimentales de1 sistema a extraer.
Gammas1Eexp = Gammas1E(1:f-740);
Gammas2Eexp = Gammas2E(1:f-740);
systemseval = systems(sys,:); % Matriz de informacion de1
sistema a extraer.
systemsexp = systems(1:7ength(systems(:,1))-39,:);
IntXeval1 = Xevalc(1,1:8:1ength(Xevalc(1,:))); % Interacciones
en Xevalc parte de Gammal.
IntXeval1 = reshape(IntXeva11,1,prod(size(IntXeva11))); %
Arreglo de las interacciones en un solo vector.

```

IntXeva11 = unique(nonzeros(IntXeva11)); \% Interacciones presentes en el sistema de interes para determinar Gammal. IntXeva12 \(=\) Xevalc(2,1:8:1ength(Xevalc(2,:))); \% Interacciones en Xevalc parte de Gamma2.

IntXeval2 = reshape(IntXeval2,1,prod(size(IntXeva12))); \% Arreglo de las interacciones en un solo vector.

IntXeval2 = unique(nonzeros(IntXeva12)); \% Interacciones presentes en el sistema de interes para determinar Gamma2.
\% Training Matrices Creation
message = ['Creating Training Matrices for system 's '!'];
disp(message);
Xe1 = []; \% Experimental Data Training Matrix for Gamma1.
TG1 = []; \% Targets Matrix for Gamma1.
TA1 = [];
TY1 = [];
T1 = [];
P1 = [];
sumINTe1 = [];
sumINTe2 \(=[] ;\)
monitor1 \(=[] ;\)
Xe2 = []; \% Experimental Data Training Matrix for Gamma2.
TG2 \(=\) []; \% Targets Matrix for Gamma2.
TA2 \(=\) [];
TY2 \(=\) [];
T2 = [];
\(\mathrm{P} 2=\) [];
monitor2 = [];
\([f, c]=\operatorname{size}(X e x p) ; \%\) Experimental Matrix rows and columns.
int \(=c / 8 ; \%\) Maximum number of interactions for systems in the Experimental Matrix.
[fp,cp] = size(Xevalc); \% Evaluation Matrix rows and columns.
intp \(=c p / 8 ; \%\) Number of interactions for the system of interest.
\% Training Matrix Creation for Gammal
monitor1 = zeros(1,1ength(IntXeva11));
L = 1;
\(o=0 ;\)
\(\mathrm{p}=0\);
\(\mathrm{S}=0 ;\)
\(\mathrm{t}=0\);
SysXe1 \(=\) []; \% Chosen systems matrix to determine Gamma1.
sysXe2 = []; \% Chosen systems matrix to determine Gamma2.
 systems in the Experimental Matix.
\(\mathrm{s}=\mathrm{s}+1\);
\(\mathrm{t}=\mathrm{t}+1\);
while \(s<=2\)
\(p=0 ;\)
for \(j=1\) :intp
\(L=1\);
if \(s\) <= 2
for \(m=1: i n t\)
if and \((\operatorname{Xexp}(t, L)==\)
IntXeval1(j), monitor1(j)<totalsys)
\(0=0+1 ;\)
monitor1 \((j)=\) monitor1 \((j)+1\);
SysXe1(o,:) = systemsexp(i,:);
\(\operatorname{Xe1}(\mathrm{o},:)=\operatorname{Xexp}(\mathrm{t},:) ;\)
```

                        TG1(o) = Gammas1Eexp(t);
                        TA1(o,:) = A_Margules3_fminunc(i,:);
                        TY1(o) = Y1exp(t);
                        T1(o) = Texp(t);
                    P1(o) = Pexp(t);
                        sumINTe1(o) = sumINTexp(t);
                        L = 1;
                        p = 1;
                    break
                            else
                                    L = L + 8;
                                    end
            end
            else
            break
            end
            if p == 1
            break
            end
            end
            s = s + 1;
            t = t + 1;
        end
        s = 0;
        t = t - 1;
    end
    % Training Matrix Creation for Gamma2
    monitor2 = zeros(1,1ength(IntXeva12));
    L = 1;
    o = 0;
    p = 0;
    S = 0;
    t = 0;
    for i = 1:length(systemsexp(:,1)) % Evaluation of al1 available
    systems in the Experimental Matix.
s = s + 1;
t = t + 1;
k = 1;
while s <= 2
p = 0;
k = 1;
for j'= 1:intp
L = 1;
if s <= 2
for m = 1:int
if and (Xexp (t,L) ==
IntXeva12(j),monitor2(j)<totalsys)
0 = 0 + 1;
monitor2(j) = monitor2(j)+1;
SysXe2(o,:) = systemsexp(i,:);
xe2(o,:) = xexp(t,:);
TG2(o) = Gammas2Eexp(t);
TA2(o,:) = A_Margules3_fminunc(i,:);
TY2(o) = Y2 exp(t);
T2(o) = Texp(t);
P2(o) = Pexp(t);
sumINTe2(o) = sumINTexp(t);
L = 1;
p = 1;

```

> break else
\% Training Matrices manipulation and re-arrangement
if isempty (Xe2) == 0
Xe12 = [Xe1 Xe2];
Xeval12 \(=[\operatorname{Xevalc}(1,:)\) Xevalc \((2,:)]\);
sumINTe12 \(=\) sumINTe1 + sumINTe2;
sumINTeval12 = sumINTeval (1) + sumINTeval (2);
IntXe12 = Xe12(:,1:8:1ength (Xe12(1,:))); \% Interactions in
Xe12.
IntXe12 = reshape(IntXe12,1,prod(size(IntXe12))); \% Rearrangement in one vector for interaction in Xe12.

IntXeval12 = Xeval12(1,1:8:1ength(Xeva112(1,:))); \%
Interactions in Xeval12 to determine margules equation parameters.
IntXeval12 = reshape(IntXeva112,1,prod(size(IntXeva112))); \%
Re-arrangement in one vector for interactions in Xeval12.
Intjun12 =
unique(union(nonzeros(IntXe12)', nonzeros(IntXeva112)')); \% Al1 interactions toghether.

Xe12mod \(=\) zeros (1ength (Xe12 (:,1)),1ength(Intjun12)*8); \% Initialization for Modified Experimental Matrix.

Xeval12mod \(=\) zeros \((1,1\) ength(Intjun12)*8); \% Initialization for Modified Evaluation Matrix.
\% Verifing that all interactions from the system of interest
are
\% present in the Experimental Matrix
IntXe12 = unique(nonzeros(IntXe12)); \% Interactions present
in the experimental data to determine margules parameters.
IntXeval12 = unique(nonzeros(IntXeva112)); \% Interactions
present in the system of interest to determine Margules parameters.
tf12 = ismember (IntXeval12, IntXe12); \% Interactions from the system of interest present in the experimental data to determine Margules parameters.

Intfound12 = sum(tf12); \% Interactions from the system of interest found in the experimental data to determine Margules parameters.

Ints12 = length(tf12); \% Interactions from the system of interest available to determine Margules parameters.

Match12(sys,:) = [Intfound12 Ints12]; s12 = 0;
\% Modifying evaluation and experimental variables to align
\% interactions data
for \(i=1: 1\) ength (nonzeros (SysXe1 (:,1)))
for \(j=1: 8: 7 \mathrm{ength}(\operatorname{Xe} 12(1,:))\)
u12 \(=\) find \((i\) smember \((\) Int jun \(12, x e 12(s 12+1, j))\) );
if \(\mathrm{Xe} 12(\mathrm{~s} 12+1, \mathrm{j})=0\)
else
xe12mod(s12+1,8*u12-7:8*u12) = Xe12(s12+1,j:j+7);
end
end
s12 = s12 + 1;
end
for \(\mathrm{j}=1: 8: 1\) ength \((X e v a 112(1,:))\)
ueval12 \(=\) find (ismember (Intjun12, Xeval12 \((1, j))\) );
if \(\operatorname{Xeval12(1,j)}=0\)
else
Xeva112mod(:,8*ueva112-7:8*ueva112) =
Xeval12(1,j:j+7);
end
end
datapoints(loop) = sum(SysXe1(:,3));
\% Extracting excess data from Experimental Training Matrices \(\mathrm{j}=0\);
PG12 = []; \% Training Matrix with only information to be
used to determine Mergules parameters.
PG12 = [T1', P1'];
for \(i=1\) : 1 ength (Intjun12)
PG12 =
[PG12, (Xe12mod(:, \(\mathrm{j}+4) . * X e 12 \bmod (:, j+5)) . / s u m I N T e 12 '] ;\)
\(j=j+8 ;\)
end
\% Extracting excess data from Evaluation Training Matrices \(\mathrm{j}=0\);
SG12 = []; \% Evaluation Matrix with only information to be
used to determine'margules parameters.
SG12 = [Teval,Peval];
for \(i=1: 1\) length (Intjun12)
SG12 =
[SG12, (Xeva112mod(:,j+4).*Xeva112mod(:,j+5))./sumINTeva112(1)'];
\(j=j+8 ;\)
end
TGeval1 = Gammas1Eeval(1:systemseval(1,3)); \% Targets Matrix
for Gamma1.
TGeval2 = Gammas2Eeval(1:systemseval(1,3)); \% Targets Matrix
for Gamma2.
TYeval1 = Y1eval (1:systemseval \((1,3)\) );
TYeval2 = Y2eval (1: systemseval \((1,3)\) );
PG12 = PG12';
SG12 = SG12';
TA1 = TA1';
\% Neural Networks Training
[fPG1 CPG1] = size(PG12);
[fTA1 cTA1] = size(TA1);
P11 = PG12 (:,1:ceil(cPG1/2));
P21 = PG12 (: ', ceil(cPG1/2)+1: ©PG1);
T11 = TA1 (: \(1:\) :ceil(cTA1/2));
T21 = TA1 (:, cei1 (cTA1/2) \(+1:\) cTA1) ;
P31 = SG12;
```

    T31 = A_Margules3_eva1';
    n2 = 3;
    pp1 = [P11 P21];
    tt1 = [T11 T21];
    mmax1 = minmax(PG12);
    pack
    b111 =
    w111 =
    b121 = [];
    w121 = [];
    e = [];
    a31 = [];
    max_n = 5;
    % NN Optimum Structure Search
tf = {'logsig' 'purelin'};
for i = 1:9
disp(i)
e1 = [];
for j = 1:max_n % Hidden layer optimum number of neurons

```
search.
nneu \(=\) [j n2];
net1 \(=\) newff(mmax1, nneu,tf);
net1.trainParam.show = NaN; \%Instruction to disable
training graphics.
net1.trainParam.mem_reduc \(=4\); \%Instruction to reduce
memory requirement for Jacobian Matrix calculation.
                        [net1 tr1] = train(net1,P11,T11);
a1 = sim(net1,P21);
e1 (j,: ) = mean (T21 - a1);
pack \% Instruction to reduce memory space used for
variables.
    end
    SSE1 = diag(e1 * e1');
    [m1 pos1] = min(SSE1);
    nno1(loop) = pos1;
    nneu1 = [nno1(1oop) n2];
    a1 = [];
    app1 = [];
    e1 = [];
    \% Optimum initial point search
    for \(k=1: 20\)
        net1 = newff(mmax1, nneu1,tf);
        net1.trainParam.show = NaN;
        net1.trainParam.mem_reduc \(=4\);
        [net1 tr1] = train(net1, pp1, tt1);
        eval(['b11', num2str(k),' = net1.b\{1,1\};'])
        eval (['b21', num2str(k),' = net1.b\{2,1\};'])
        eval (['w11', num2str(k),' = net1.iw\{1,1\};'])
        eval(['w21',num2str(k)',' = net1.1w\{2,1\};'j)
        a1(:,:,k) = sim(net1,pp1);
        e1(k,:) = mean(tt1 - a1(:,:,k));
        pack
        end
        SSE1 = diag(e1 * e1');
        [m1 piol] = min(SSE1);
        net1 = newff(mmax1, nneu1, tf);
        eval (['net1.b\{1,1\} = b11', num2str (pio1), ';'])
    eval (['net1.b\{2,1\} = b21', num2str(pio1),'';'])
    eval (['net1. iw \(\{1,1\}=\) w11', num2str(piol), ', ;'])
    eval(['net1.7w\{2,1\} = w21',num2str(pio1),';'])
```

            net1.trainParam.show = NaN;
            net1.trainParam.mem_reduc = 4;
            [net1 tr1] = train(net1,pp1,tt1);
            app1 = sim(net1,pp1);
            a31(i,:) = sim(net1,P31);
    end
            % Final results determination based on data central tendency.
            aSG1 = sort(a31);
            for e = 1:2
            aSG1(1,:) = [];
    end
    for e = 7:-1:6
            asG1(e,:) = [];
    end
    aSG1med = mean(aSG1);
    A_NN = aSG1med(1);
    B_NN = aSG1med(2);
    C_NN = aSG1med(3);
    Gamma1M = exp(((A_NN+3*B_NN+5*C_NN).*(X2eval.^2))-
    ((4*(B_NN+4*C_NN)).*(X2eval.^3))+((12*C_NN).*(X2eval.^4)));
Gamma2M = exp(((A_NN-3*B_NN+5*C_NN).*(x1eva1.^2))+((4*(B_NN-
4*C_NN)).*(X1eval.^3))+((12*C_NN).*(X1eval.^4)));
eSG1 = TGeva11 - Gamma1m;
eSG2 = TGeva12 - Gamma2M;
% Data Plot and Saving
timett1 = 1:length(TG1)
time31 = 1:1ength(TGeva11);
eU1 = TGeva11 - Gamma1Ueva1;
eU2 = TGeva12 - Gamma2Ueva1;
Y1predANN = ((X1eval.*10.^(Antoine1eval(:,1)'-
(Antoineleval(:,2)'./((Teval_Y)+Antoine1eval(:,3)')))).*Gamma1M)./(P
eval_Y);
Y2predANN = ((X2eval.*10.^(Antoine2eval(:,1)'-
(Antoine2eval(:,2)'./((Teval_Y)+Antoine2eval(:,3)')))).*Gamma2M)./(P
eval_Y);
Y1predU = ((X1eva1.*10.^(Antoine1eval(:,1)'-
(Antoine1eval(:,2)'./((Teval_Y)+Antoine1eval(:,3)')))).*Gamma1Ueval)
./(Peval_Y);
Y2predu = ((X2eval.*10.^(Antoine2eval(:,1)'-
(Antoine2eval(:,2)'./((Teval_Y)+Antoine2eval(:,3)')))).*Gamma2Ueva1)
./(Peval_Y);
eva1(['figure(',num2str(sys),num2str(tota1sys),')'])
subplot(2,2,1)
p1ot(X1eval,TYeva11,'k',X1eval,Y1predANN,'g',X1eval,Y1predU,'r')
tit1e(['System: Methanol(1) + n-Propyl Acetate (2)'])
legend('Exp','ANN','UNIFAC')
xlabel('x1');
ylabel('Y1');
subplot(2,2,2)
plot(X1eval,TGeval1,'k',x1eval,Gamma1m,'g',X1eval,Gamma1Ueva1,'r')
legend('Exp','ANN','UNIFAC')
xlabel('x1');
y7abe1('Gamma1');
subplot(2,2,3)
p1ot(X2eval,TYeva12,'k',X2eva1,Y2predANN,'g',X2eval,Y2predu,'r')

```
```

    legend('Exp','ANN','UNIFAC')
    xlabe1('x2');
    y1abe1('Y2');
    subp1ot(2,2,4)
    p1ot(X2eva1,TGeva12,'k',X2eva1,Gamma2m,'g',X2eva1,Gamma2Ueva1,'r')
legend('Exp','ANN','UNIFAC')
xlabe1('x2');
ylabe1('Gamma2');
toc
time(loop) = toc;
eva1(['save system',num2str(sys),'_Margules3.txt Gamma1Ueva1
TGeva11 X1eva1 aSG1med Gamma1M Gamma2Ueva1 TGeva12 X2eva1 aSG1
Y1predANN Y2predANN Y1predU Y2predU time -ascij'])
Predsys1 =
[Predsys1; sys.*ones(1ength(Gamma1M) , 1),Gamma1M,Gamma1Ueva1,TGeva11];
Predsys2 =
[Predsys2;sys.*ones(1ength(Gamma2M) , 1),Gamma2M,Gamma2Ueva1 ,TGeva12];
end
end

```

The third MatLab program was called Gamma_ANN_user.m and it purpose is to provide the users with the tool for using the ANN method for predicting activity coefficients for their own systems. This program uses the function Create_Gamma_user.m that creates the required matrices from the system of interest data to be used as input for predicting the activity coefficients using the ANN method. The instructions for using the program Gamma_ANN_user.m are as follow:
1) Create the system of interest data file in a Microsoft Excel spreadsheet following the format specified in Table 35. Use the functional groups table in Appendix B to assign the functional groups numbers.

Table 35. System of interest data spreadsheet format
\begin{tabular}{|c|c|c|c|c|c|c|c|}
\hline System \# & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\
\hline 0 & A1 & B1 & C1 & 0 & 0 & 0 & 0 \\
\hline 0 & A2 & B2 & B3 & 0 & 0 & 0 & 0 \\
\hline 0 & G11 & G12 & G13 & G14 & G15 & G16 & G17 \\
\hline 0 & n 11 & n 12 & n 13 & n 14 & n 15 & n 16 & n 17 \\
\hline 0 & G21 & G22 & G23 & G24 & G25 & G26 & G27 \\
\hline 0 & n21 & n22 & n23 & n24 & n25 & n26 & n27 \\
\hline 0 & T1 & P1 & X1 & 0 & 0 & 0 & 0 \\
\hline 0 & T2 & P2 & X2 & 0 & 0 & 0 & 0 \\
\hline 0 & T3 & P3 & X3 & 0 & 0 & 0 & 0 \\
\hline 0 & T4 & P4 & X4 & 0 & 0 & 0 & 0 \\
\hline 0 & T5 & P5 & X5 & 0 & 0 & 0 & 0 \\
\hline 0 & T6 & P6 & X6 & 0 & 0 & 0 & 0 \\
\hline 0 & Tn & Pn & Xn & 0 & 0 & 0 & 0 \\
\hline 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\
\hline
\end{tabular}

This table presents the format used to organize the system of interest data.

Where,
System \# is the data system number.
\(A 1, B 1\) and C1 are the Antoine constants for molecule 1.
\(A 2, B 2\) and \(C 2\) are the Antoine constants for molecule 2.
G11 to G17 are the number of the functional groups for molecule 1.
n11 to n17 are the quantity of each functional group for molecule 1 .
G21 to G27 are the number of the functional groups for molecule 2 .
\(n 21\) to \(n 27\) are the quantity of each functional group for molecule 2.
\(T 1\) to Tn are the system temperature for each data point.
P1 to Pn are the system pressure for each data point.
Xl to Xn are the liquid mol fraction for molecule 1 for each data point.
2) Run the MatLab program Gamma_ANN_user.m by typing the program name without the ".\(m\) " extension at the MatLab command window and pressing Enter.
3) The program will ask for the system of interest data file name. Type the system of interest data file name without the ". \(x l s\) " extension and press Enter.
4) The program will ask for the molecules names. Type the name of the first molecule and press Enter. Then, type the name of the second molecule and press Enter.
5) The program will predict the activity coefficients using the ANN method and at the end it will save the results in the same file created to store the data for the system of interest but in a different worksheet called Output1. Also the program plots a graph of the predicted activity coefficients vs. the liquid molar fraction and the predicted vapor molar fraction of each molecule vs. its respective liquid molar fraction.

The MatLab code for program Gamma_ANN_user.m and function
Create_Gamma_user.m is presented below.
\%Program Gamma_ANN_user.m
\%This program will predict the activity coefficients using the \%the Neural Networks method.
clear
clc close all
\% Load the data file where user data is contain. userdata = input('Enter your data file name:','s'); Create_Gamma_user(userdata);
userdata = [userdata '.x1s'];
load database_user.mat
disp('User data have been processed and loaded!') warning off all
totalsys = 1000;
Predsys1 = [];
Predsys2 = [];
\% Specify system(s) to be evaluated
evalsys = systems_user(:,1);
```

    for loop = 1:length(evalsys)
    Header = [];
    Data = [];
    Molecule1 = [];
    Molecule2 = [];
    Molecule1 = input('Enter the name of molecule (1):','s');
    Molecule2 = input('Enter the name of molecule (2):','s');
    sys = evalsys(loop);
    tic % Start time counter.
    % Load the experimental database file from DECHEMA.
    load Databasenew_Margules3.mat
    sse3 = [];
    [f,c] = size(x1mol);
    % Determine systems data position in Matrix x.
    systems(1,4) = 1;
    systems(1,5) = 1;
    systems_user(1,4) = 1;
    systems_user(1,5) = 1;
    for i = 2:1ength(systems(:,1))
        systems(i,4) = systems(i-1,4) + 2;
        systems(i,5) = systems(i-1,5) + systems(i-1,3);
    end
    if lengthh(evalsys) > 1
        for i = 2:1ength(systems_user(:,1))
                systems_user(i,4) = systems_user(i-1,4) + 2;
                systems_user(i,5) = systems_user(i-1,5) + systems_user(i-
    1,3);
end
else
end
A_Margules3_eval = [];
tfsys = [];
nneusys = [];
Gammaspred = [];
GammasT = [];
errorssys = [];
Xevalc = [];
Xeval =[];
xexp = [];
Yeva1 =
Y1exp =
Y2exp = [];
Peval = [];
Pexp = [];
Teval = [];
Texp = [];
Antoineleval = [];
Antoine2eval = [];
TPeva1 = [];
TPexp = [];
x1eval =
x2eva1 = [];
x1x2exp = [];
Gammaseval = [];
Gammasexp = [];
systemseva1 = [];
systemsexp = [];
IntXeval1 = [];
IntXeval2 = [];
S = num2str(sys);

```
```

    sysnumber = ['Evaluating system #' S '.'];
    disp(sysnumber);
    Xeva1 = X_user(systems_user(sys,4):systems_user(sys,4) + 1,:);
    % Matriz de evaluacion = sistema extraido.
IntXeva1 = Xeva1(:,1:8:1ength(Xeva1(1,:)));
Xevalc = X_user(systems_user(sys,4):systems_user(sys,4) +
1,1:8*1ength(nonzeros(IntXeval(1,:)))); % Matriz de evaluacion con
1a cantidad de interacciones del sistema a ser extraido.
Xexp = X (1:2*921,:);
Y1exp = Y1mol(1:f-740);
Y2exp = Y2mo1(1:f-740);
Peva1 = X_user(systems_user(sys,4),3);
Peval_Y = P_exp_user(systems_user(sys,5):systems_user(sys,5) +
systems_user(sys,3)-1);
Pexp = X(1:2*921,3);
Teva1 = X_user(systems_user(sys,4),2);
Teva1_Y = T_exp_user(systems_user(sys,5):systems_user(sys,5) +
systems_user(sys,3)-1);
Texp = X (1:2*921,2);
Antoineleval = Antoine1_user(sys,:);
Antoine2eval = Antoine2_user(sys,:);
sumINTexp = sumINT(1:2*921); % Vector de cantidad de
interacciones de1 sistema a extraer.
sumINTeva1 =
sumINT_user(systems_user(sys,4):systems_user(sys,4) + 1);
X1eva1 = X1mol_user(systems_user(sys,5):systems_user(sys,5) +
systems_user(sys,3) - 1);
X2eva1 = X2mo1_user(systems_user(sys,5):systems_user(sys,5) +
systems_user(sys,3)- - 1);
Gammas1Eexp = Gammas1E(1:f-740);
Gammas2Eexp = Gammas2E(1:f-740);
systemseval = systems_user(sys,:); % Matriz de informacion de1
sistema a extraer.
systemsexp = systems(1:1ength(systems(:,1))-39,:);
IntXeva11 = Xevalc(1,1:8:1ength(Xevalc(1,:))); % Interacciones
en Xevalc parte de Gamma1.
IntXeva11 = reshape(IntXeva11,1,prod(size(IntXeva11))); %
Arreglo de las interacciones en un solo vector.
IntXeva11 = unique(nonzeros(IntXeva11)); % Interacciones
presentes en el sistema de interes para determinar Gammal.
IntXeval2 = Xevalc(2,1:8:1ength(Xevalc(2,:))); % Interacciones
en Xevalc parte de Gamma2.
IntXeva12 = reshape(IntXeva12,1,prod(size(IntXeva12))); %
Arreglo de las interacciones en un solo vector.
IntXeva12 = unique(nonzeros(IntXeva12)); % Interacciones
presentes en el sistema de interes para determinar Gamma2.
% Training Matrices Creation
message = ['Creating Training Matrices for system ' s '!'];
disp(message);
Xe1 = []; % Experimental Data Training Matrix for Gamma1.
TG1 = []; % Targets Matrix for Gamma1.
TA1 = [];
TY1 = [];
T1 = [];
P1 = [];
sumINTe1 = [];
sumINTe2 = [];
monitor1 = [];
Xe2 = []; % Experimental Data Training Matrix for Gamma2.

```
```

    TG2 = []; % Targets Matrix for Gamma2.
    TA2 = [];
    TY2 = [];
    T2 = [];
    P2 = [];
    monitor2 = [];
    [f,c] = size(Xexp); % Experimental Matrix rows and columns.
    int = c/8; % Maximum number of interactions for systems in the
    Experimental Matrix.
[fp,cp] = size(Xevalc); % Evaluation Matrix rows and columns.
intp = cp/8; % Number of interactions for the system of
interest.
% Training Matrix Creation for Gamma1
monitor1 = zeros(1,1ength(IntXeva11));
L = 1;
o = 0;
p = 0;
s = 0;
t = 0;
SysXe1 = []; % Chosen systems matrix to determine Gamma1.
SysXe2 = []; % Chosen systems matrix to determine Gamma2.
for i = 1:1ength(systemsexp(:,1)) % Evaluation of al1 available
systems in the Experimental Matix.
s = s + 1;
t = t + 1;
while s <= 2
p = 0;
for j = 1:intp
L = 1;
if s <= 2
for m = 1:int
if and(Xexp(t,L) ==
IntXeva11(j),monitor1(j)<totalsys)
o = o + 1;
monitor1(j) = monitor1(j)+1;
SysXe1(o,:) = systemsexp(i,:);
Xe1(o,:) = Xexp(t,:);
TG1(o) = Gammas1Eexp(t);
TA1(o,:) = A_Margules3_fminunc(i,:);
TY1(o) = Y1exp(t);
T1(o) = Texp(t);
P1(o) = Pexp(t);
sumINTe1(o) = sumINTexp(t);
L = 1;
p = 1;
break
e1se
L}=L+8
end
end
else
break
end
if p == 1
break
end
end
s = s + 1;
t = t + 1;

```
```

            end
            s = 0;
            t = t - 1;
    end
    % Training Matrix Creation for Gamma2
    monitor2 = zeros(1,1ength(IntXeva12));
    L = 1;
    o = 0;
    p = 0;
    s = 0;
    t = 0;
    for i = 1:1ength(systemsexp(:,1)) % Evaluation of al1 available
    systems in the Experimental Matix.
s = s + 1;
t = t + 1;
k = 1;
while s <= 2
p = 0;
k = 1;
for j'= 1:intp
L = 1;
if s <= 2
for m = 1:int
if and(Xexp(t,L) ==
IntXeva12(j),monitor2(j)<totalsys)
o = 0 + 1;
monitor2(j) = monitor2(j)+1;
SysXe2(o,:) = systemsexp(i,:);
Xe2(o,:) = Xexp(t,:);
TG2(o) = Gammas2Eexp(t);
TA2(o,:) = A_Margules3_fminunc(i,:);
TY2(o) = Y2 exp(t);
T2(o) = Texp(t);
P2(o) = Pexp(t);
sumINTe2(o) = sumINTexp(t);
L = 1;
p = 1;
break
else
L = L + 8;
end
end
else
break
end
if p == 1
break
end
end
s = s + 1;
t = t + 1;
end
s = 0;
t = t - 1;
end
% Training Matrices manipulation and re-arrangement
if isempty(Xe2) == 0
Xe12 = [Xe1 Xe2];

```

Xeva112 = [Xevalc(1,:) Xevalc(2,:)];
sumINTe12 = sumINTe1 + sumINTe2;
sumINTeval12 \(=\) sumINTeval (1) + sumINTeval (2);
IntXe12 = Xe12 (:, 1:8:1ength (Xe12 (1,:))) ; \% Interactions in
Xe12.
IntXe12 = reshape(IntXe12,1,prod(size(IntXe12))); \% Rearrangement in one vector for interaction in Xe12.

IntXeva112 \(=\) Xeva112 (1,1:8:1ength \((X e v a 112(1,:))) ; \%\)
Interactions in Xeval12 to determine Margules equation parameters.
IntXeval12 = reshape(IntXeval12,1,prod(size(IntXeva112))); \%
Re-arrangement in one vector for interactions in Xeval12.
Intjun12 =
unique(union(nonzeros(IntXe12)', nonzeros(IntXeva112)')); \% A11 interactions toghether.

Xe12mod \(=\) zeros(length (Xe12 (: 1, 1)), length(Intjun12)*8); \%
Initialization for Modified Experimental Matrix.
Xeval12mod \(=\) zeros (1,1ength(Intjun12)*8); \% Initialization
for Modified Evaluation Matrix.
\% Verifing that all interactions from the system of interest
are
\% present in the Experimental Matrix
IntXe12 = unique(nonzeros(IntXe12)); \% Interactions present
in the experimental data to determine Margules parameters.
IntXeval12 = unique(nonzeros(IntXeva112)); \% Interactions
present in the system of interest to determine Margules parameters.
tf12 = ismember(IntXeva112,IntXe12); \% Interactions from the system of interest present in the experimental data to determine Margules parameters.

Intfound12 = sum(tf12); \% Interactions from the system of interest found in the experimental data to determine Margules parameters.

Ints12 = 1ength(tf12); \% Interactions from the system of interest available to determine Margules parameters.

Match12(sys,:) = [Intfound12 Ints12];
s12 = 0;
\% Modifying evaluation and experimental variables to align
\% interactions data
for \(\mathbf{i}=1: 1\) ength \((\) nonzeros \((\operatorname{Sys} X e 1(:, 1)))\)
for \(j=1: 8: 1\) ength \((\operatorname{Xe} 12(1,:))\)
u12 = find(ismember (Intjun12,Xe12 (s12+1,j))); if \(\mathrm{Xe} 12(\mathrm{~s} 12+1, \mathrm{j})=0\) else end
end \(\mathrm{s} 12=\mathrm{s} 12+1 ;\)
end
for \(j=1: 8: 7\) ength (Xeva112(1,:))
ueva112 = find(ismember(Intjun12, \(\operatorname{Xeva112(1,j)));~}\)
if Xeval12 \((1, j)==0\)
else
Xeva112mod(: ,8*ueva112-7:8*ueva112) \(=\)
Xeva112(1,j:j+7);
end
end
datapoints (loop) \(=\) sum(SysXe1 (: 3) \()\);
\% Extracting excess data from Experimental Training Matrices \(j=0\);
PG12 \(=\) []; \% Training Matrix with only information to be used to determine Mergules parameters.

PG12 = [T1',P1'];
for \(\mathrm{i}=1\) : 1 ength (Intjun12)
PG12 =
[PG12, (Xe12mod(:,\(j+4) . * x e 12 \bmod (:, j+5)) . / s u m I N T e 12 '] ;\) j = j + 8;
end
\% Extracting excess data from Evaluation Training Matrices \(\mathrm{j}=0\);
SG12 = []; \% Evaluation Matrix with only information to be
used to determine Margules parameters.
SG12 = [Teval, Peval];
for \(\mathbf{i}=1\) :1ength(Intjun12)
SG12 =
[SG12, (Xeva112mod (:,j+4).*Xeva112mod(:,j+5))./sumINTeva112(1)'];
j = j + 8;
end
PG12 = PG12';
SG12 = SG12';
TA1 = TA1';
\% Neural Networks Training
[fPG1 cPG1] = size(PG12);
[fTA1 cTA1] = size(TA1);
P11 = PG12 (: , 1:cei1 (cPG1/2));
P21 = PG12 (:, ceil(cPG1/2)+1:cPG1);
T11 = TA1(:,1:cei1(cTA1/2));
T21 = TA1 (:, cei1(cTA1/2) \(+1:\) cTA1);
P31 = SG12;
T31 = A_Margules3_eval';
n2 = 3;
pp1 = [P11 P21];
tt1 = [T11 T21];
\(\operatorname{mmax} 1=\operatorname{minmax}(P G 12)\);
pack
b111 =
w111 =
b121 = [];
w121 = [];
e = [];
a31 = [];
max_n = 5;
\% NN Optimum Structure Search
tf = \{'logsig' 'purelin'\};
for \(i=1: 9\)
disp(i)
e1 = [];
for \(\mathrm{j}=1:\) max_n \% Hidden layer optimum number of neurons
nneu = [j n2];
net1 = newff(mmax1,nneu,tf);
net1.trainParam.show = NaN; \%Instruction to disable
training graphics.
net1.trainParam.mem_reduc \(=4\); \%Instruction to reduce
memory requirement for Jacobian Matrix calculation.
[net1 tr1] = train(net1,P11,T11);
a1 = \(\operatorname{sim}(\) net1, P21) ;
e1 (j,:) = mean(T21 - a1);
pack \% Instruction to reduce memory space used for
variables.
end
```

        SSE1 = diag(e1 * e1');
        [m1 pos1] = min(SSE1);
        nno1(loop) = pos1;
        nneu1 = [nno1(1oop) n2];
        a1 = [];
        app1 = [];
        e1 = [];
        % Optimum initial point search
        for k = 1:20
        net1 = newff(mmax1,nneu1,tf);
        net1.trainParam.show = NaN;
        net1.trainParam.mem_reduc = 4;
        [net1 tr1] = train(net1,pp1,tt1);
        eva1(['b11',num2str(k),'= net1.b{1,1};'])
        eval(['b21',num2str(k),' = net1.b{2,1};'])
        eva1(['w11',num2str(k),' = net1.iw{1,1};'])
        eval(['w21',num2str(k),' = net1.1w{2,1};'])
        a1(:,:,k) = sim(net1,pp1);
        e1(k,:) = mean(tt1 - a1(:,:,k));
        pack
    end
    SSE1 = diag(e1 * e1');
    [m1 piol] = min(SSE1);
    net1 = newff(mmax1, nneu1,tf);
    eval(['net1.b{1,1} = b11',num2str(pio1),';'])
    eval(['net1.b{2,1} = b21',num2str(pio1),';'])
    eval(['net1.iw{1,1} = w11',num2str(pio1),';''])
    eval(['net1.7w{2,1} = W21',num2str(pio1),';'])
    net1.trainParam.show = NaN;
    net1.trainParam.mem_reduc = 4;
    [net1 tr1] = train(net1,pp1,tt1);
    app1 = sim(net1,pp1);
    a31(i,:) = sim(net1,P31);
    end
    % Final results determination based on data central tendency.
    aSG1 = sort(a31);
    for e = 1:2
        aSG1(1,:) = [];
    end
    for e = 7:-1:6
        aSG1(e,:) = [];
    end
    aSG1med = mean(aSG1);
    A_NN = aSG1med(1);
    B_NN = aSG1med(2);
    C_NN = aSG1med(3);
    Gamma1M = exp(((A_NN+3*B_NN+5*C_NN).*(X2eva1.^2))-
    ((4*(B_NN+4*C_NN)).*(X2eval.^3))+((12*C_NN).*(X2eval.^4)));
Gamma2M = exp(((A_NN-3*B_NN+5*C_NN).*(x1eval.^2))+((4*(B_NN-
4*C_NN)).*(X1eva1.^3))+((12*C_NN).*(X1eval.^4)));
% Data Plot and Saving
linex = [0 1];
liney = [0 1];
Y1predANN = ((x1eval.*10.^(Antoine1eval(:,1)'-
(Antoine1eval(:,2)'./((Teval_Y)+Antoine1eval(:,3)')))).*Gamma1M)./(P
eva1_Y);
Y2predANN = ((X2eval.*10.^(Antoine2eval(:,1)'-
(Antoine2eva1(:,2)'./((Teva1_Y)+Antoine2eva1(:,3)')))).*Gamma2M)./(P
eva1_Y);
eva1(['figure(',num2str(sys),num2str(tota1sys),')'])

```
```

    subplot(2,2,1:2)
    plot(X1eval,Gamma1M,'b',X1eva1,Gamma2m,'r')
    title(['System: ' Molecule1 ' (1) + ' Molecule2 ' (2)'])
    1egend('Gamma1','Gamma2','Best')
    xlabel('x1');
    ylabel('Gamma');
    xlim([0 1]);
    subplot(2,2,3)
    plot(linex,\iney,'k',x1eval,Y1predANN,'g')
    xlabel('x1');
    ylabe1('Y1pred');
    axis([0 1 0 1]);
    subplot(2,2,4)
    plot(7inex, liney,'k',x2eva1,y2predANN,'g')
    xlabel('x2');
    ylabe1('Y2pred');
    axis([0 1 0 1]);
    toc
    time(loop) = toc;
    Header =
    {'Temp(}\mp@subsup{}{}{\circ}\textrm{C})','P(mmHg)','x1','Y1_pred','Gamma1_ANN','Gamma2_ANN'}
Data = [Teval_Y Peval_Y X1eval Y1predANN Gamma1M Gamma2M];
eval(['xlswrite(''',userdata, ''', Header, ''Output',
num2str(sys), ''');']);
eva1(['x1swrite(''',userdata, ''', Data, ''Output',
num2str(sys),''',''A2'');']);
end
end

```
\%Function Create_Gamma_user.m
\% This program will create the data base for the activity coefficients
\% estimation program.
function g = Create_Gamma_user(userdata)
\% Load the data file where the user data is contain. s = ['data = xlsread(''' userdata '.xls'');']; eval(s); \(\mathrm{g}=186\);
\begin{tabular}{lllllllllll} 
MW \(=[12\) & 13 & 14 & 15 & 16 & 12 & 13 & 14 & 12 & 13 & 29 \\
30 & 31 & 32 & 29 & 30 & 31 & 40 & 42 & 44 & 46 & 41 \\
42 & 43 & 43 & 44 & 45 & 43 & 44 & 45 & 42 & 43 & 41 \\
43 & 41 \\
43 & 44 & 52 & 54 & 56 & 58 & 53 & 54 & 55 & 55 & 56 \\
55 & 56 & 57 & 54 & 55 & 53 & 46 & 59 & 58 & 59 & 60 \\
57 & 58 & 59 & 60 & 68 & 70 & 72 & 74 & 69 & 70 & 71 \\
71 & 72 & 74 & 71 & 72 & 73 & 70 & 71 & 69 & 28 & 29 \\
30 & 31 & 39 & 41 & 43 & 45 & 50 & 52 & 56 & 59 & 27 \\
38 & 39 & 40 & 41 & 58 & 59 & 60 & 61 & 45 & 46 & 47 \\
48 & 47.5 & 48.5 & 49.5 & 50.5 & 32 & 52 & 31 & 50 & 69 & 51 \\
70 & 34 & 33 & 85.5 & 102 & 104.5 & 137.567 .5 & 84 & 119.5 & 83 \\
118.5 & 86.5 & 103 & 66.5 & 68.5 & 85 & 121 & 154 & 12 & 13 & 29 \\
54 & 84 & 73.5 & 40 & 56 & 57 & 58 & 59 & 67 & 69 & 71 \\
73 & 68 & 69 & 70 & 71 & 72 & 73 & 70 & 71 & 72 & 69 \\
70 & 68 & 66 & 81 & 85 & 87 & 80 & 82 & 84 & 83 & 85 \\
86 & 81 & 83 & 85 & 80 & 82 & 79 & 18 & 68 & 73 & 28 \\
44 & 32 & 57 & 62.5 & 96 & \(31] ;\) & & & & &
\end{tabular}
\% Raw data manipulation
systems \(=[\) nonzeros(data(:,1)) find(data(:,1))];
systems_Margules3 = [nonzeros(data(:,1)) find(data(:,1))];
```

systems_Margules3 = [systems_Margules3; 1ength(systems_Margules3)+1
1ength(data(:,1))];
X = [];
x1mol]= [];
x2mol = [];
GF1 = [];
GF2 = [];
Antoine1 = [];
Antoine2 = [];
P_exp = [];
T_exp = [];
Max = max(systems(:,1));
for i = 1:1ength(systems(:,1))
S = int2str(i);
M = num2str(Max);
% x matrix creation
X1_Margules3 = [];
x2_Margules3 = [];
T_Margules3 = [];
P_Margules3 = [];
Antoine1_Margules3 = [];
Antoine2_Margules3 = [];
points_Margules3(i) = systems_Margules3(i+1,2) -
systems_Margules3(i,2) - 8;
X1_Margules3 =
data(systems_Margules3(i,2)+8:systems_Margules3(i,2)+8+points_Margu1
es3(i)-1,4)';
X2_Margules3 = 1-X1_Margules3;
T_Margules3=
data(systems_Margules3(i,2)+8:systems_Margules3(i,2)+8+points_Margu7
es3(i)-1,2)';
P_Margu1es3 =
data(systems_Margules3(i,2)+8:systems_Margules3(i,2)+8+points_Margu7
es3(i)-1,3)';
Antoine1_Margules3 =
[nonzeros(data(systems_Margules3(i,2)+1,:))'];
Antoine2_Margules3 =
[nonzeros(data(systems_Margules3(i,2)+2,:))'];
if or(x1_Margules3(1)==0, x1_Margules3(1)==1) == 1
x1_Margules3(1) = [];
X2_Margules3(1) = [];
T_Margules3(1) = [];
P_Margules3(1) = [];
points_Margules3(i) = points_Margules3(i)-1;
else
end
if
or(X1_Margu1es3(points_Margu7es3(i))==0,X1_Margu1es3(points_Margu7es
3(i))==1) == 1
X1_Margules3(points_Margules3(i)) = [];
x2_Margules3(points_Margules3(i)) = [];
T_Margules3(points_Margu7es3(i)) = [];
P_Margules3(points_Margules3(i)) = [];
points_Margules3(i) = points_Margules3(i)-1;
else
end
Antoine1 = [Antoine1;Antoine1_Margules3];
Antoine2 = [Antoine2;Antoine2_Margules3];
x1mol = [x1mol;x1_Margules3'];
x2mol = [x2mol;x2_Margules3'];

```
```

    P_exp = [P_exp;P_Margules3'];
    T_exp = [T_exp;T_Margu7es3'];
    P = data(systems(i,2)+7,3);
    points = 0;
    point = 0;
    while P ~= 0
    xpoint = 1;
    ypoint = 1;
    if data(systems(i,2)+point+8,4) == 0
        ypoint = 0;
    end
    if data(systems(i,2)+point+8,4) == 1
        ypoint = 0;
    end
    if and(xpoint,ypoint) == 1
        points = points + 1;
    else
    end
    point = point + 1;
    P = data(systems(i,2)+8+point,3);
    end
    systems(i,3) = points;
    NGF1 = 1ength(nonzeros(data(systems(i,2)+3,:)));
    NGF2 = 1ength(nonzeros(data(systems(i,2)+5,:)));
    [o,p] = size(X);
    k = 1;
    = 0;
    % Suma de 1a cantidad total de interacciones.
sumINT(o+1) = 0;
sumINT(o+2) = 0;
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
sumINT(0+1) = sumINT(0+1) +
(data(systems(i,2)+4,r+1)*data(systems(i,2)+6,s+1));
sumINT(o+2) = sumINT(o+2) +
(data(systems(i,2)+4,r+1)*data(systems(i,2)+6,s+1));
else
end
end
end
% 1)Posisionar el numero de la interacción.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
GF1 = [GF1;data(systems (i, 2)+3,r+1)];
GF2 = [GF2;data(systems(i,2)+5,s+1)];
x(o+1,1+k) = g * (data(systems(i,2)+3,r+1) - 1) +
data(systems(i, 2)+5,s+1);
x(o+2,1+k) = g * (data(systems(i,2)+5,s+1) - 1) +
data(systems(i,2)+3,r+1);
1 = 1 + 8;
else
end
end
end
k = k + 1;
1 = 0;
% 2)Posisionar la Temperatura del sistema.
for r = 1:NGF1

```
```

        for s = 1:NGF2
            if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
                X(0+1,1+k) = mean(T_Margules3);
                        x(0+2,1+k) = mean(T_Margules3);
                        1 = 1 + 8;
            else
            end
                end
            end
    k = k + 1;
    1 = 0;
    % 3)Posisionar la Presión del sistema.
    for r = 1:NGF1
        for s = 1:NGF2
            if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
                X(0+1,1+k) = mean(P_Margules3);
                x(0+2,1+k) = mean(P_Margules3);
                1 = 1 + 8;
            else
            end
        end
    end
    k = k + 1;
    1 = 0;
    % 4)Posisionar la cantidad de GF de la molécula \#1 en la
interacción.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
x(0+1,1+k) = data(systems(i,2)+4,r+1);
x(0+2,1+k) = data(systems(i,2)+6,s+1);
1 = 1 + 8;
else
end
end
end
k = k + 1;
1 = 0;
% 5)Posisionar la cantidad de GF de 1a molécula \#2 en la
interacción.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
x(0+1,1+k) = data(systems(i,2)+6,s+1);
X(0+2,1+k) = data(systems(i,2)+4,r+1);
1 = 1 + 8;
else
end
end
end
k = k + 1;
1 = 0;
sumMW1 = 0;
sumMW2 = 0;
% 6)Posisionar el peso molecular de1 grupo funcional de la molécula
\#1.
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)

```
```

                        x(0+1,1+k) =
    data(systems(i,2)+4,r+1)*MW(data(systems(i, 2)+3,r+1));
X(o+2,1+k) =
data(systems(i,2)+6,s+1)*MW(data(systems(i, 2)+5,s+1));
1 = 1 + 8;
else
end
end
sumMW1 = sumMW1 +
data(systems(i, 2)+4,r+1)*MW(data(systems(i, 2)+3,r+1));
end
k = k + 1;
1 = 0;
% 7)Posisionar el peso molecular del grupo funcional de la molécula
\#2.
for s = 1:NGF2
for r = 1:NGF1
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
x(0+1,1+k) =
data(systems(i,2)+6,s+1)*MW(data(systems(i, 2)+5,s+1));
x(0+2,1+k)=
data(systems(i,2)+4,r+1)*MW(data(systems(i, 2)+3,r+1));
1=1+8;
else
end
end
sumMW2 = sumMW2 +
data(systems(i, 2)+6,s+1)*MW(data(systems(i, 2)+5,s+1));
end
k = k + 1;
1 = 0;
% 8)Posisionar 1
for r = 1:NGF1
for s = 1:NGF2
if data(systems(i,2)+3,r+1) ~= data(systems(i,2)+5,s+1)
X(0+1,1+k) = 1;
x(0+2,1+k) = 1;
1 = 1 + 8;
else
end
end
end
k = k + 1;
1 = 0;
end
X_user = X;
P_exp_user = P_exp;
T_exp_user = T_exp;
x1mol_user = x1mol;
X2mo1_user = X2mol;
systems_user = systems;
Antoine1_user = Antoine1;
Antoine2_user = Antoine2;
sumINT_user = sumINT;
save database_user X_user systems_user P_exp_user T_exp_user
X1mol_user X2mo1_user Antoine1_user Antoine2_user sumINT_user

```
```

